

Rheology of granular flows: Role of the interstitial fluid



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Motivations :
debris flows, landslides, avalanches, silo

Not Fault!!!

Low level of pressure:

10-100 kPa in natural events
0.1-1 kPa in the experiments

=> Rigid and non breakable particles



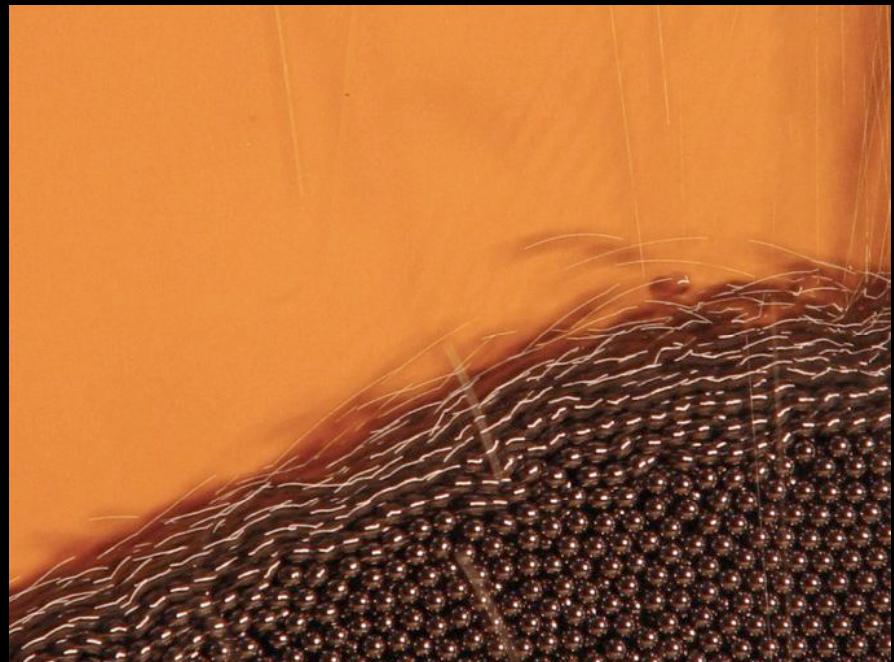
Particles of different sizes
+ liquid (non newtonian)
+ complex topography
+ unsteady flows ...

?????????????????????

In this talk :

1) rheology of dry granular flows ?...

2) What happen when coupling with the interstitial fluid matters ...?

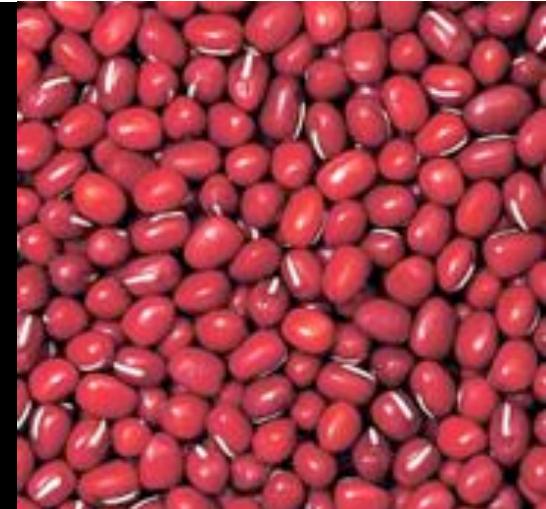


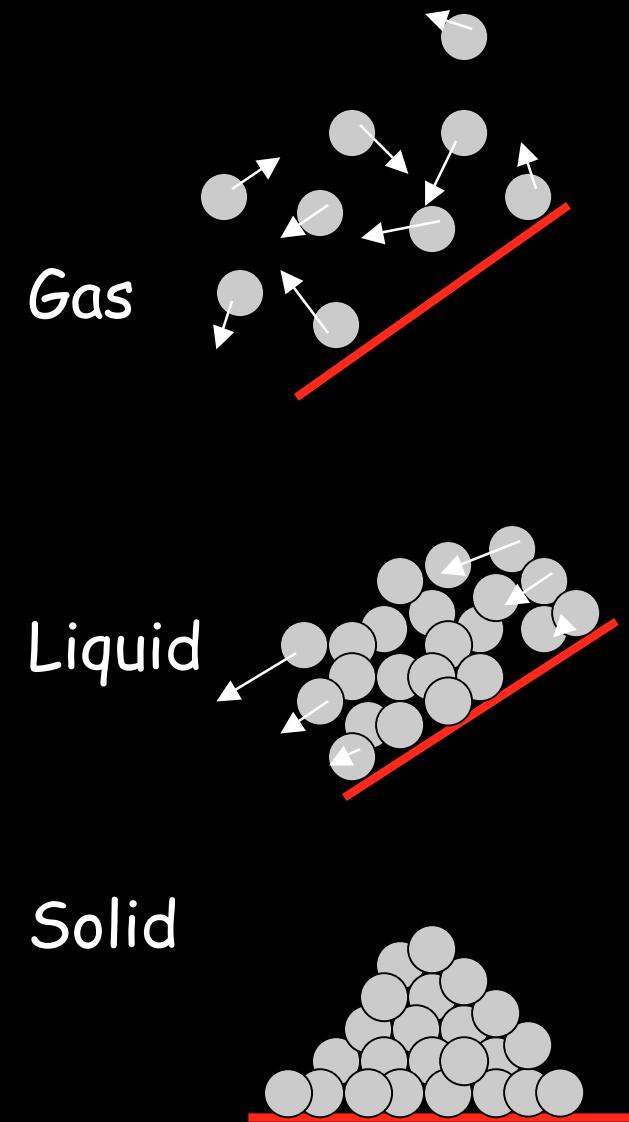
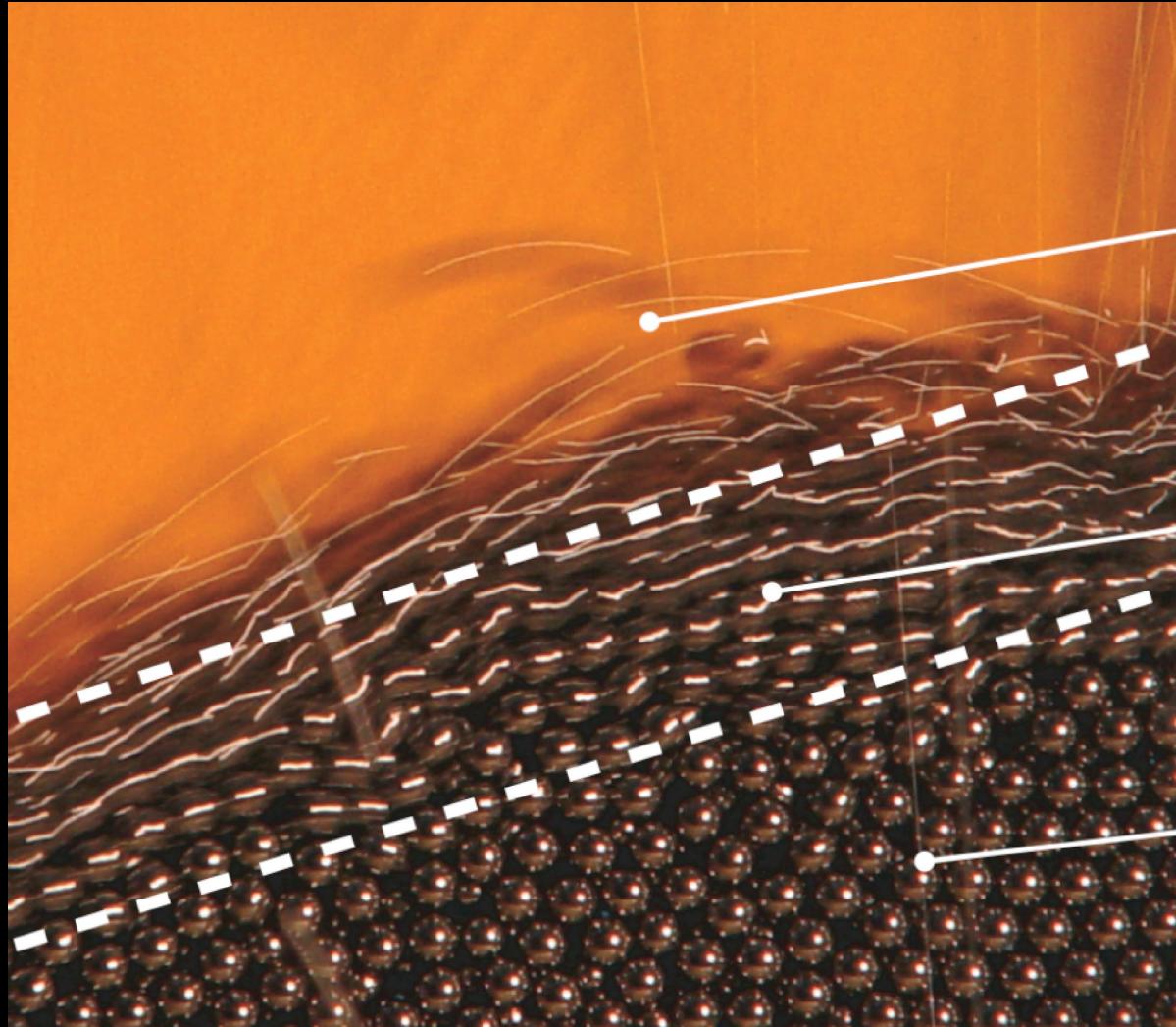
Dry granular material: Collection of grains

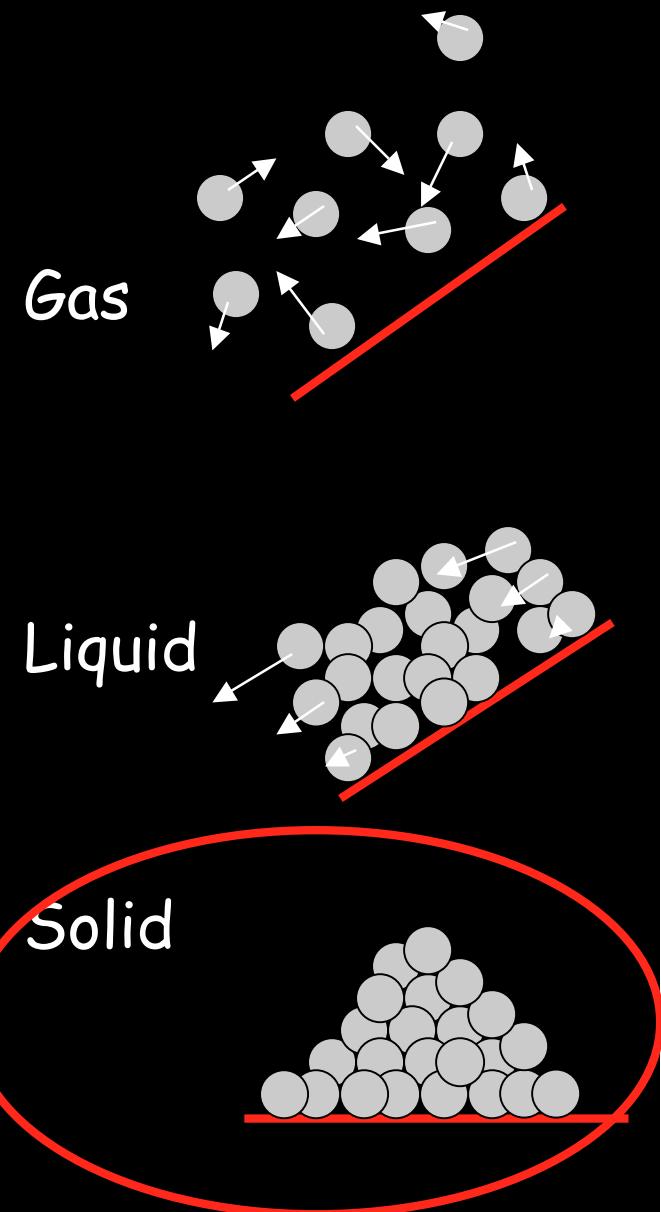
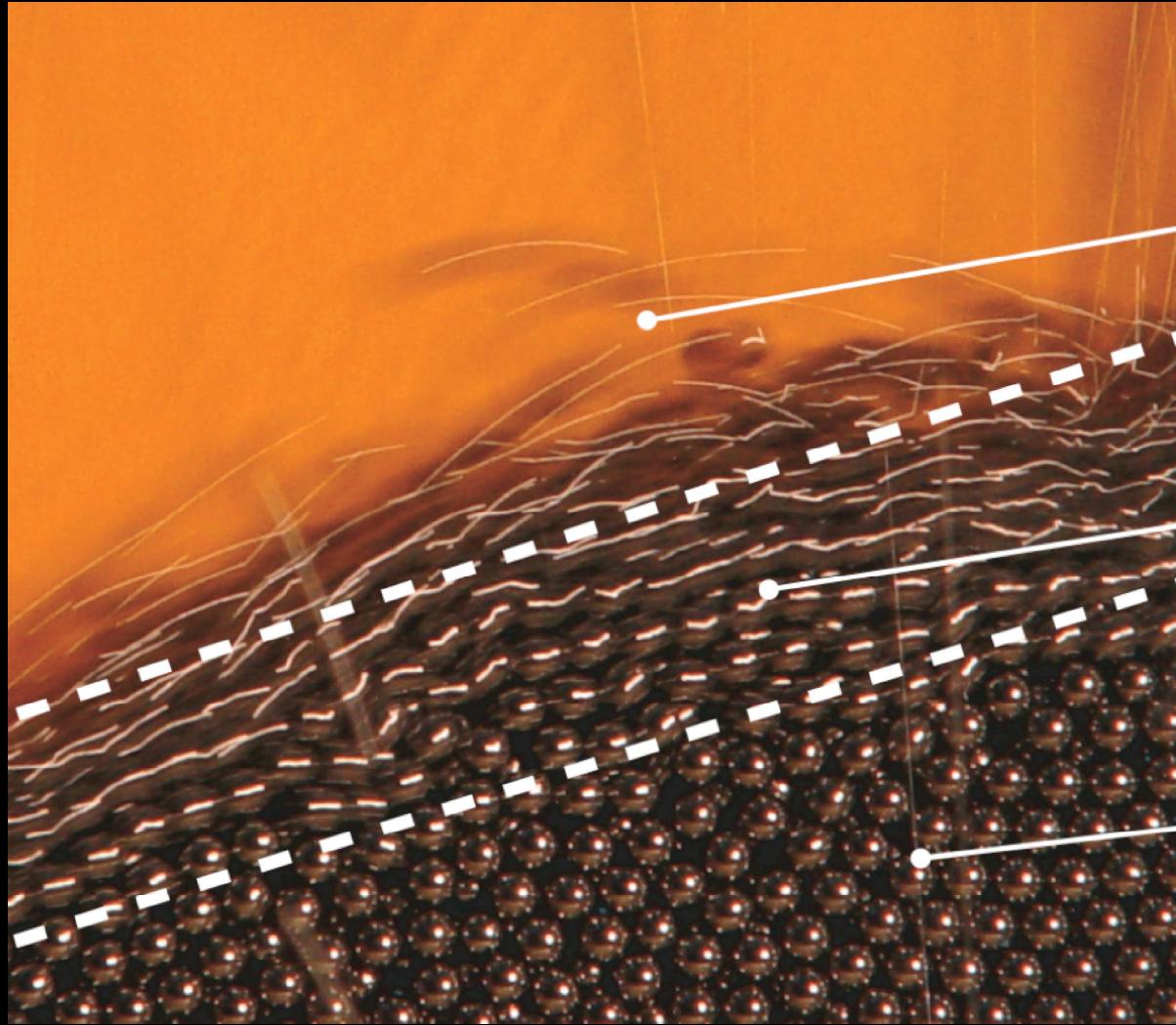
No cohesion
No brownian motion
No fluid interaction

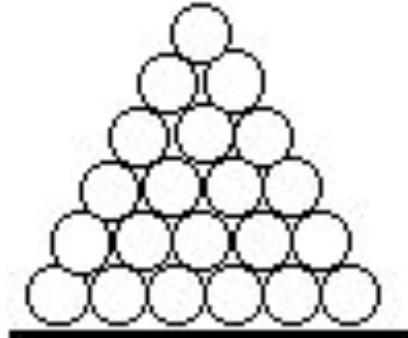
... Only contact interactions

But not so easy...









« solid »

Quasi-static deformations : Soil mechanics and plasticity

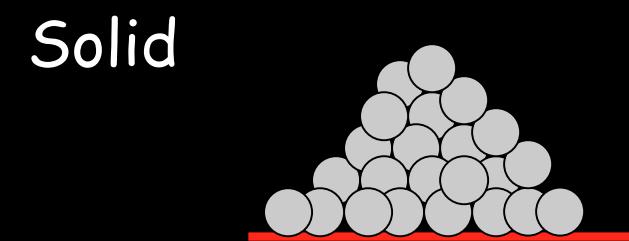
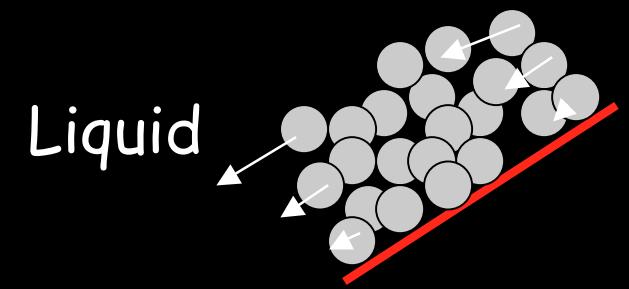
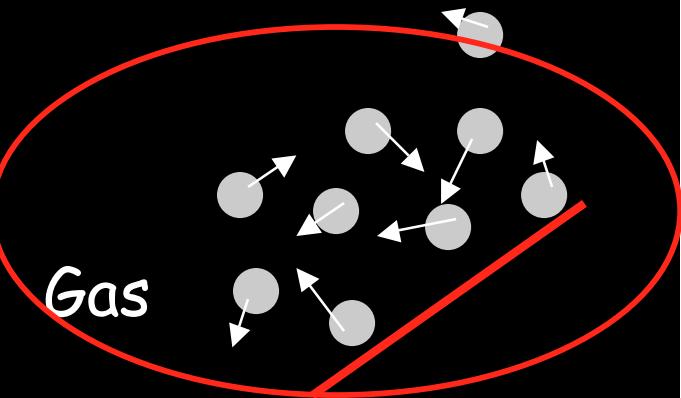
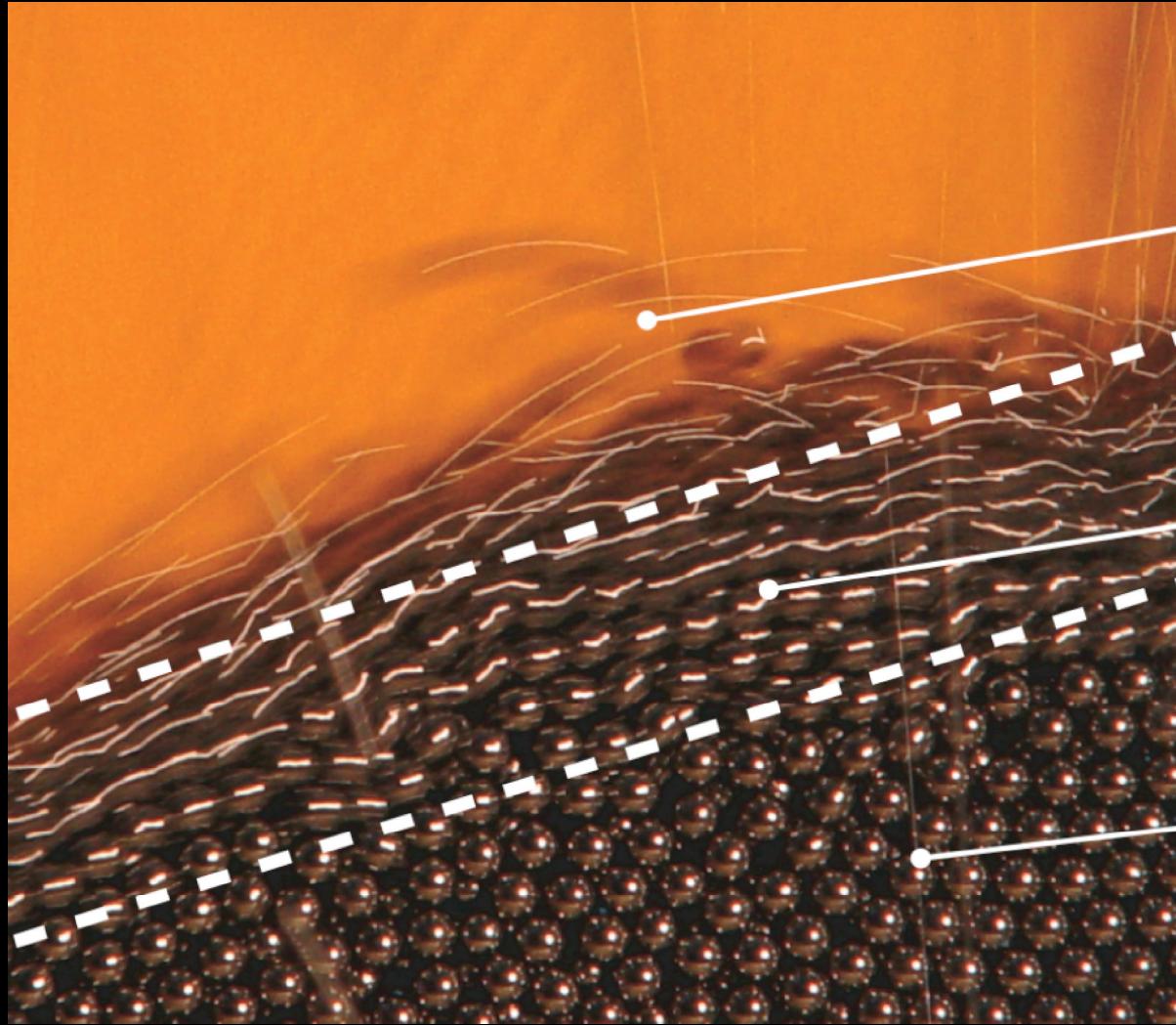
Focus on initial deformation

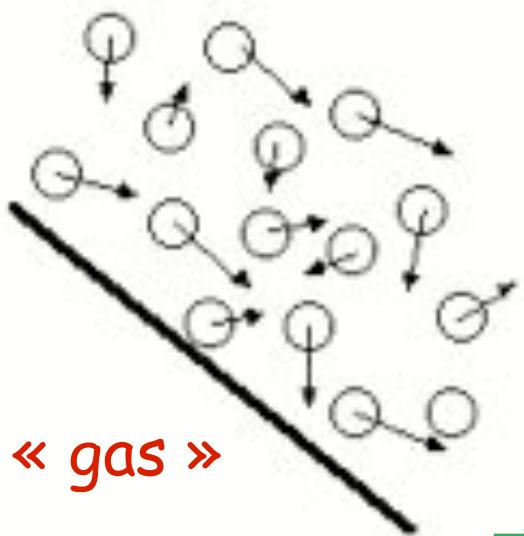
What happens :

⇒ at large deformations ?

⇒ for fast deformations ?







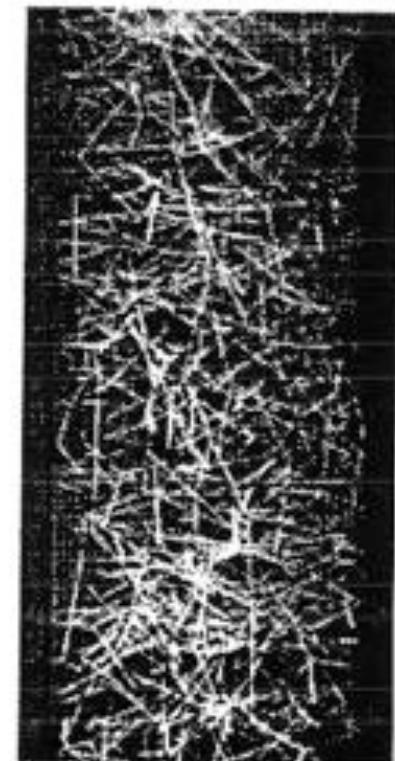
Kinetic theory for rapid granular gases

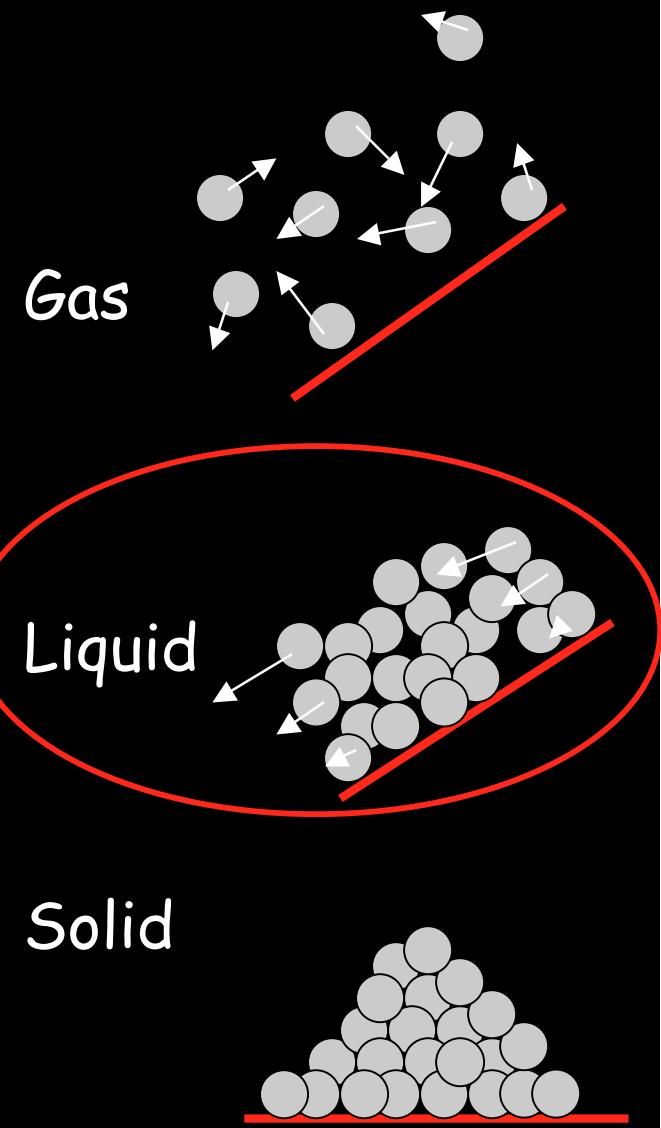
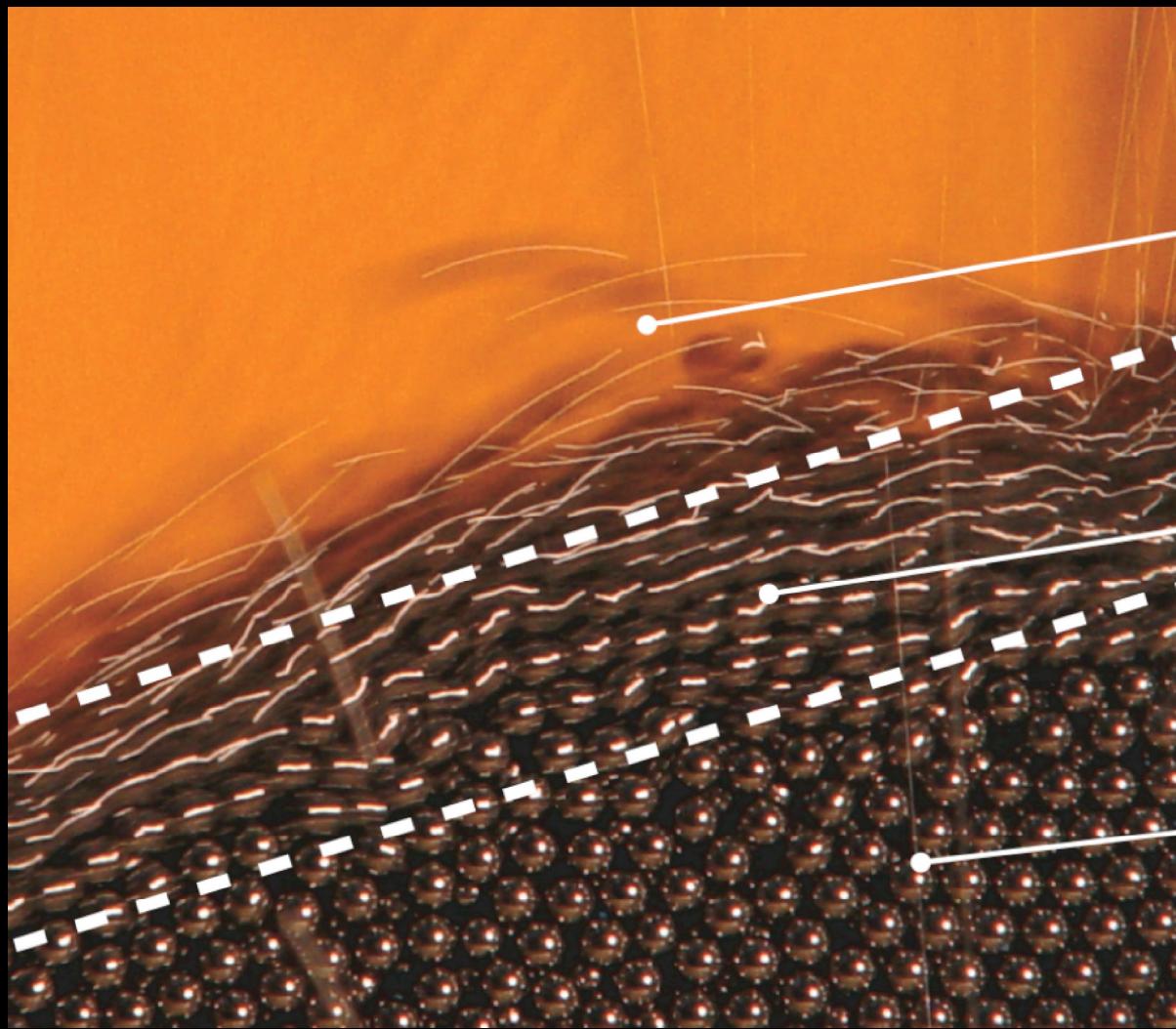
Binary collisions+inelastic collisions

⇒ constitutive equations coupling
Density, velocity and granular temperature

But if not enough energy is injected:

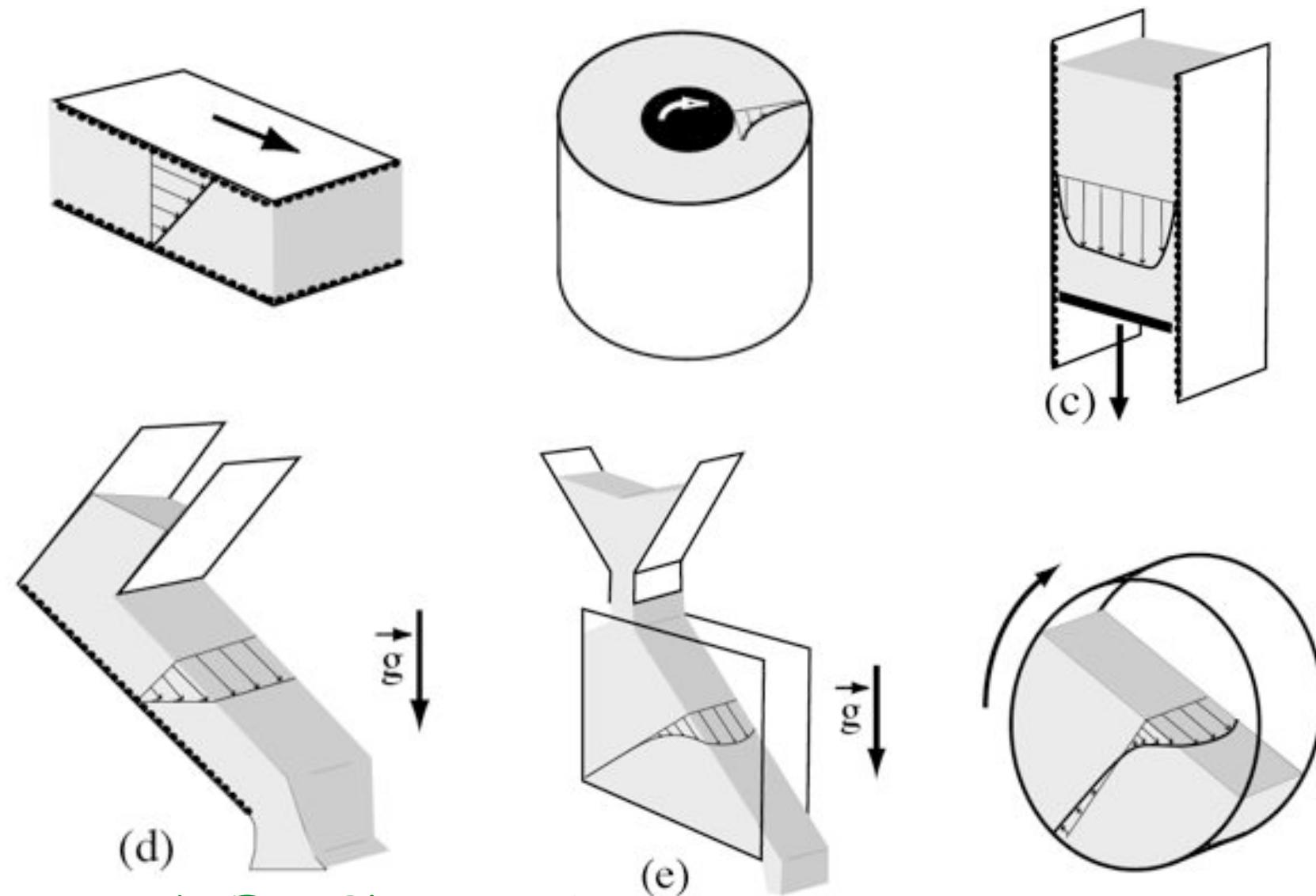
- ⇒ finite duration contact,
- ⇒ multiple contact,



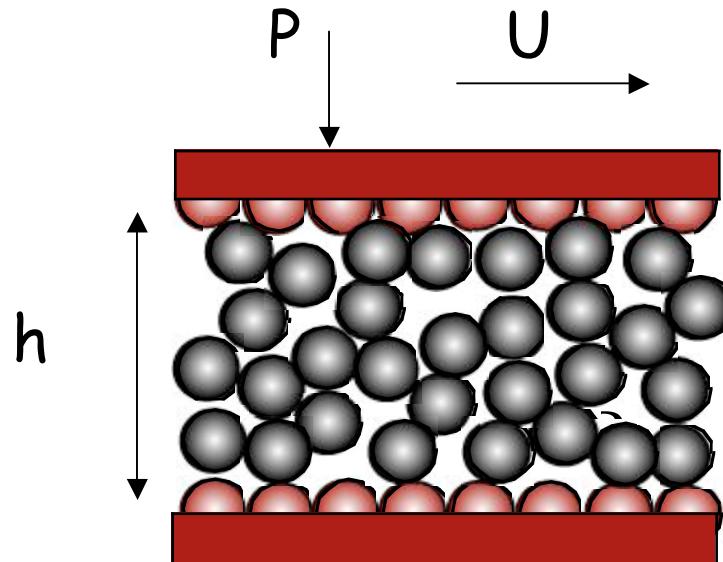




Different flow configurations studied both experimentally and numerically



plane shear under controlled normal stress



A schematic diagram of a right-angled triangle representing a small element of the granular layer. The hypotenuse is labeled $\dot{\gamma} = U/h$, representing the shear rate.

Lois et al 2005
Da Cruz et al, PRE 05
GdR Midi, Eur. Phys. J 04

One imposes P and $\dot{\gamma}$

Shear stress τ ?
Volume fraction ϕ ?

A single dimensionless number
(inertial number)

$$I = \frac{\dot{\gamma} d}{\sqrt{P/\rho_s}}$$

(Savage 84,
Ancey et al 99)

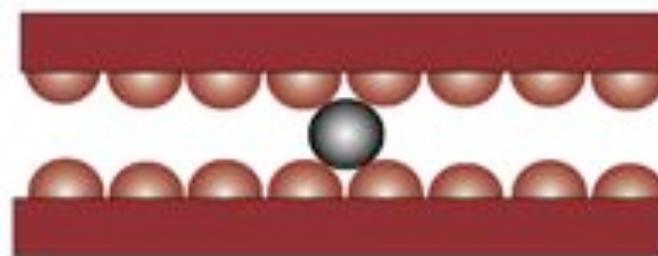
Inertial number

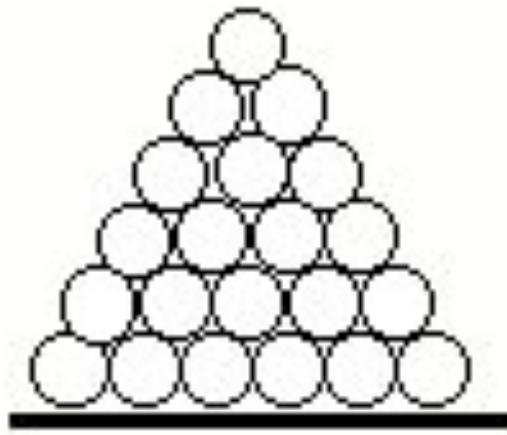
$$I = \frac{\dot{\gamma}d}{\sqrt{P/\rho_s}}$$

* ratio between 2 times :

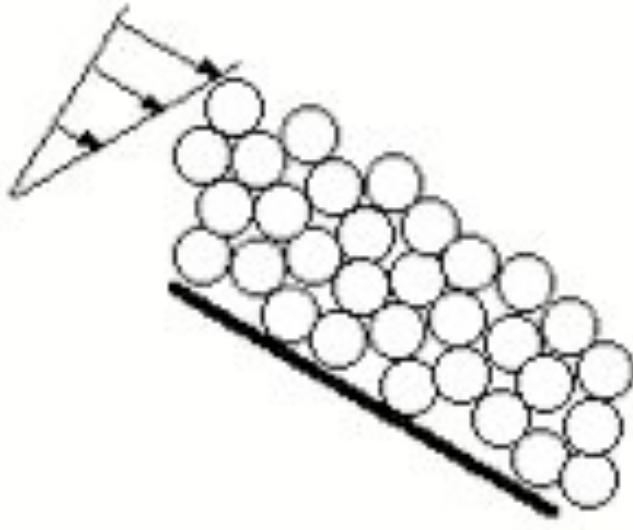
$1/\dot{\gamma}$: time scale of the mean shear

$d/\sqrt{P/\rho_s}$: microscopic time for rearrangement

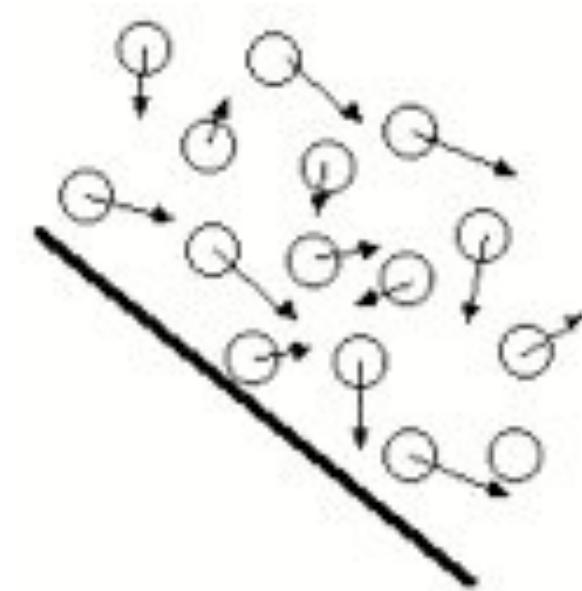




« quasi-static »



« liquid »



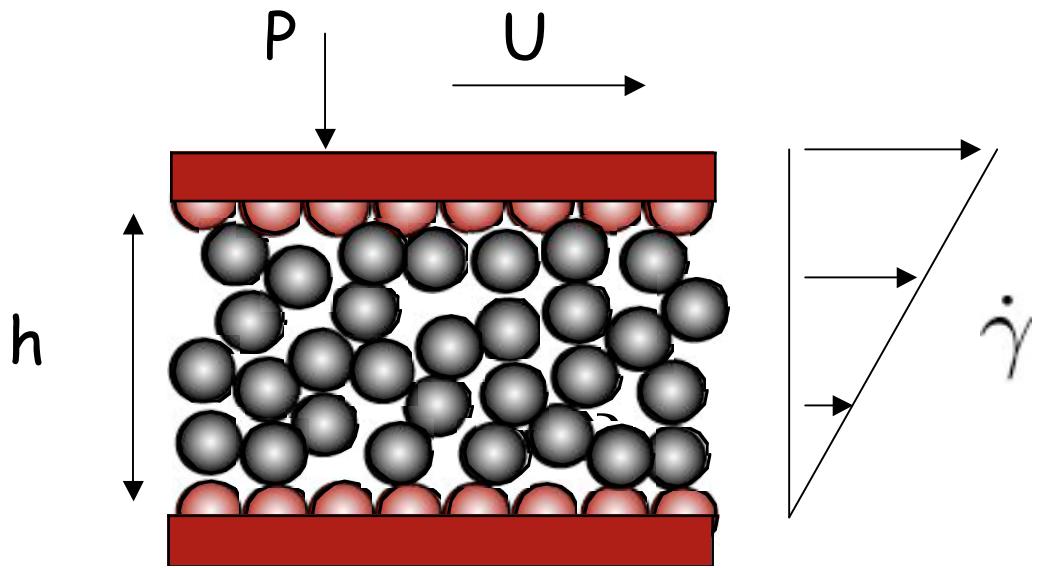
« gas »

0

1

$$I = \frac{\dot{\gamma} d}{\sqrt{P / \rho}}$$

Da Cruz et al, PRE 05
GdR Midi Eur. Phys. J 04

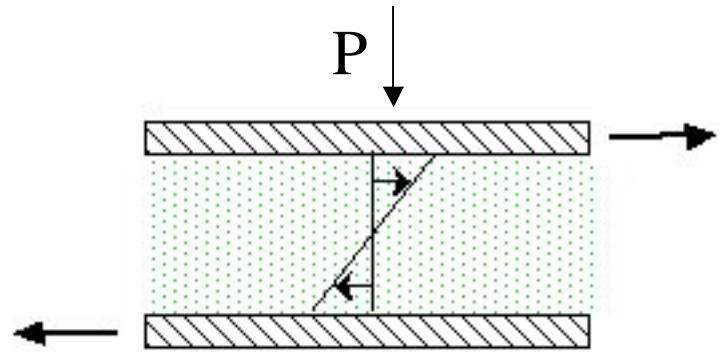


One imposes P and $\dot{\gamma}$

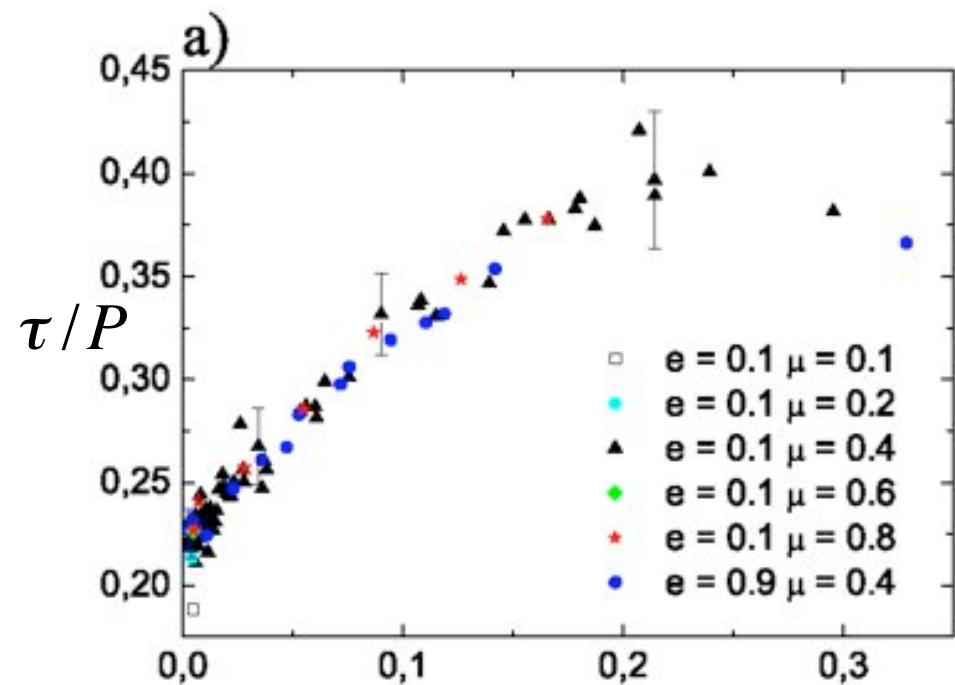
Shear stress τ ?
Volume fraction ϕ ?

$$\tau = \mu(I)P$$

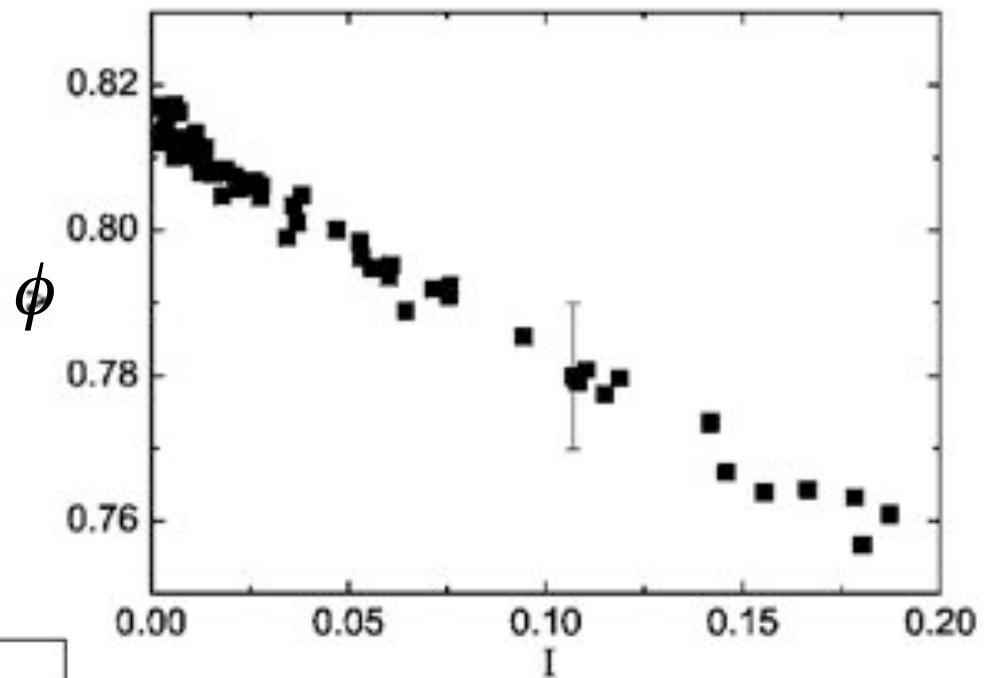
$$\Phi = \Phi(I)$$



$$\tau = \mu(I)P$$

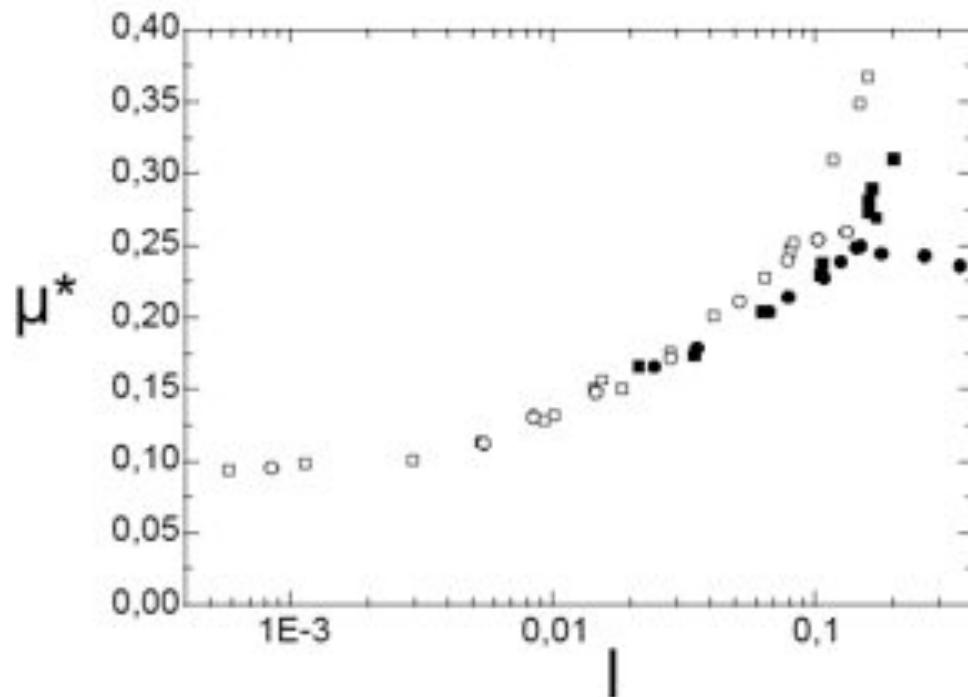


$$I = \frac{\dot{\gamma} d}{\sqrt{P/\rho}}$$



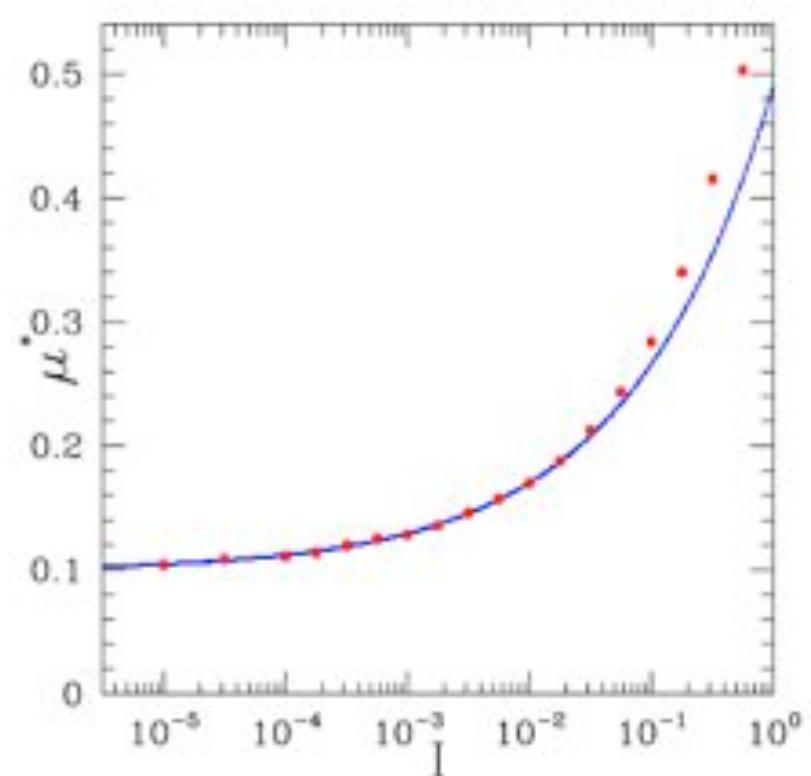
$$\phi = \phi(I)$$

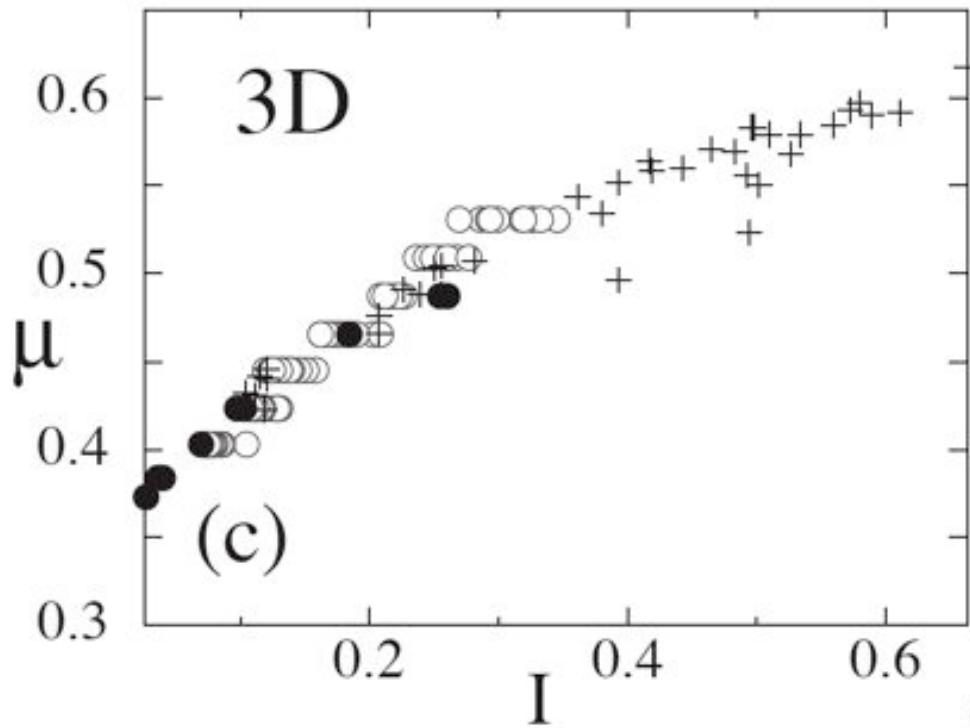
remark: No velocity weakening



Dacruz et al PRE 05

Peyneau & Roux PRE 08





Forterre, Pouliquen ARFM 08

For spheres

Data from

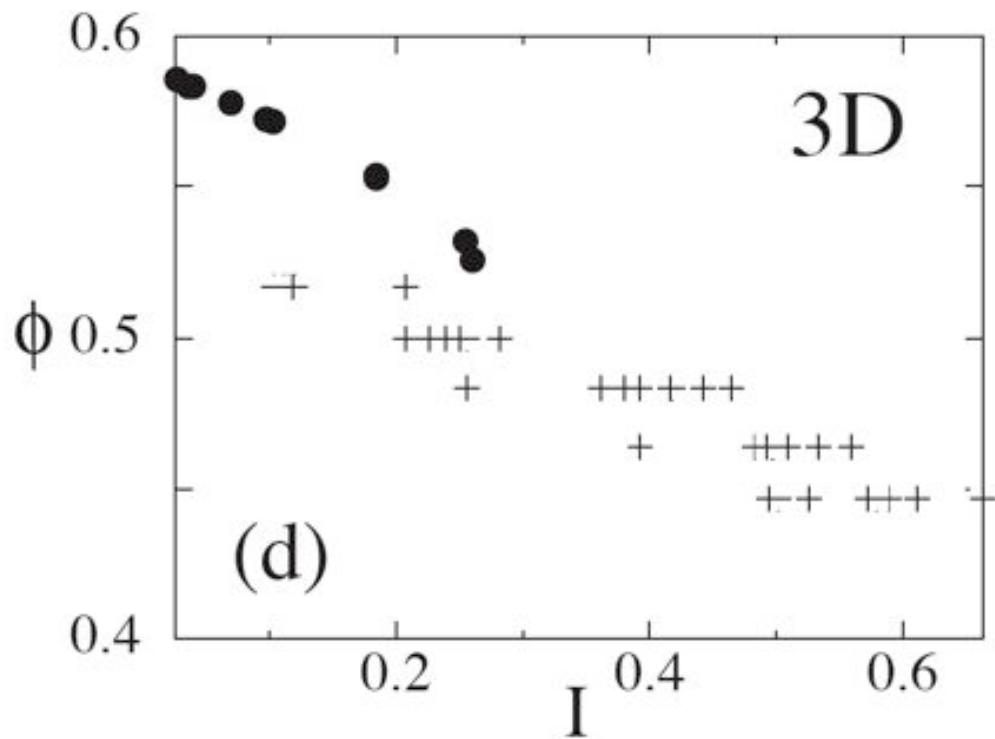
Inclined plane exp. (Pouliquen 99)

Inclined plane simulations

(Baran et al 2006)

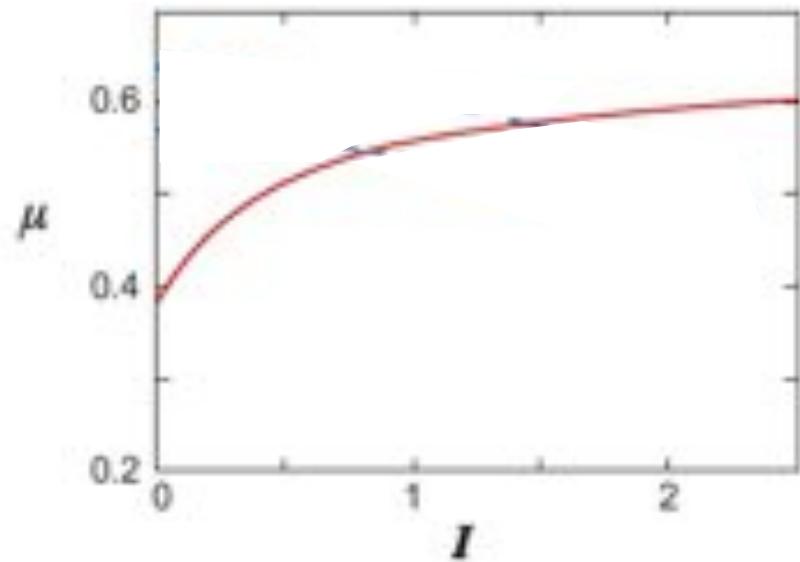
Annular shear cell exp.

(Sayed, Savage JFM, 84)

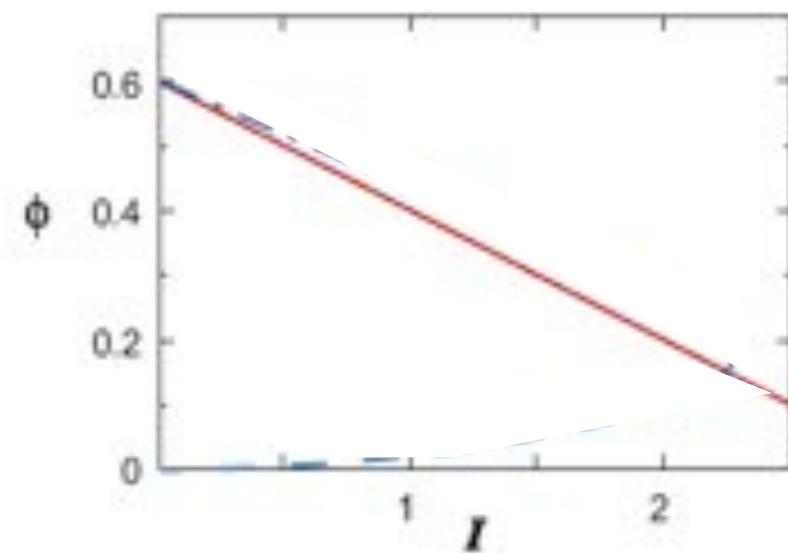


An empirical friction law:

$$\tau = \mu(I)P$$



$$\Phi = \Phi(I)$$



$$\mu(I) = \mu_s + \frac{\mu_2 - \mu_s}{I_0 / I + 1}$$

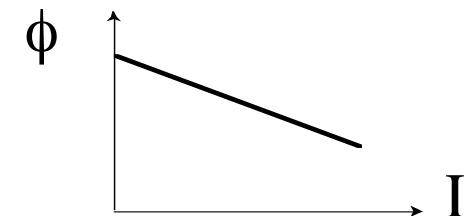
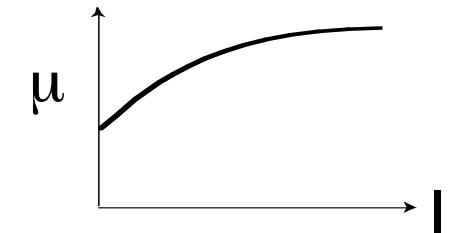
$$\phi(I) = \phi_{max} - AI$$

Constant pressure

$$I = \frac{\dot{\gamma}d}{\sqrt{P/\rho_s}}$$

$$\tau = \mu(I)P$$

$$\Phi = \Phi(I)$$



$$\Phi(I) = f_1^{-1}(1/I^2) \quad \mu(I) = I^2 f_2(f_1^{-1}(1/I^2))$$

And shear at constant volume fraction ??

Bagnold Proc. R. Soc 54

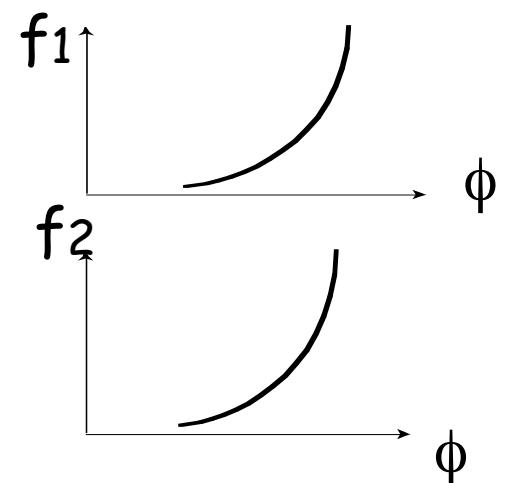
Lois et al PRE 07

Lemaître PRE 05

Da Cruz et al PRE 05

$$\tau = f_1(\Phi)\rho_s d^2 \dot{\gamma}^2$$

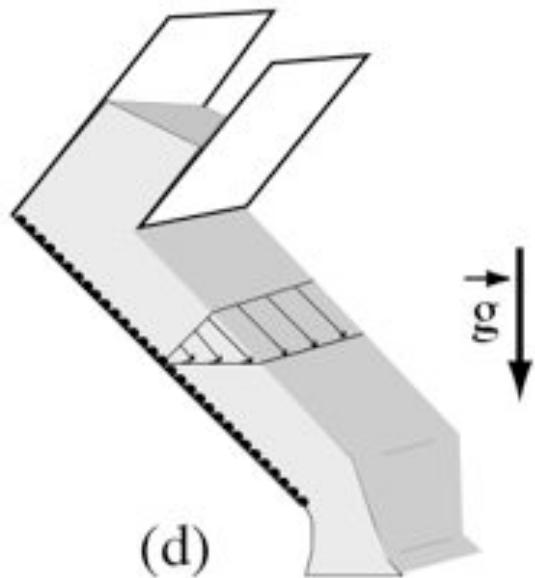
$$P = f_2(\Phi)\rho_s d^2 \dot{\gamma}^2$$



$$\tau = \mu(I)P$$

$$\Phi = \Phi(I)$$

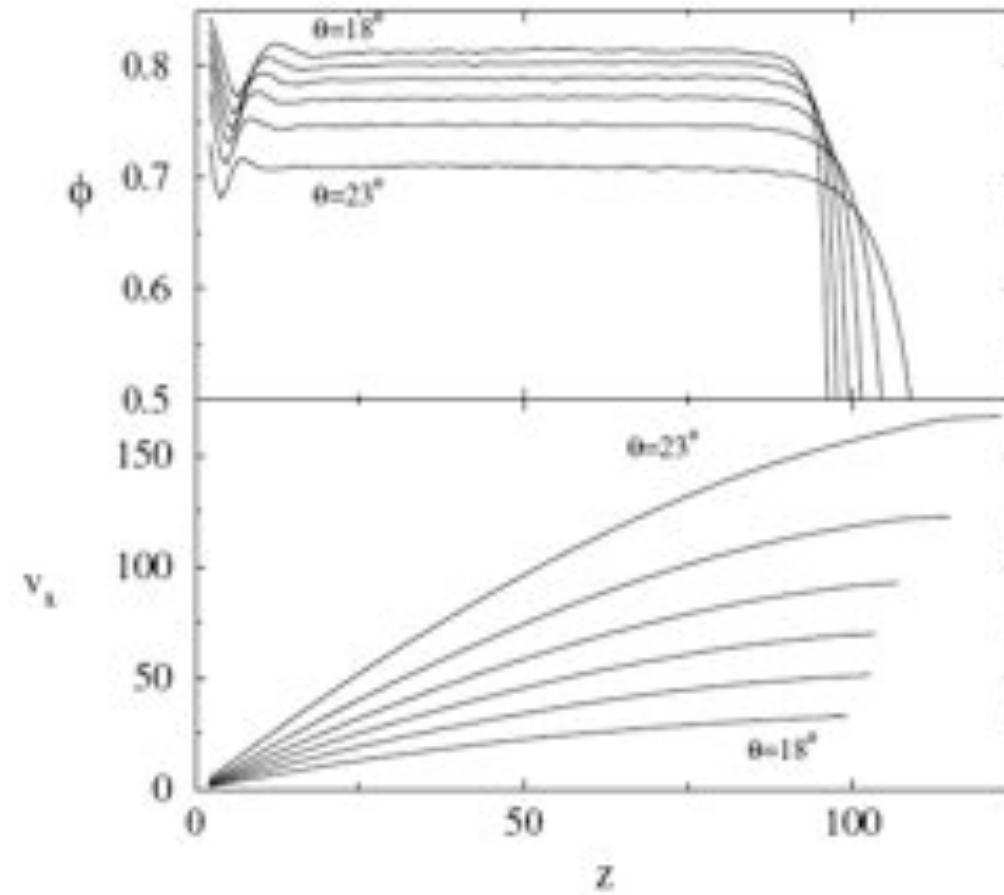
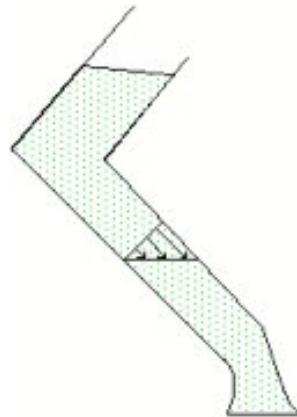
allows to describe (not perfectly) velocity profiles
on inclined plane,



Let's go further...

Predicted velocity and volume fraction profiles

Rheology $\mu(I)$ predicts $-V \propto h^{1.5} - (h-z)^{1.5}$
 $d\Phi = cte$



Gdr Midi et al, 2004,
Da cruz et al 2002,
Silbert et al 2001

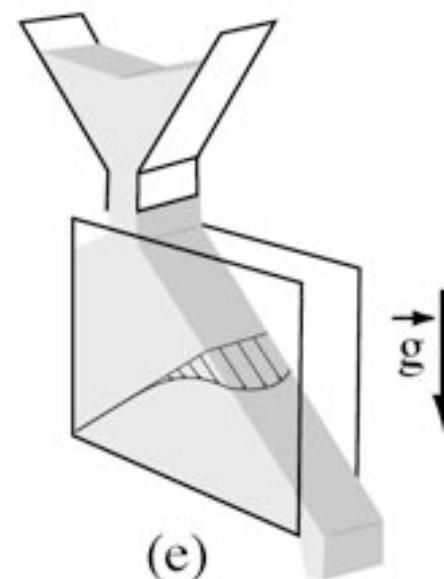
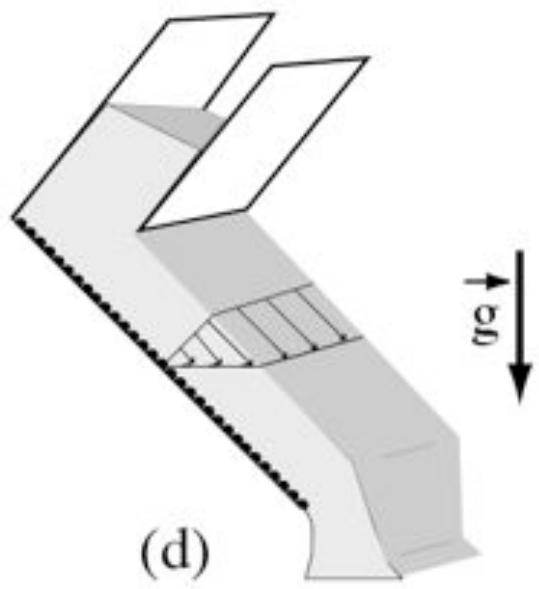
-Pb with thin flows and close to free surface

Gdr Midi et al, 2004,
Da cruz et al 2002,
Rajchenbach 2003

$$\tau = \mu(I)P$$

$$\Phi = \Phi(I)$$

allows to describe (not perfectly) velocity profiles
on inclined plane, on pile,...



Let's go further...

3D generalisation: a visco-plastic model (Jop et al Nature 06)

assumptions :

1) P isotropic

2) $\dot{\gamma}_{ij}$ and τ_{ij} are colinear

(Savage 83, Goddard 86, Schaeffer 87,...)

$$\tau_{ij} = \frac{\mu(I)P \dot{\gamma}_{ij}}{||\dot{\gamma}||}$$



Effective
viscosity

$$\dot{\gamma}_{ij} = \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}$$

$$||\dot{\gamma}|| = \sqrt{1/2 \dot{\gamma}_{ij} \dot{\gamma}_{ji}}$$

3D generalisation of the friction law :
granular flows as a viscoplastic fluid
(Jop et al Nature 06)

assumptions:

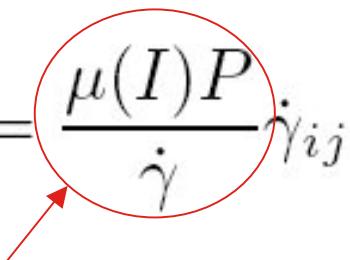
- 1) P isotropic
- 2) $\dot{\gamma}_{ij}$ and τ_{ij} are co-linear

(Savage 83, Goddard 86, Schaeffer 87,...)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial z} = 0,$$

$$\rho_s \phi \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial z} \right) = \rho_s \phi g \sin \theta - \frac{\partial P}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{xz}}{\partial z},$$

$$\rho_s \phi \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial z} \right) = -\rho_s \phi g \cos \theta - \frac{\partial P}{\partial z} + \frac{\partial \tau_{zx}}{\partial x} + \frac{\partial \tau_{zz}}{\partial z},$$

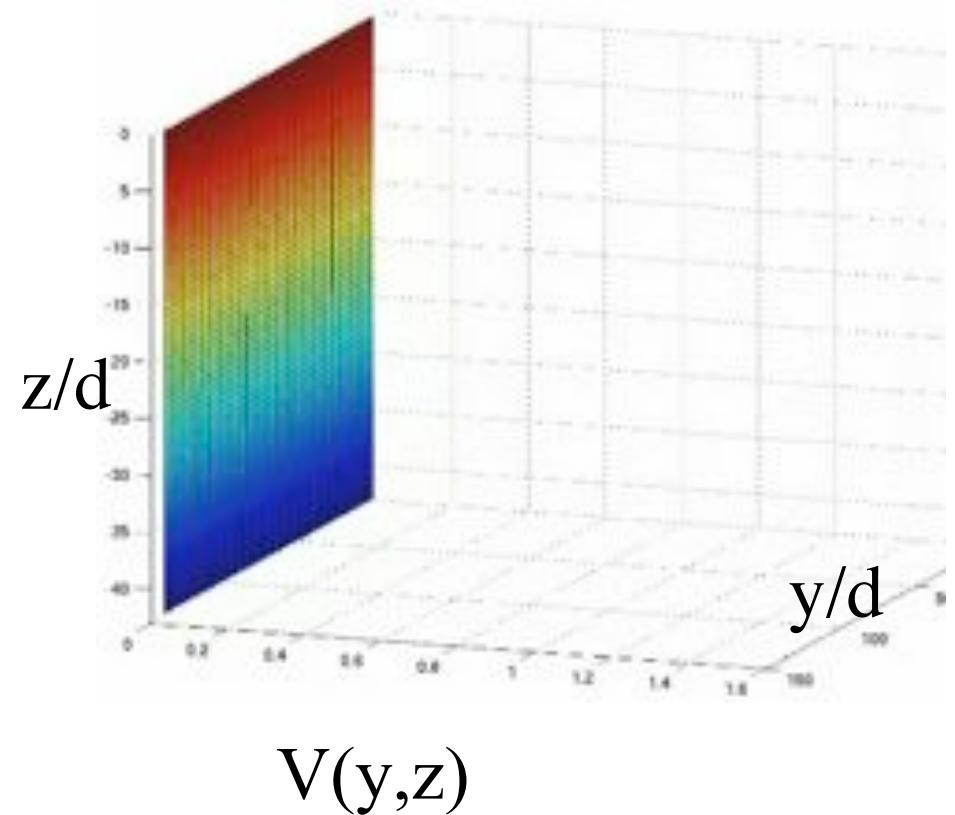
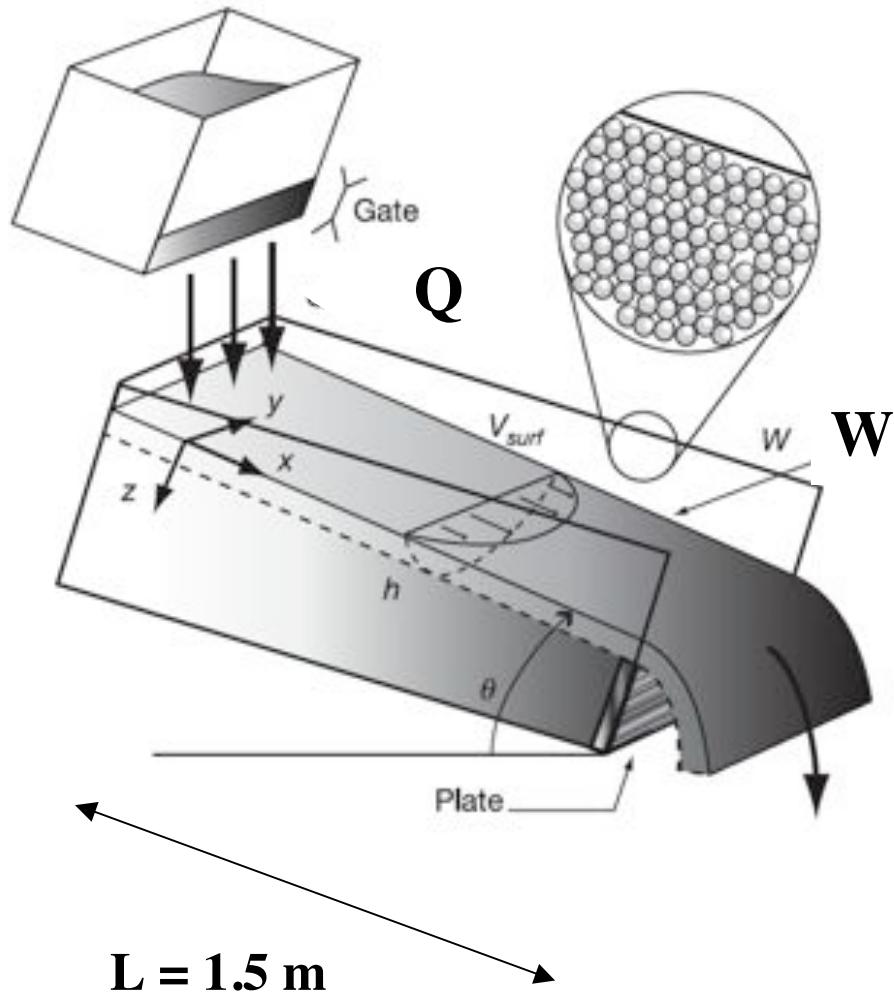
$$\tau_{ij} = \frac{\mu(I)P}{\dot{\gamma}} \dot{\gamma}_{ij}$$


$$I = \frac{\dot{\gamma} d}{\sqrt{P/\rho_s}}$$

Pressure dependent viscosity

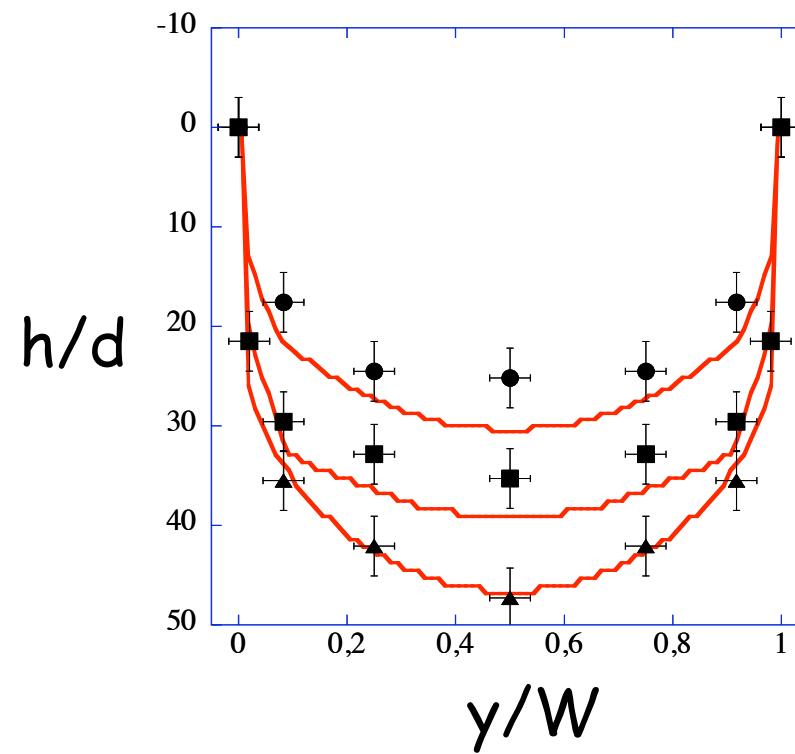
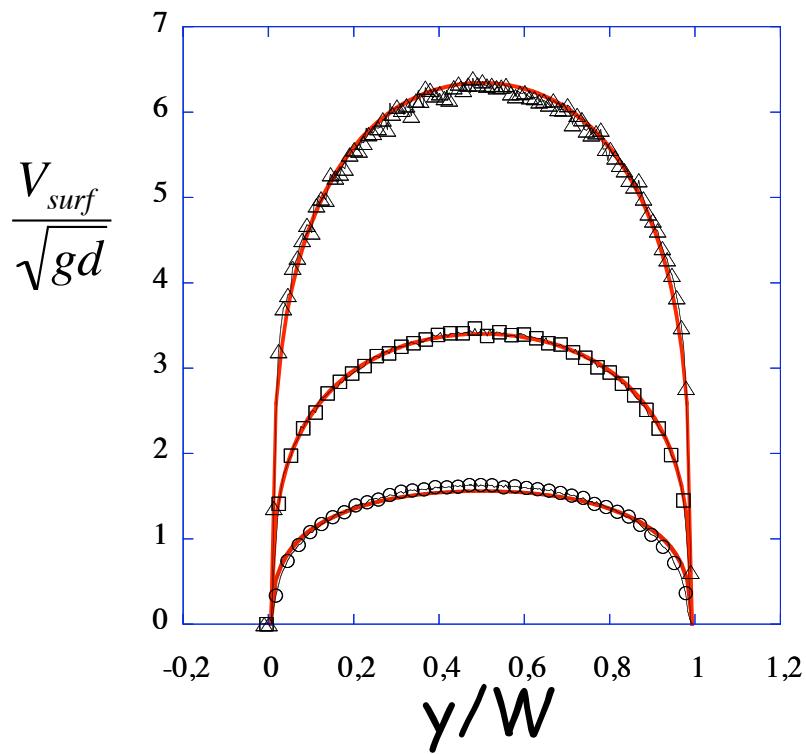
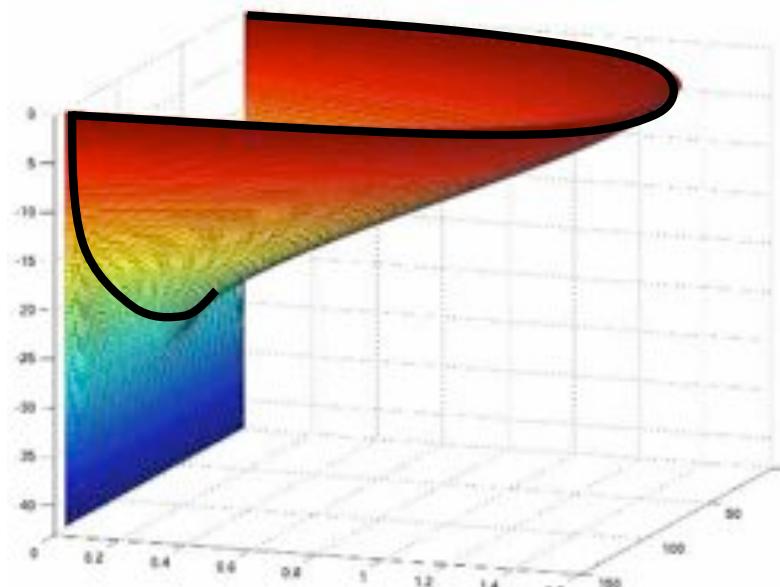
flows on a heap : a full 3D problem

(P. Jop et al Nature 06)

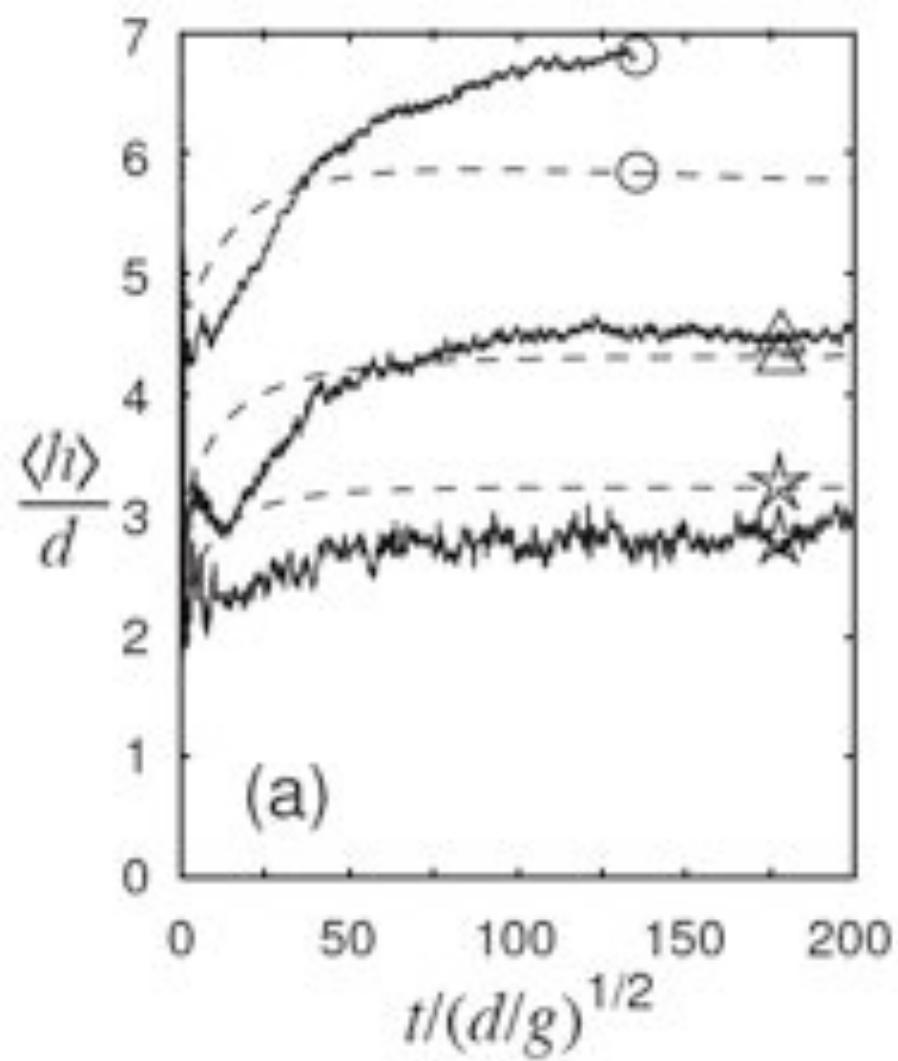
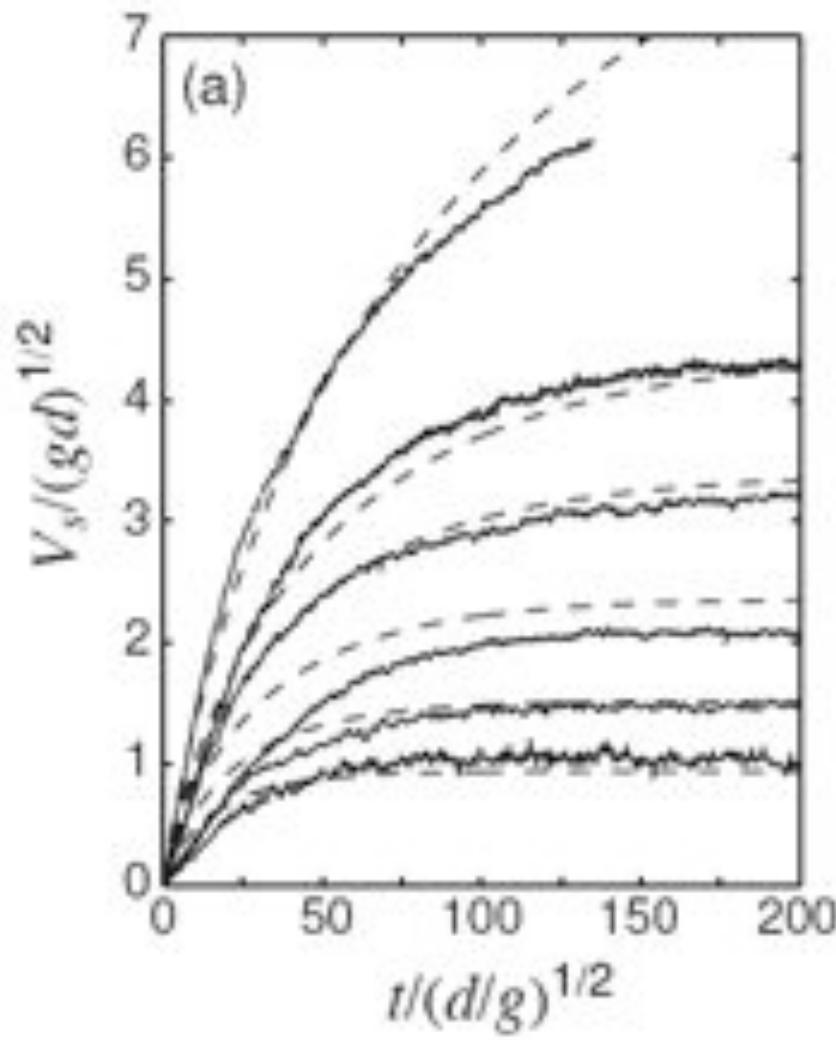


Flow between rough lateral walls:

Jop et al , Nature 2006

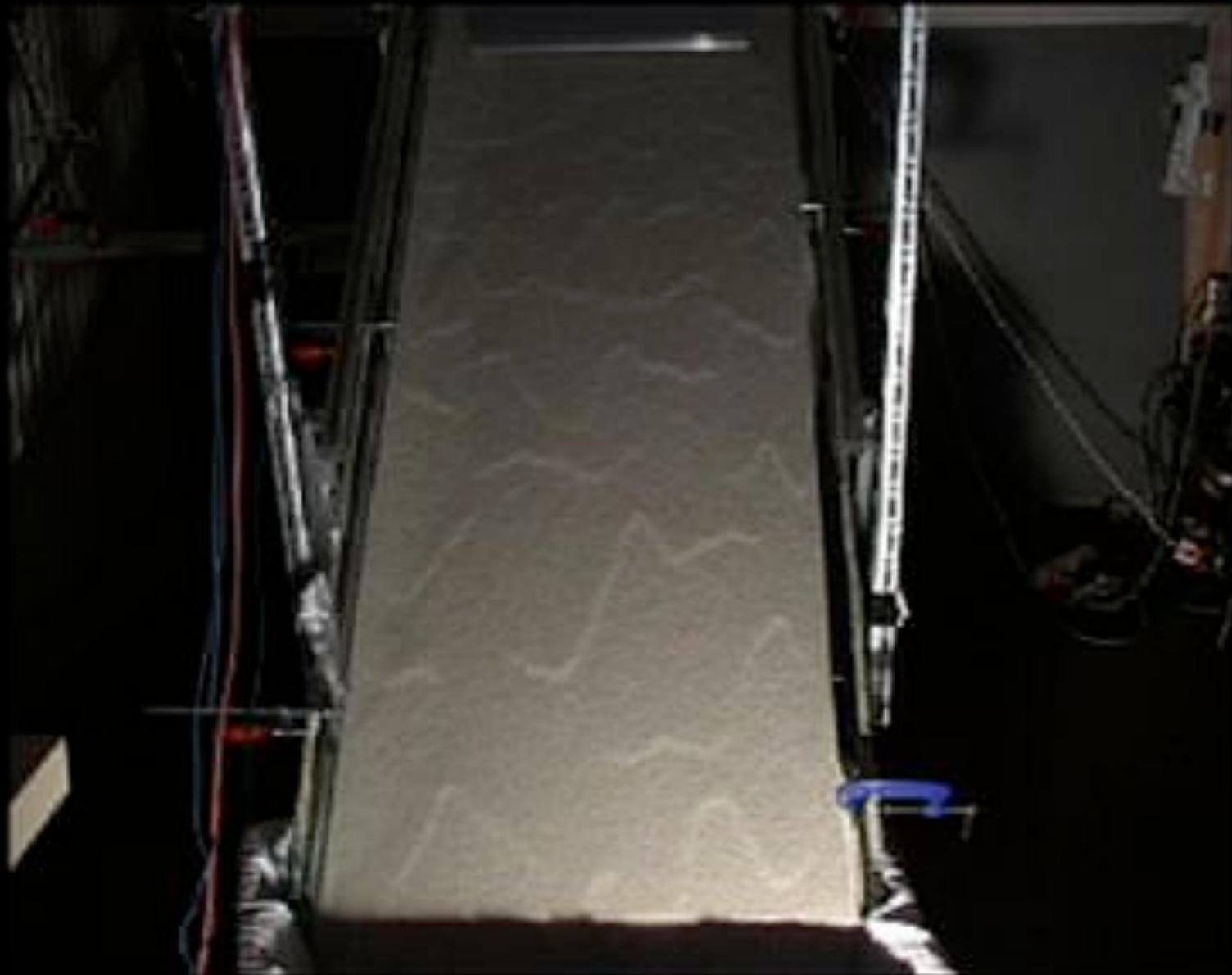


Initiation of the flow?

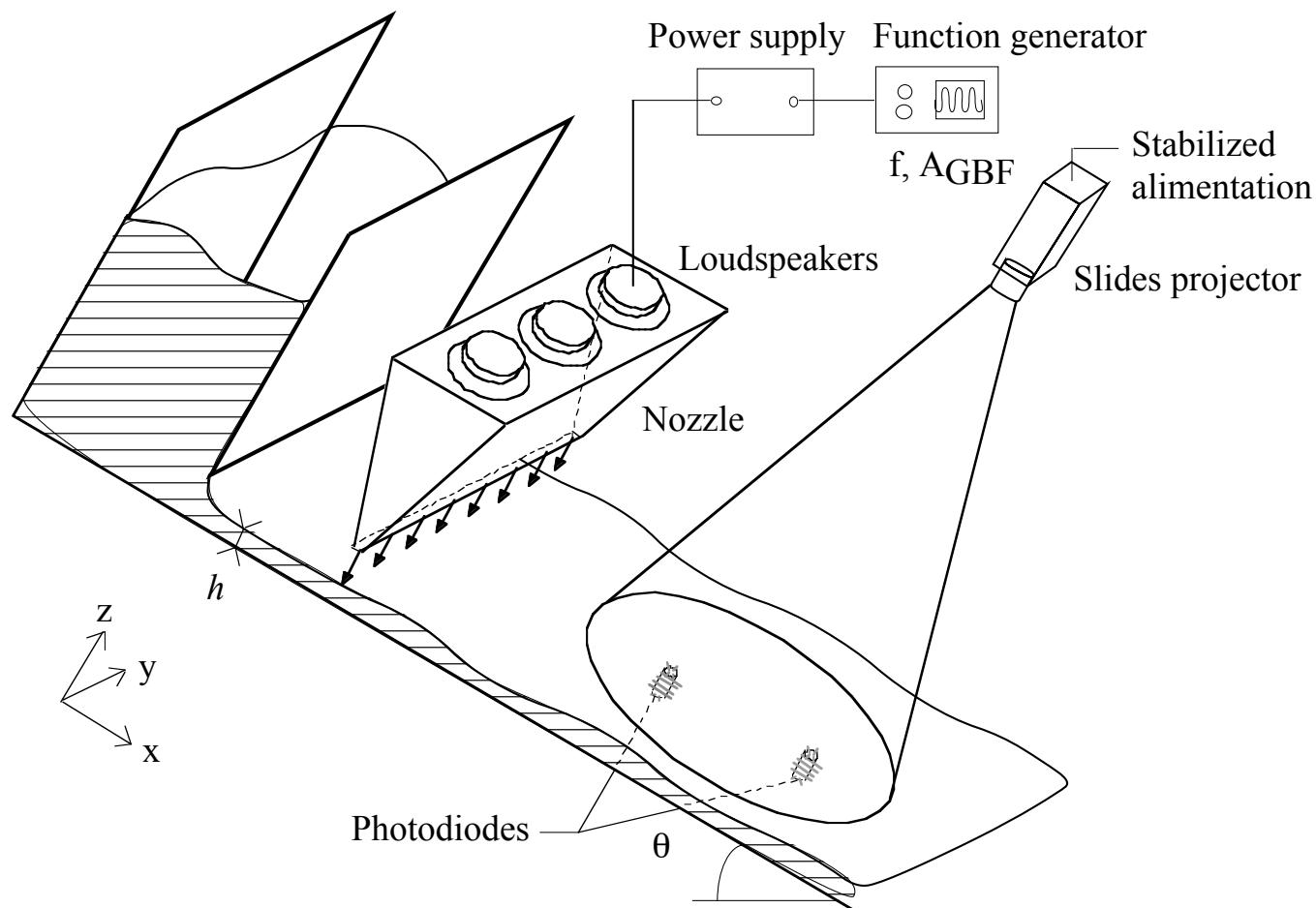


Long wave instability in granular flows

(Y. Forterre, JFM 06)

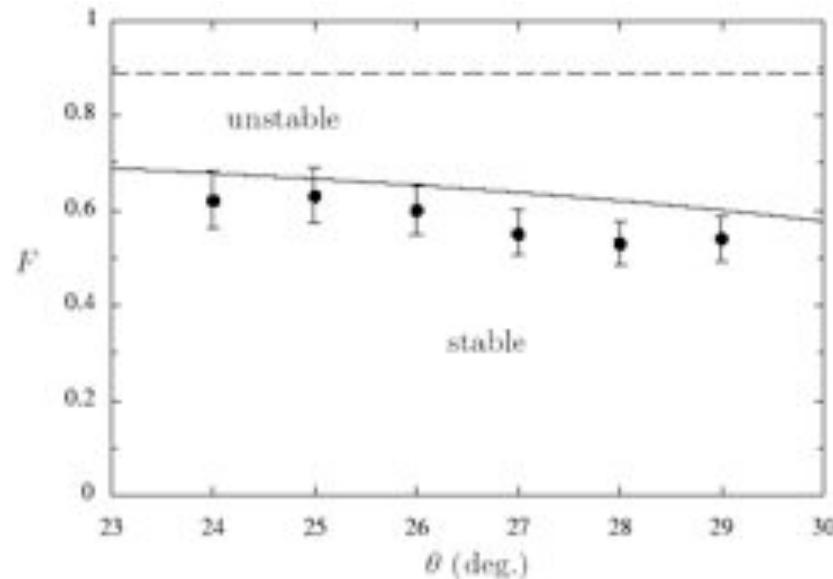


Experimental Setup : forcing of the instability

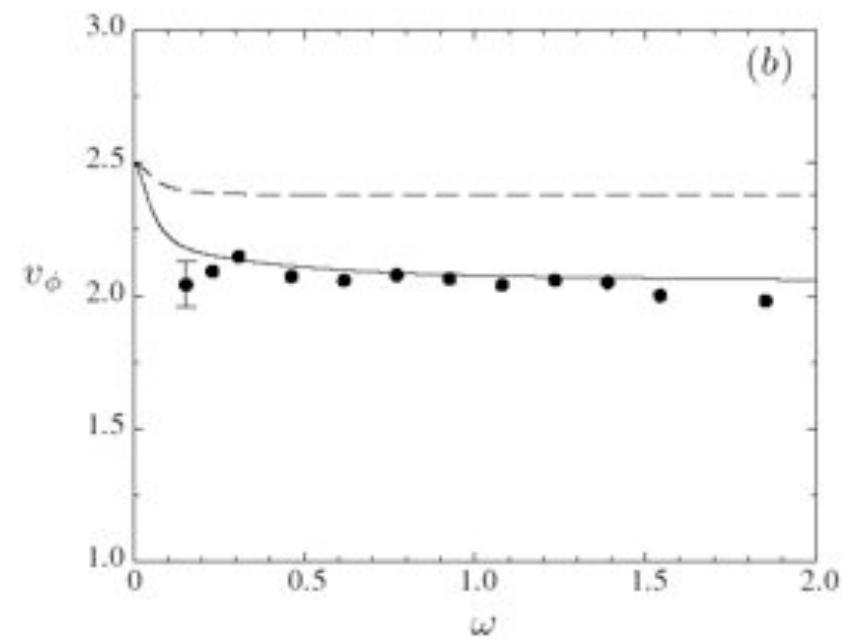
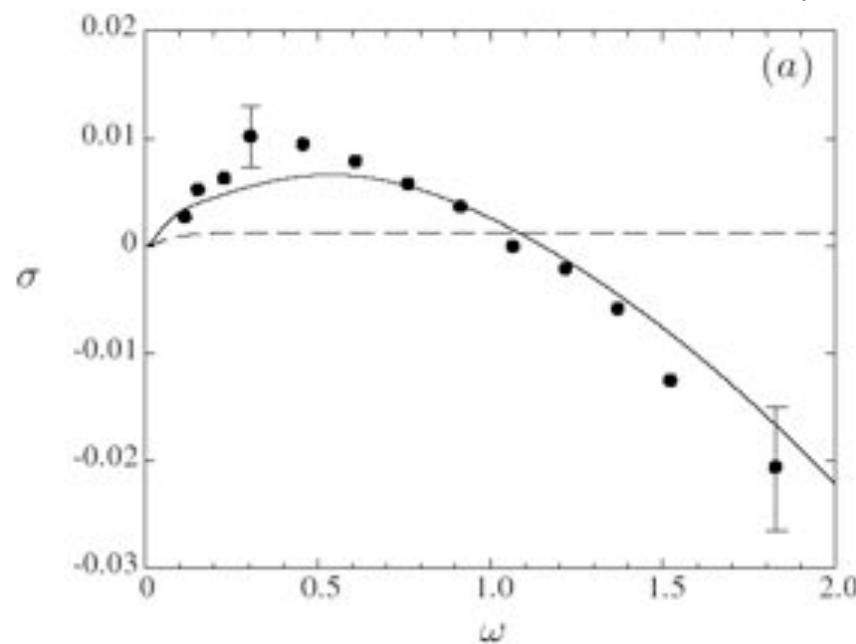


Instability threshold

Forsterre, JFM 06

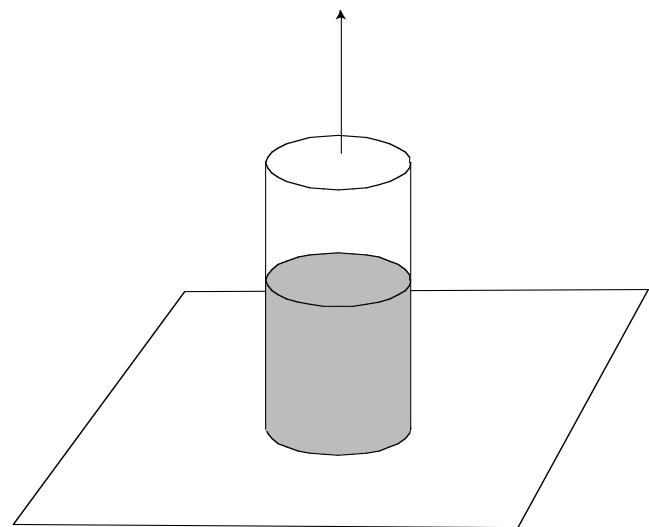


Dispersion relation



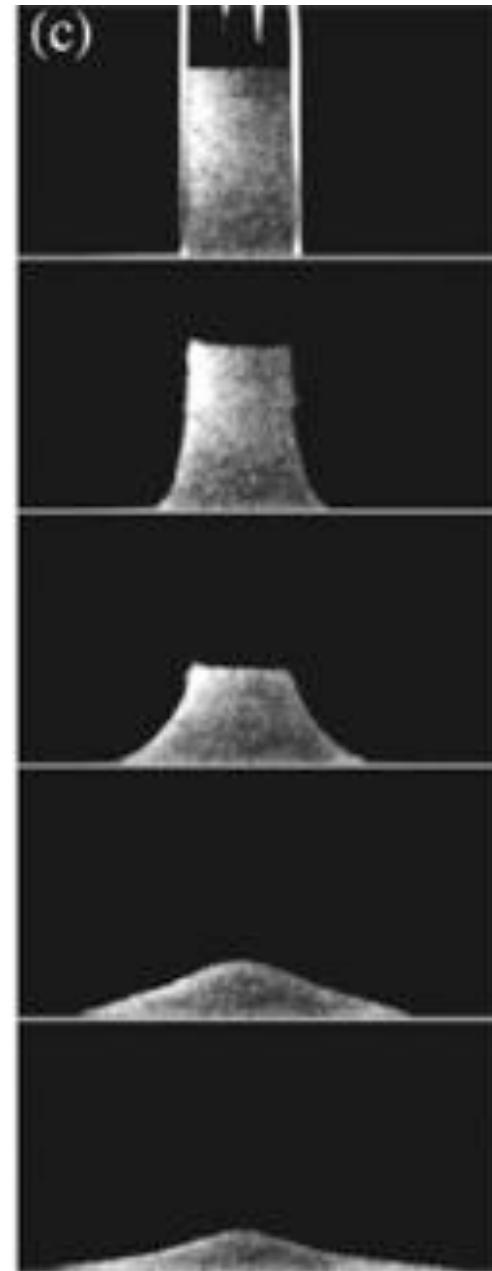
Granular slumping

(Lacaze and Kerswell 08)



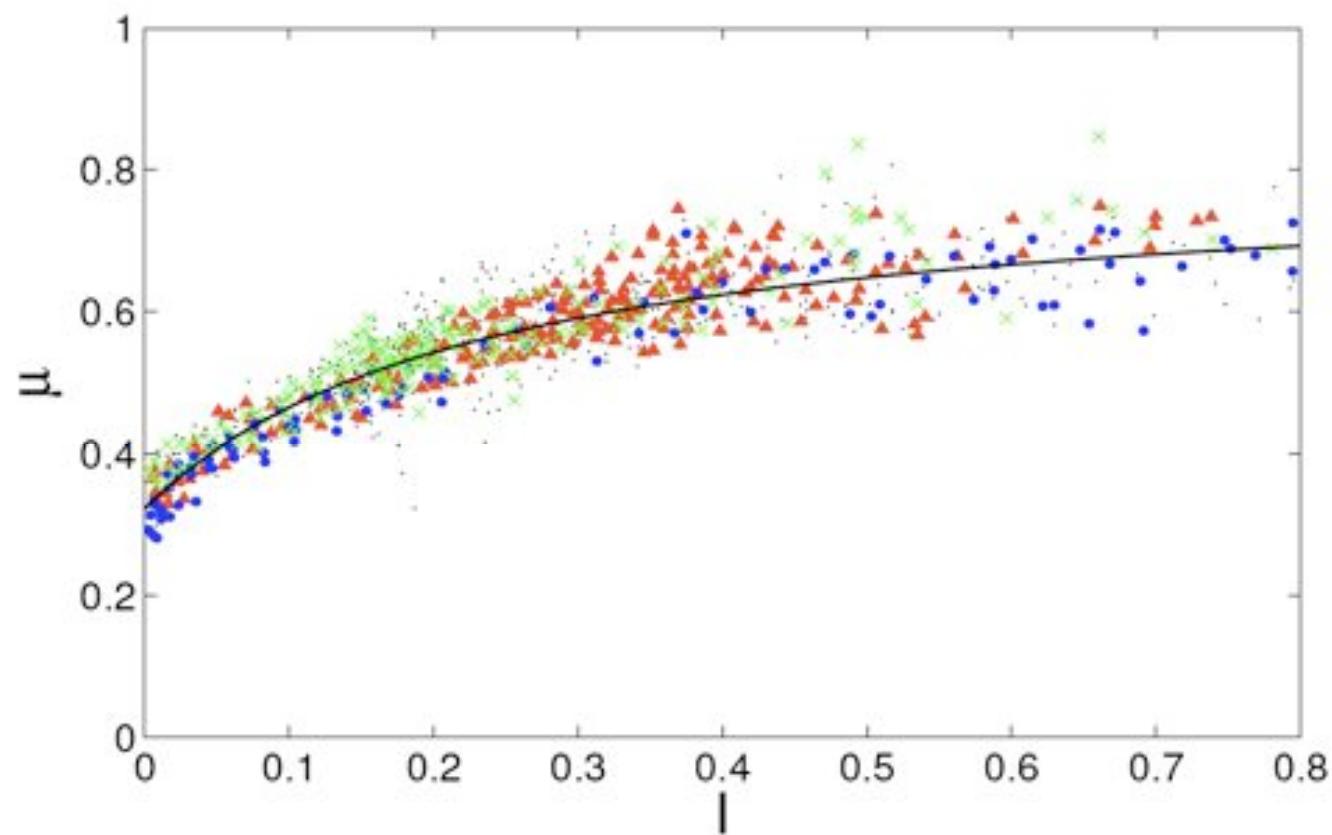
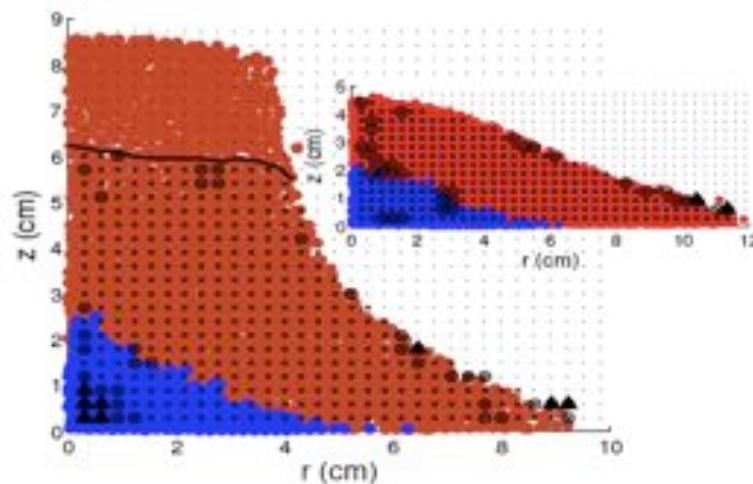
Lajeunesse et al Phys. Fluids 2004,2005
Lube et al JFM 2004,
Larrieu et al JFM 2006,
Staron & Hinch JFM 2005,
Lacaze et al Phys. Fluids 2008

...



Lajeunesse et al 05

Lacaze and Kerswell (preprint 08)



Relative Success of the visco-plastic description.

A starting point to address other configurations...
(simulating the pressure dependent visco-plastic rheology is non trivial...)

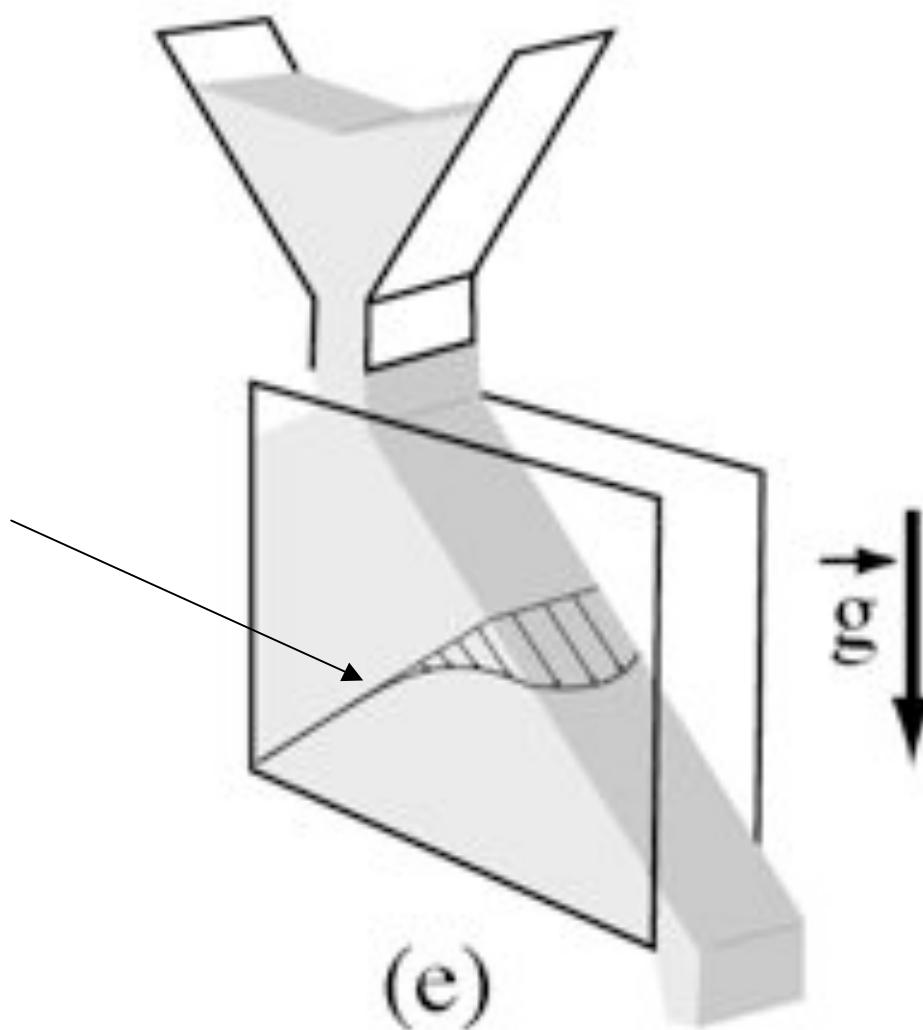
But there are problems when approaching the solid...

Limits of the viscoplastic approach:

- 1) Quasistatic flows (shear band, finite size effect....)
A need for non local approach...
- 2) Transient flows when preparation plays a crucial role

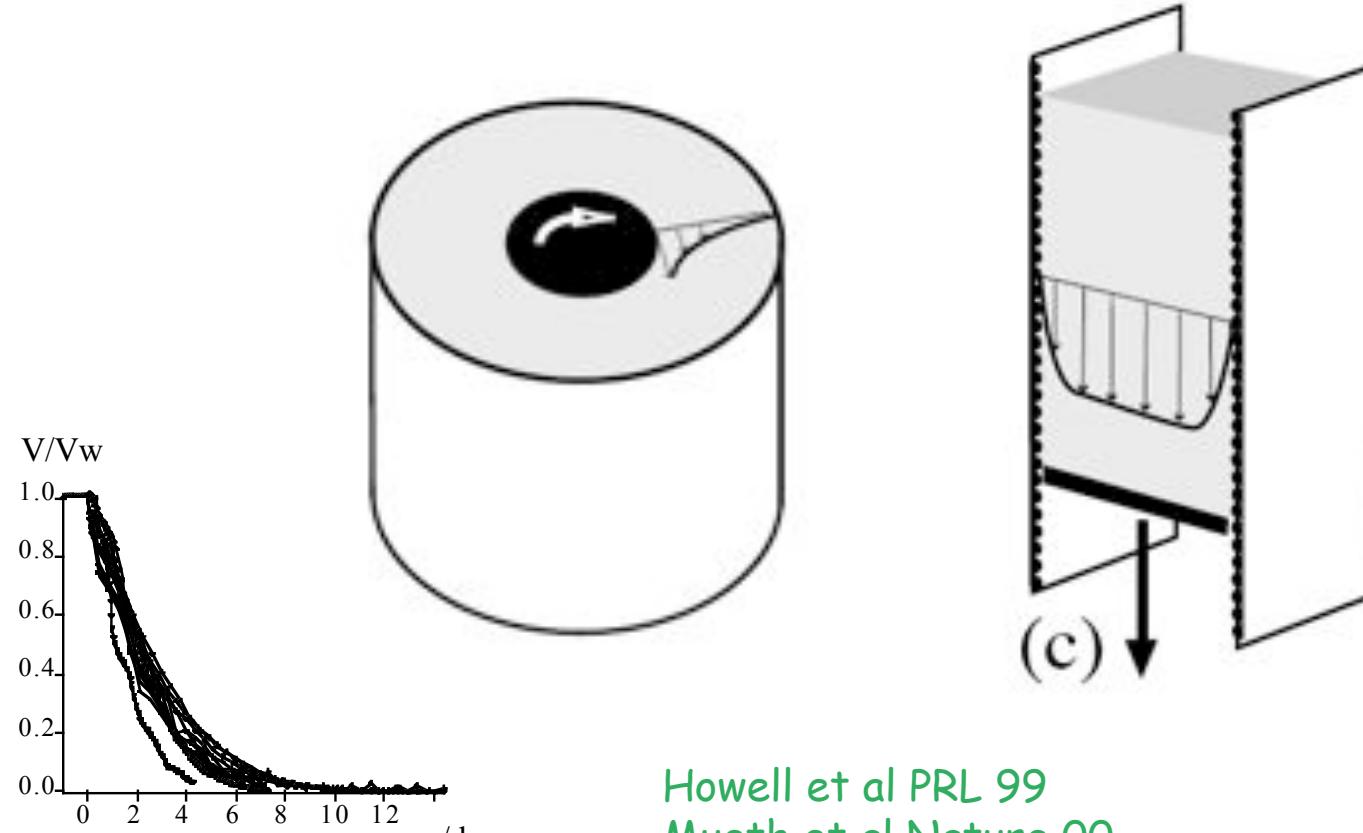
Velocity profile

Exponential tail
Not predicted..



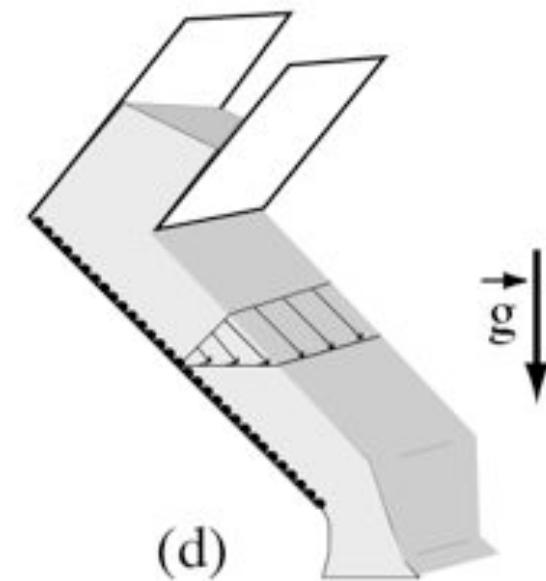
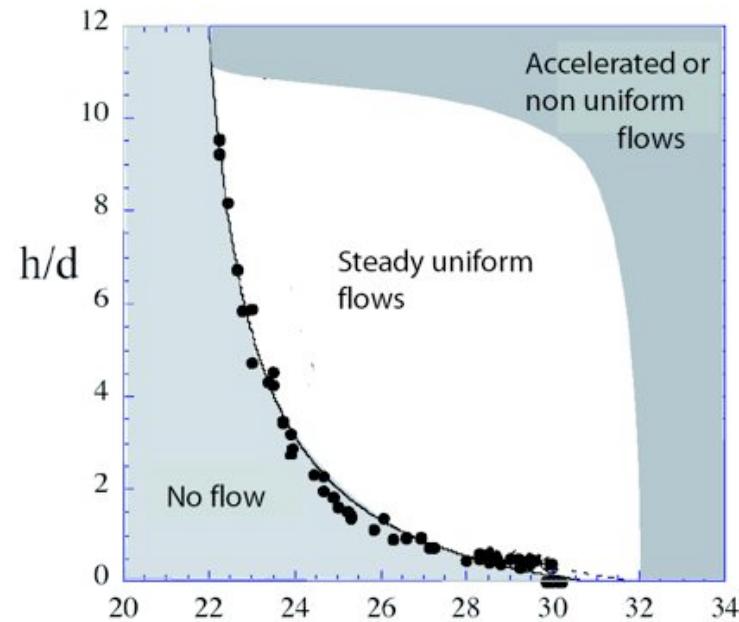
Shear bands in quasi-static flow

(Forterre & Pouliquen ARFM 08, Jop PRE 08)



Not captured by the viscoplastic approach

Flow threshold hysteresis Finite size effects



Not captured by the viscoplastic approach

Limit of a local rheology ?

to go further?

Role of the fluctuations ?

Aranson and Tsimring PRE,01,

Louge Phys. Fluids 03,

Josserand et al 06

Lemaitre 02

Bazant 07

Nott 08

Behringer 08...

Role of the correlations ?

Pouliquen et al 01,

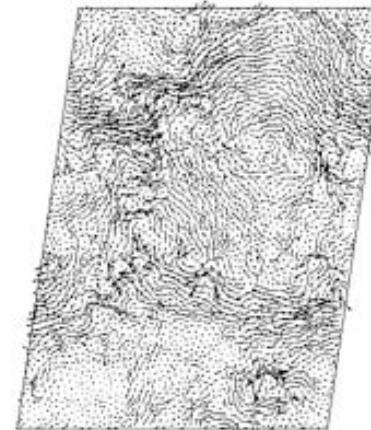
Ertas and Halsey 03,

Mills et al 08

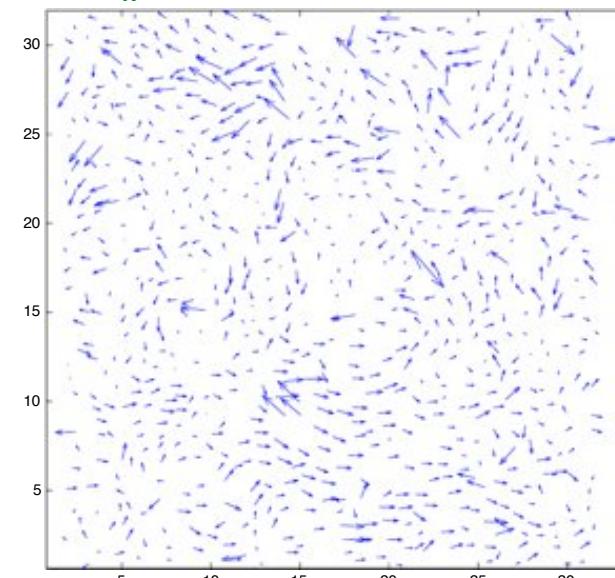
Jenkins and Chevoir 01,

Jenkins Phys. Fluids 06,

...



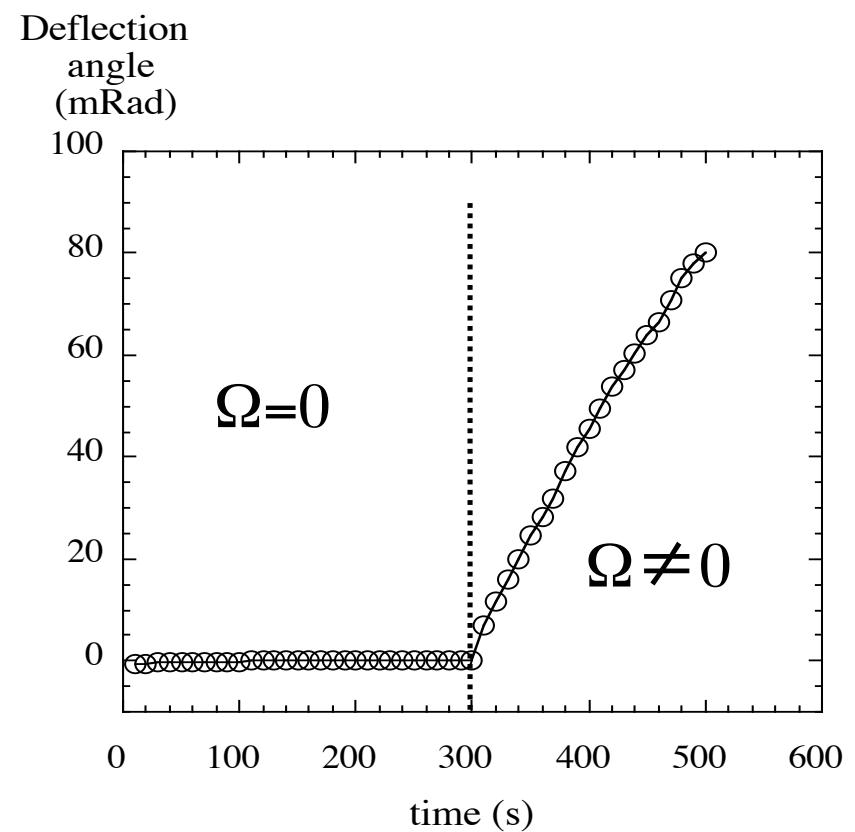
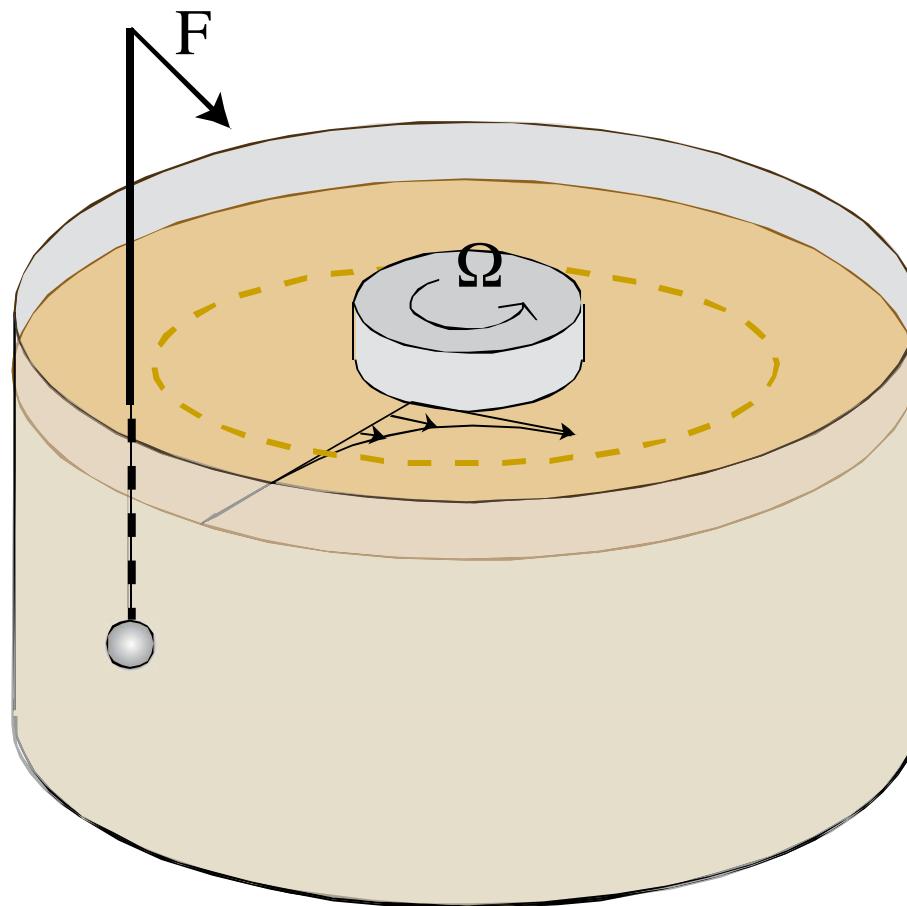
Radjai and Roux PRL 02



Pouliquen PRL 04

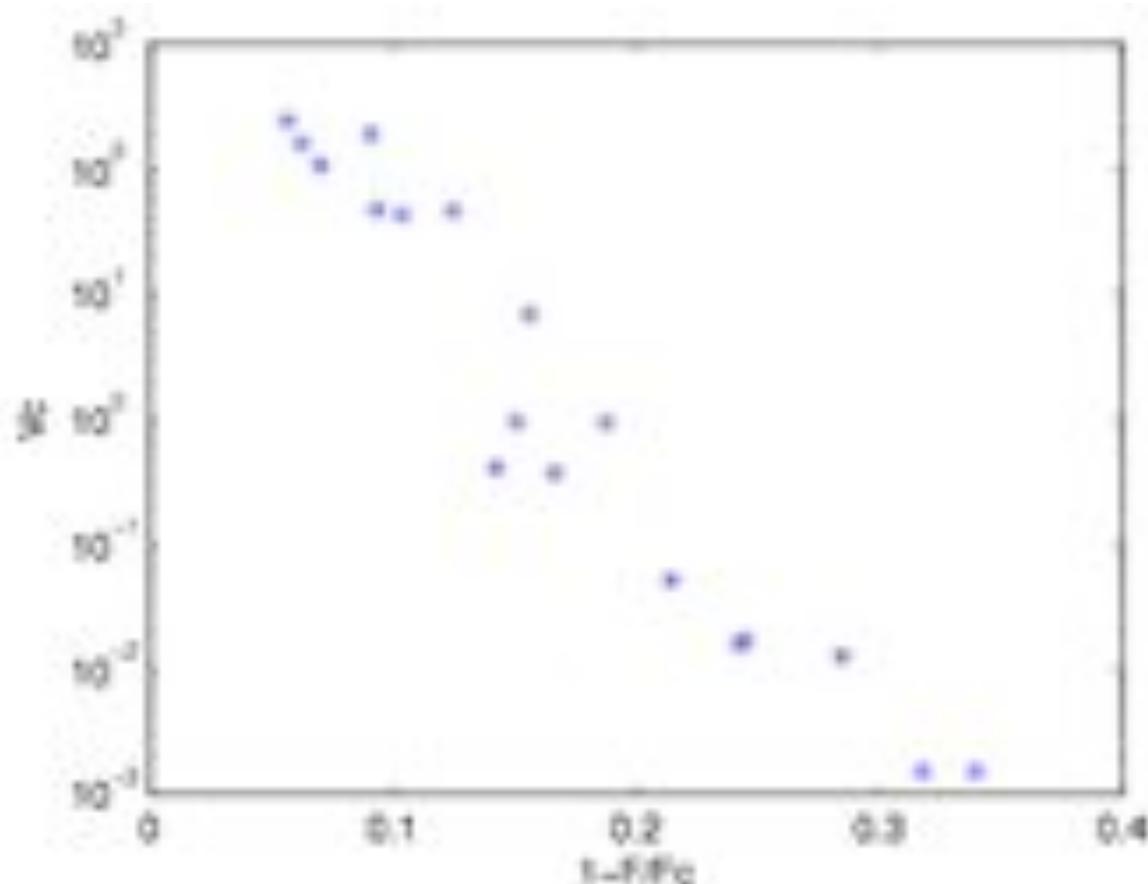
Link with plasticity of other amorphous and glassy systems

Evidence for non local effects: Microrheology experiments

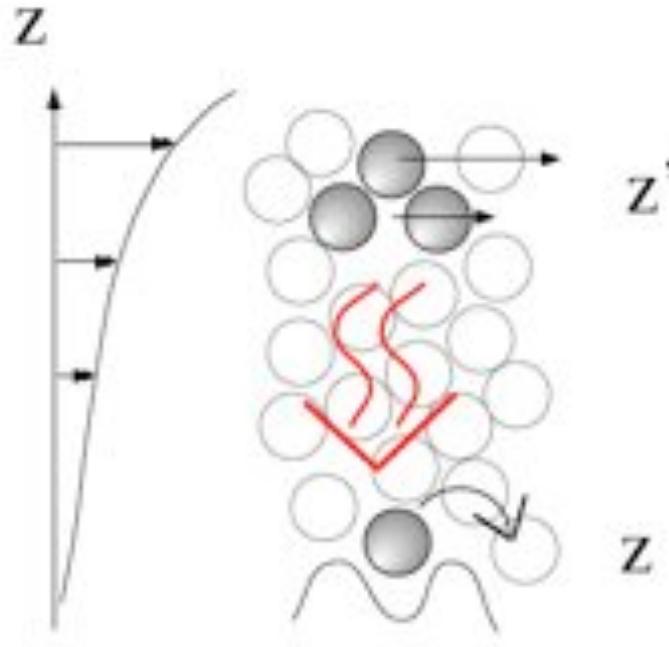


M. Van Hecke 2008
Pouliquen, Forterre, Nott

$$v_{creep} \propto \exp\left(\frac{F - F_c}{F_c}\right)$$

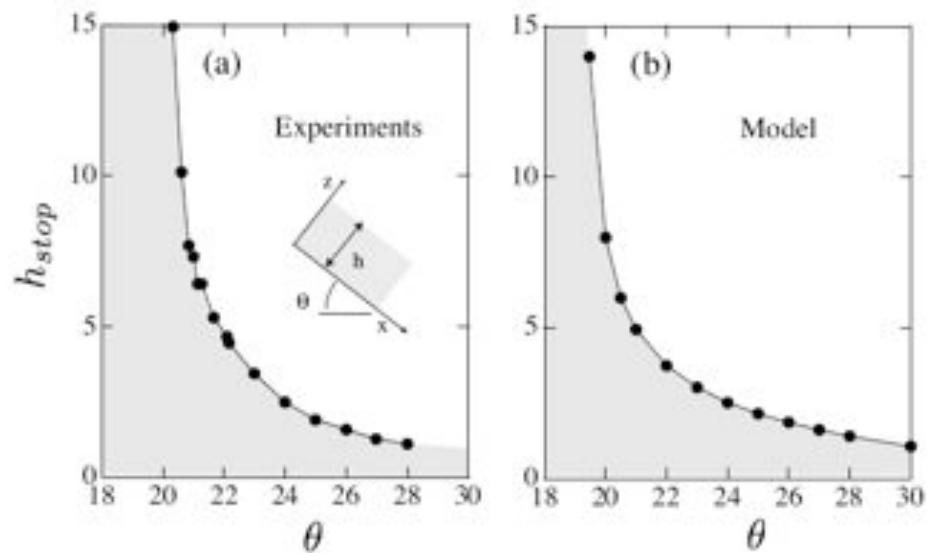
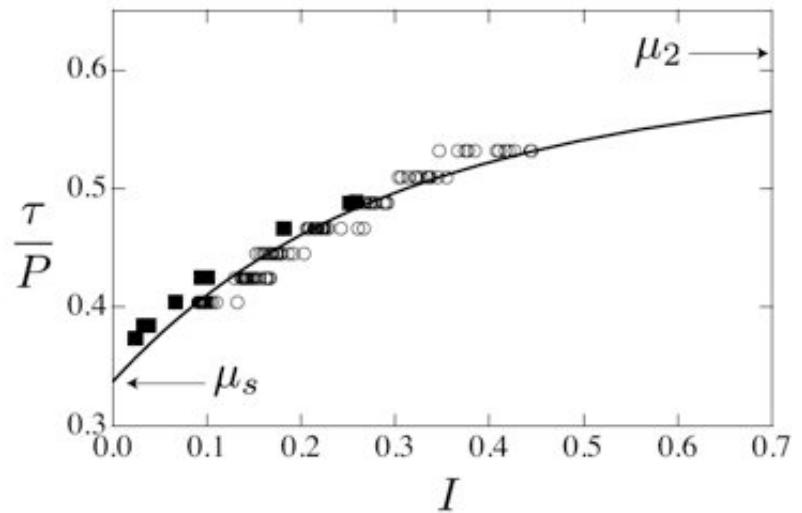


Self activated process



$$\dot{\gamma}(z) = \sum_{z'} f_{z' \rightarrow z} (p_{z' \rightarrow z}^+ - p_{z' \rightarrow z}^-),$$

$$f_{z' \rightarrow z} = |\dot{\gamma}(z')|$$



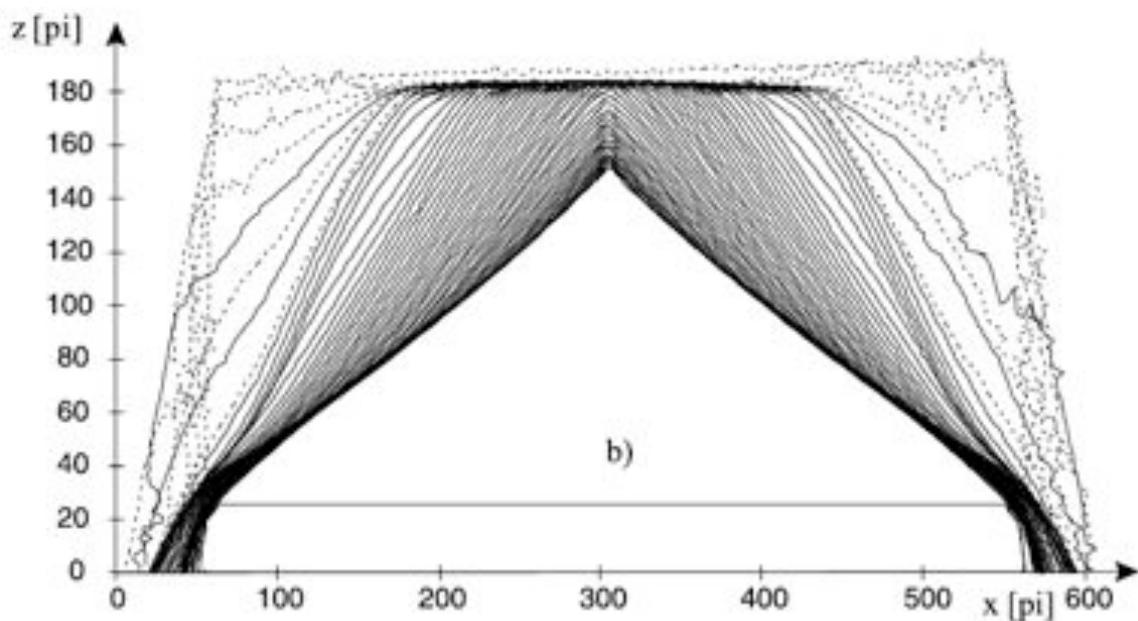
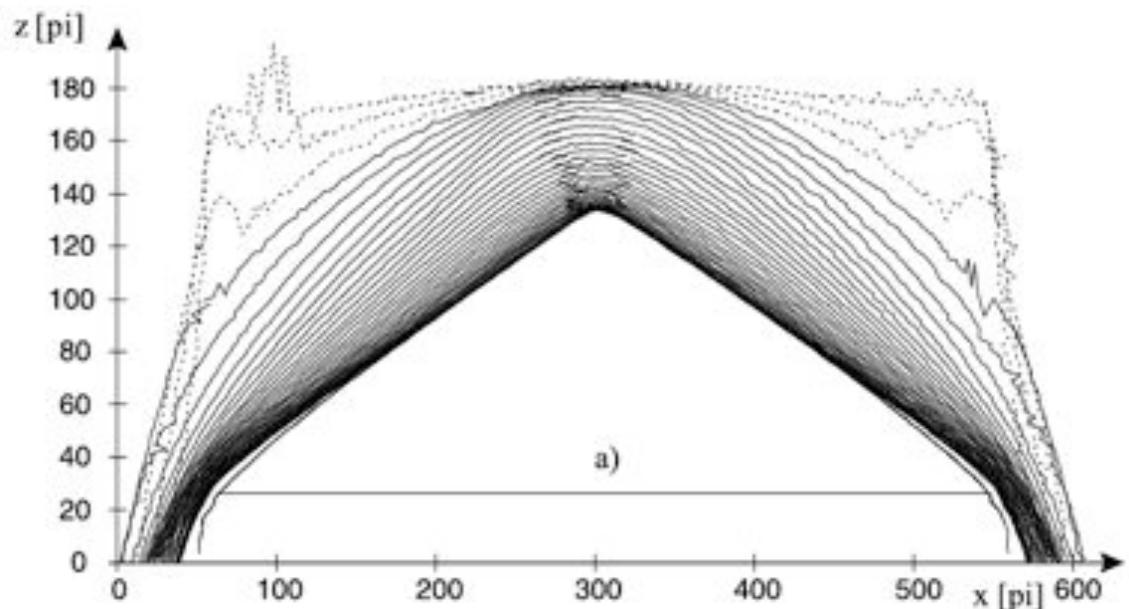
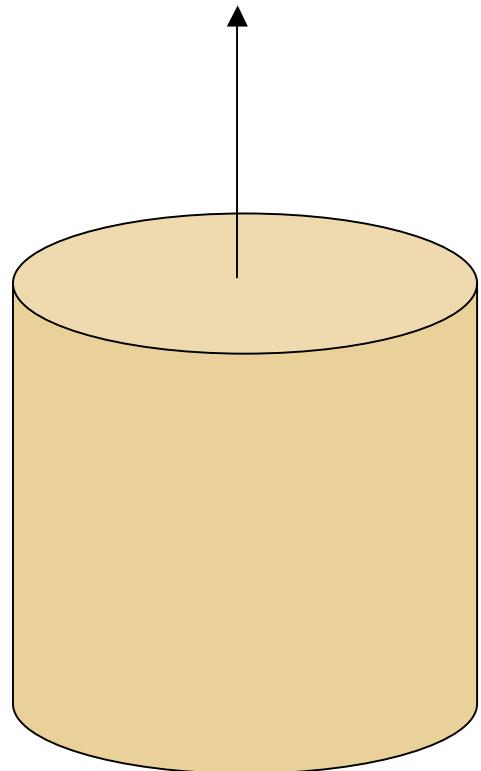
Pouliquen & Forterre, Phil. Trans, 2009

Limits of the viscoplastic approach:

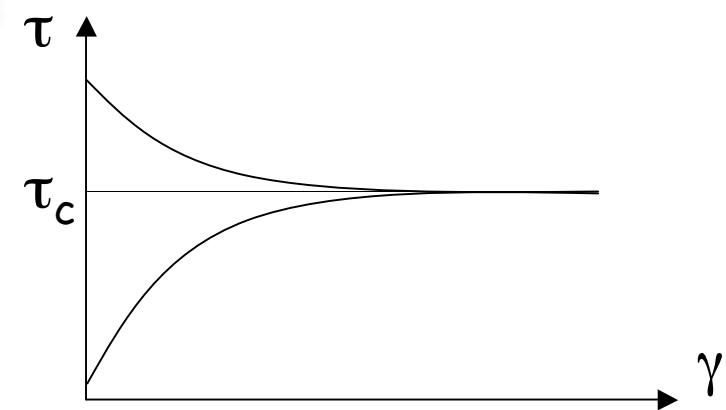
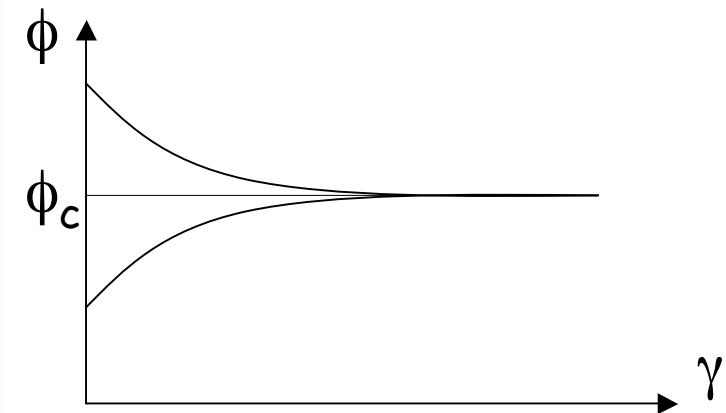
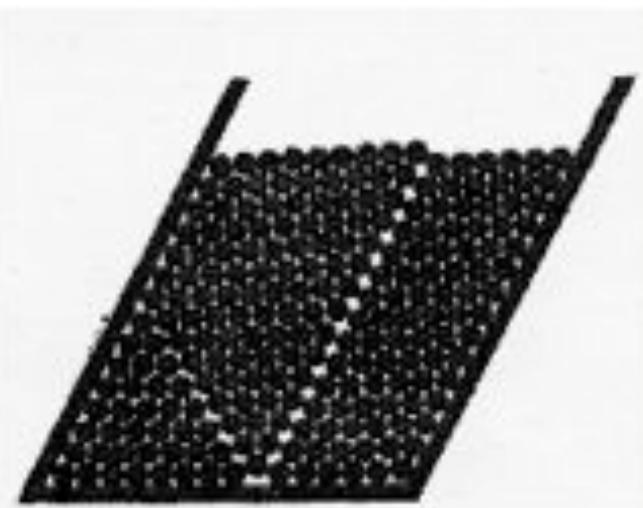
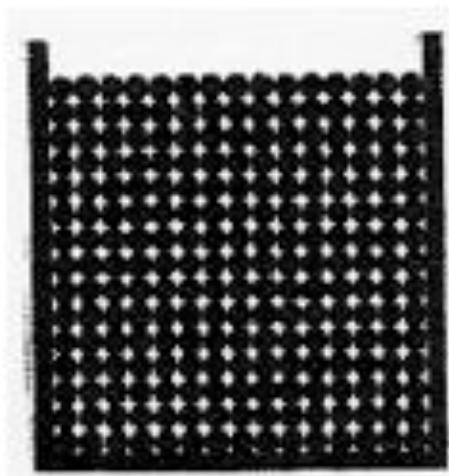
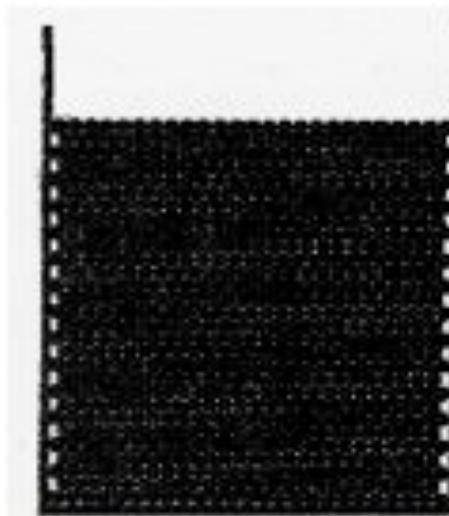
- 1) Quasistatic flows (shear band, finite size effect....)
A need for non local approach...
- 2) Transient flows when preparation plays a crucial role

Influence of the initial Volume fraction on the Collapse of a pile.

Daerr & Douady 99

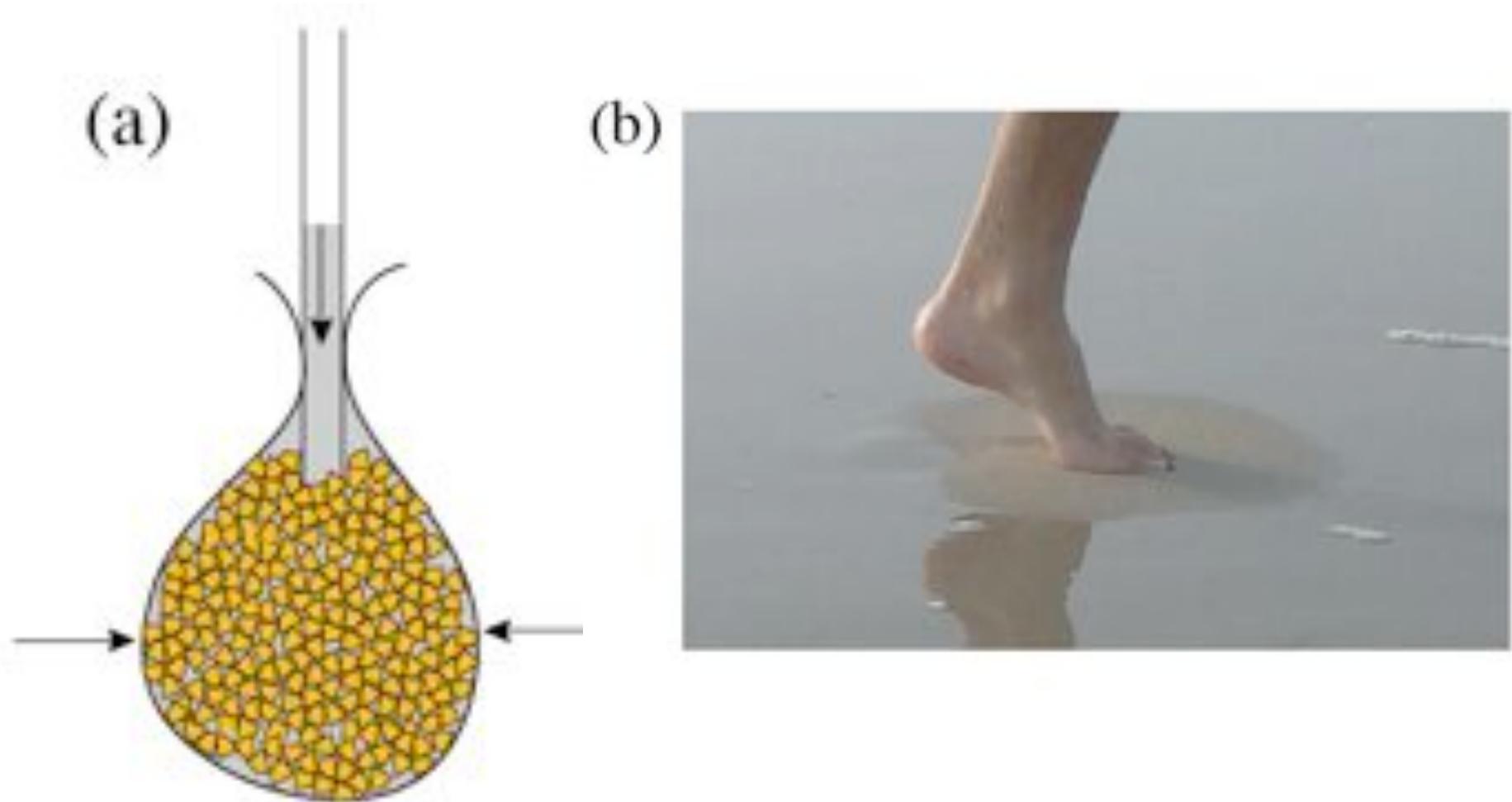


Quasi-static case : critical state theory

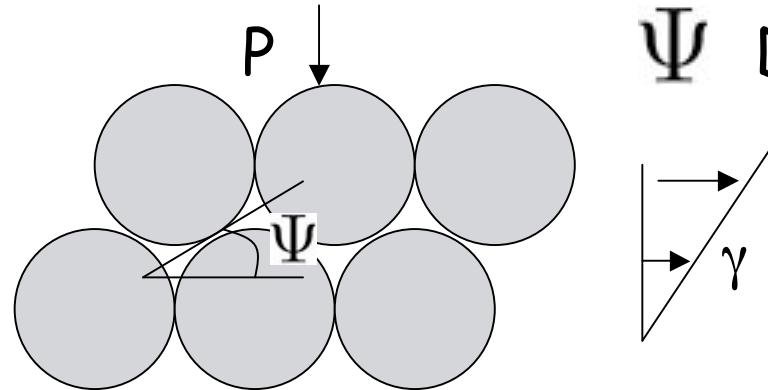


Coupling
Friction- dilatancy

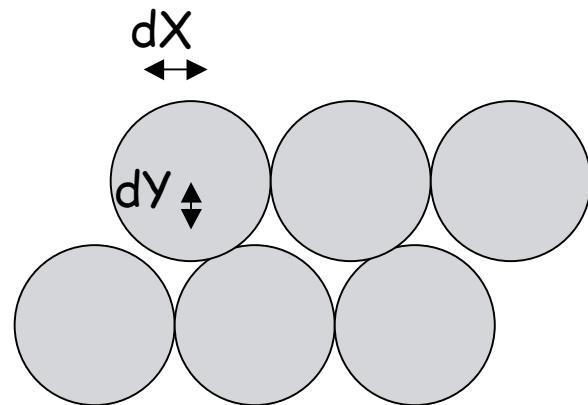
Reynolds Dilatancy



Simple critical state theory



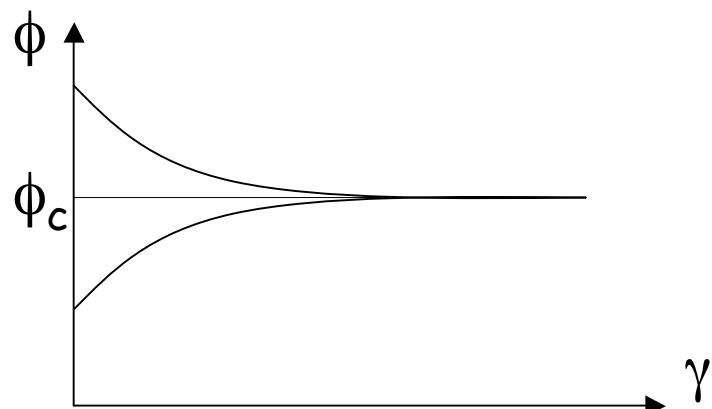
Ψ Dilatancy angle



$$\frac{dY}{dX} = -\frac{1}{\Phi} \frac{d\Phi}{d\gamma} = \tan \Psi$$

$$\tau = (\mu + \tan \Psi)P$$

assumption: \exists critical volume fraction ϕ_c

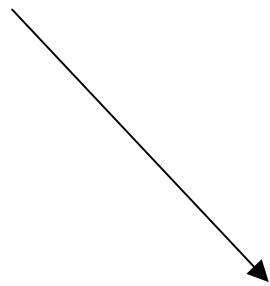


$$\tan \Psi = K(\Phi - \Phi_c)$$

(Radjai and Roux 98)

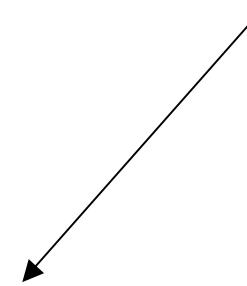
Visco plastic theory :

shear rate dependence
but no dilatancy



critical state theory :

dilatancy but
no shear rate
dependence



Shear rate dependent critical state theory

Shear rate dependent critical state theory :

$$\tau = (\mu(I) + \tan \Psi) P$$

$$\tan \Psi = K(\Phi - \Phi_{eq}(I))$$

$$\frac{1}{\Phi} \frac{d\Phi}{dt} = \dot{\gamma} \tan \Psi$$

$$I = \frac{\dot{\gamma} d}{\sqrt{P/\rho}}$$

3D generalisation :

$$\dot{\tilde{\gamma}}_{ij} = \dot{\gamma}_{ij} - \frac{1}{3} \delta_{ij} \dot{\gamma}_{kk}$$

$$I = \frac{\|\dot{\tilde{\gamma}}\| d}{\sqrt{P/\rho_s}}$$

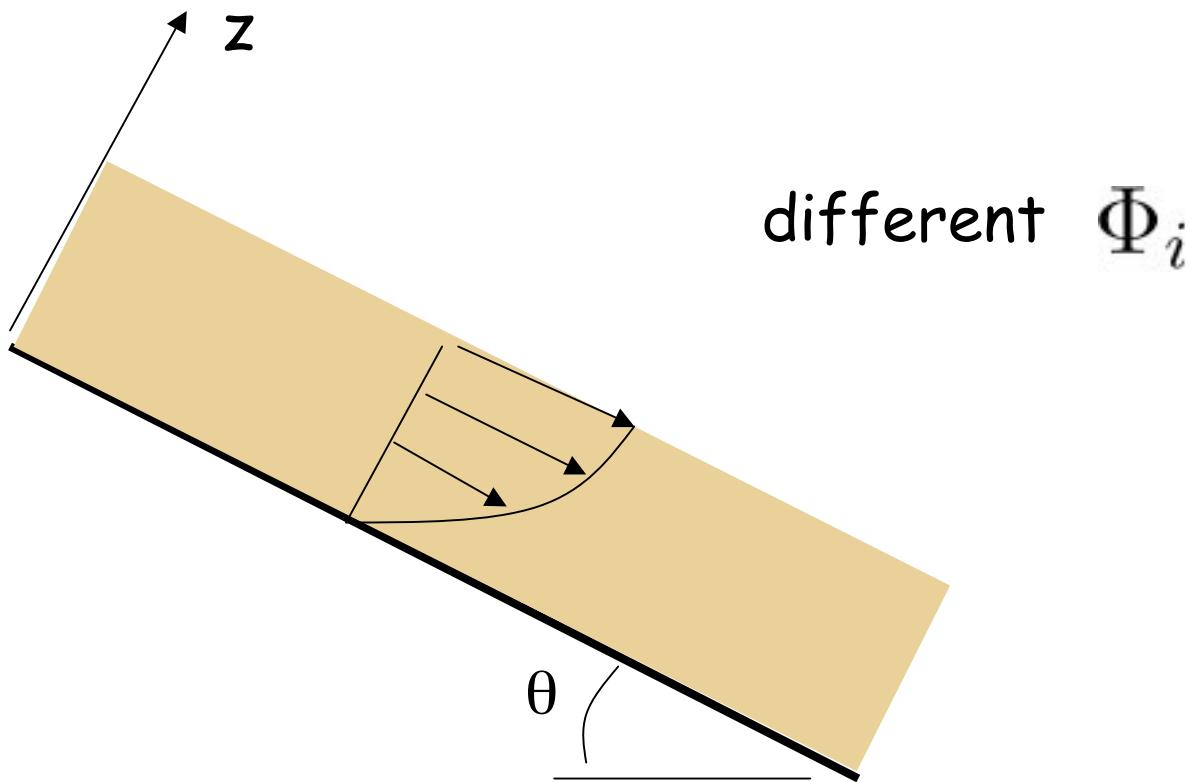
$$\tan \psi = K(\Phi - \Phi_c(I))$$

$$\tau_{ij} = (\mu(I) + \tan \Psi) \frac{\dot{\tilde{\gamma}}_{ij}}{\|\dot{\tilde{\gamma}}\|}$$

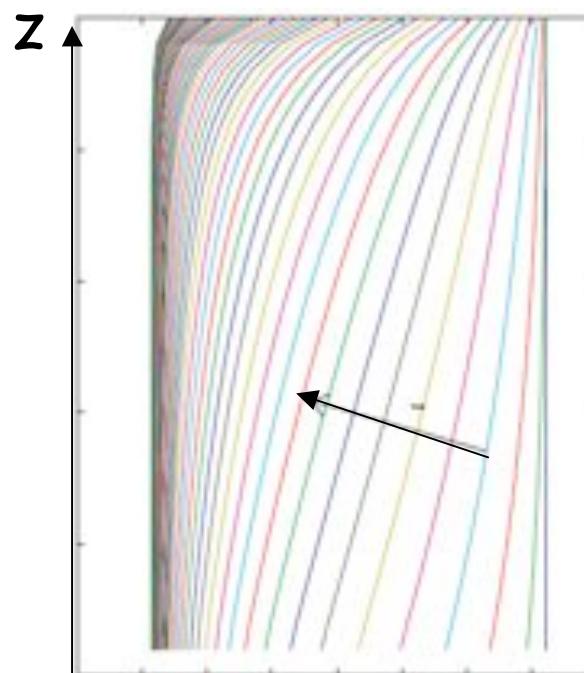
$$\frac{\partial u_i}{\partial x_i} = \tan \Psi \|\dot{\tilde{\gamma}}\|$$

Application to a dry flow:

Initiation of flow on an inclined plane:

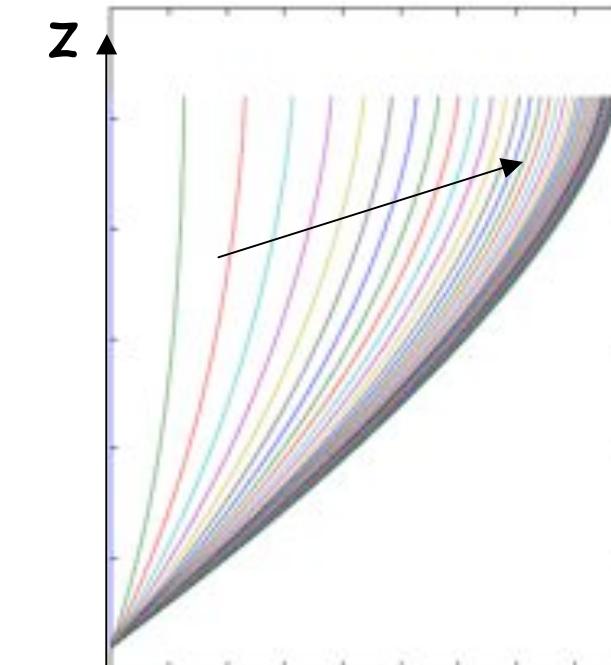
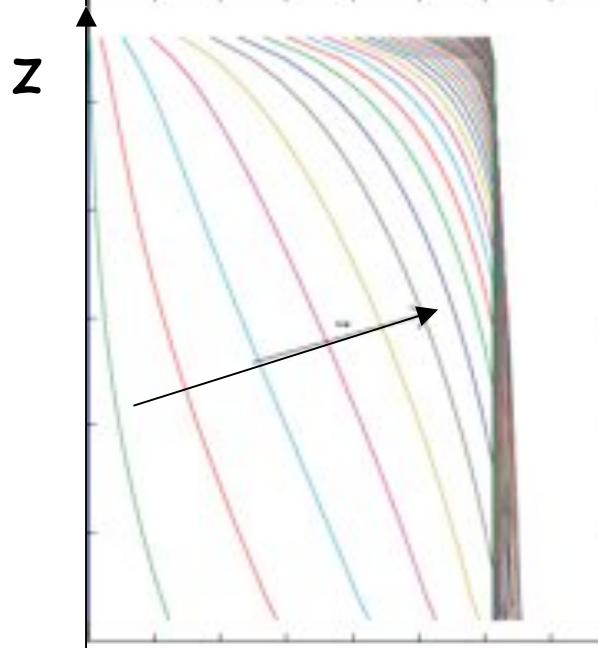


Initially
dense



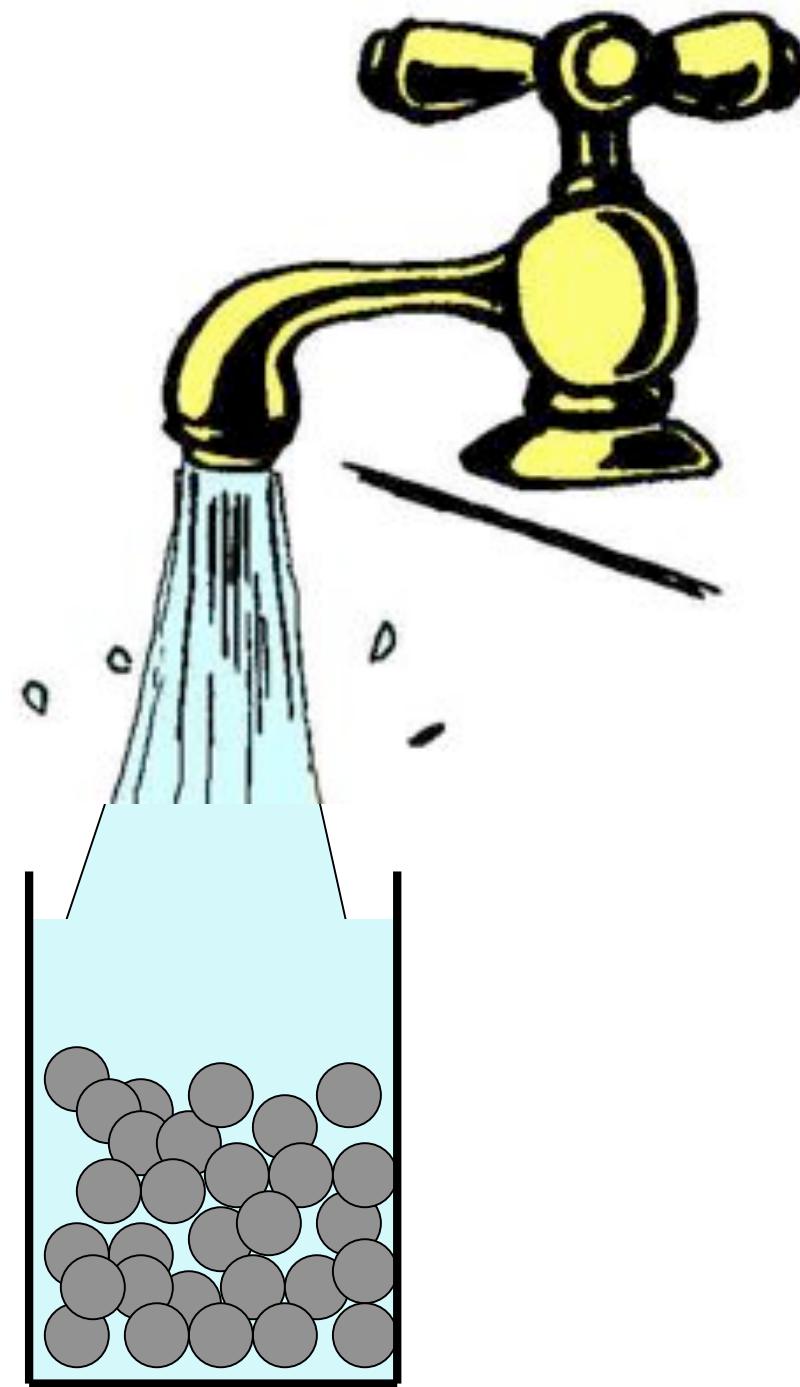
ϕ

Initially
loose

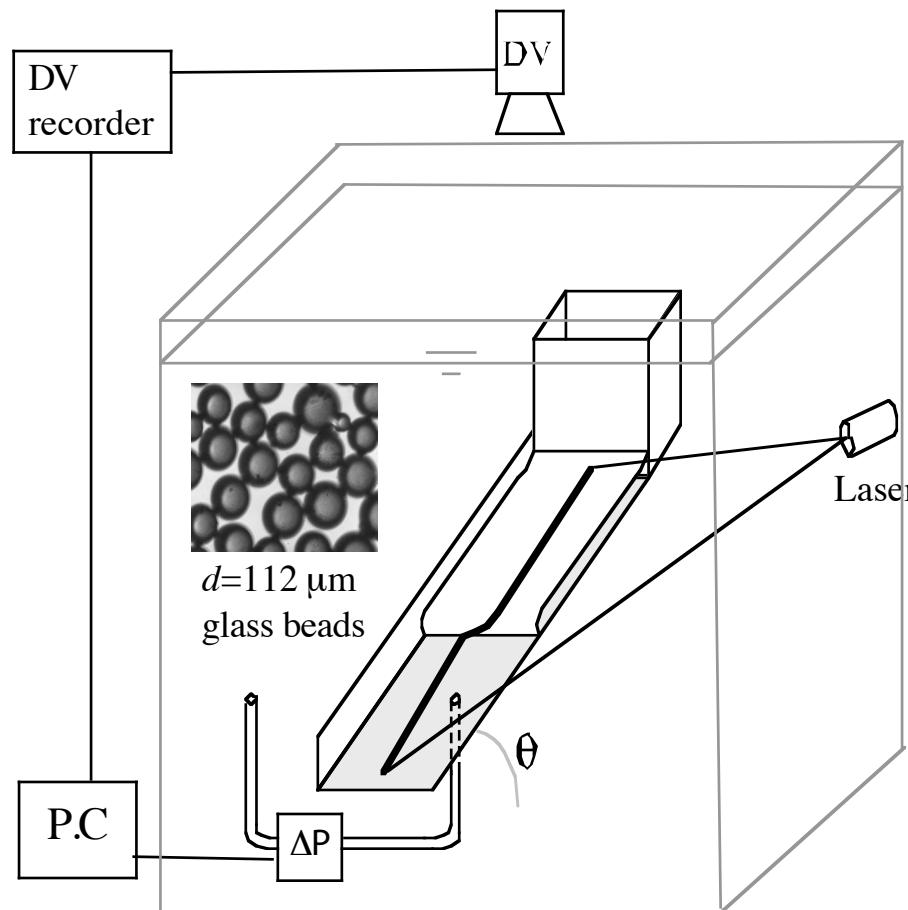


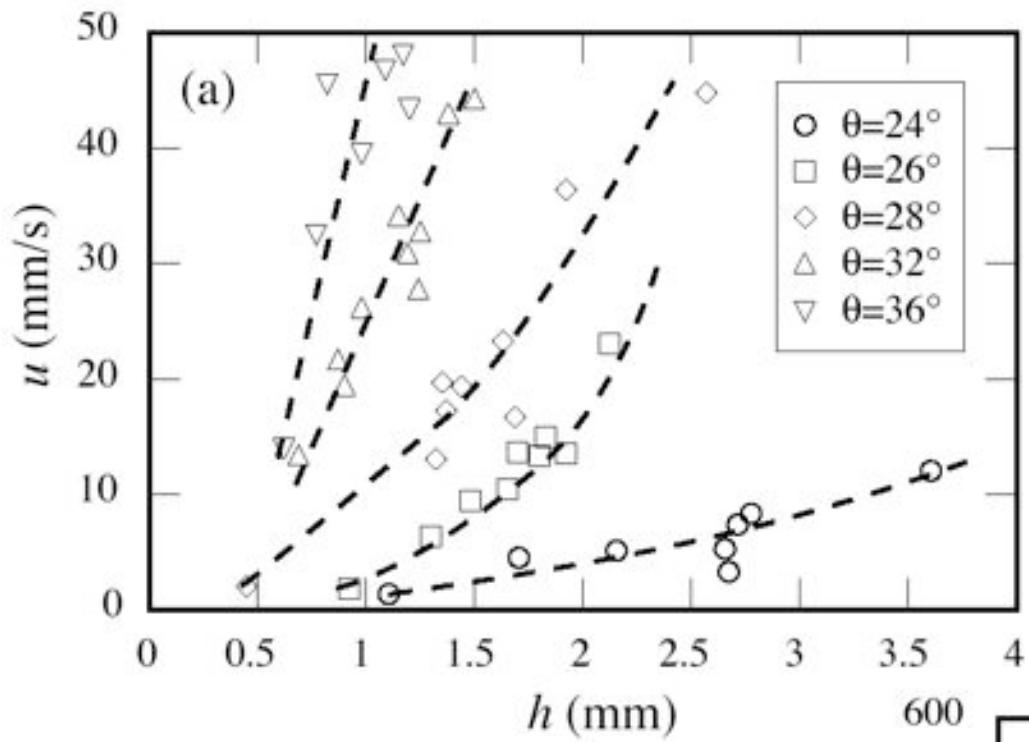
u

Comparison with DEM simulations with N. Taberlet...



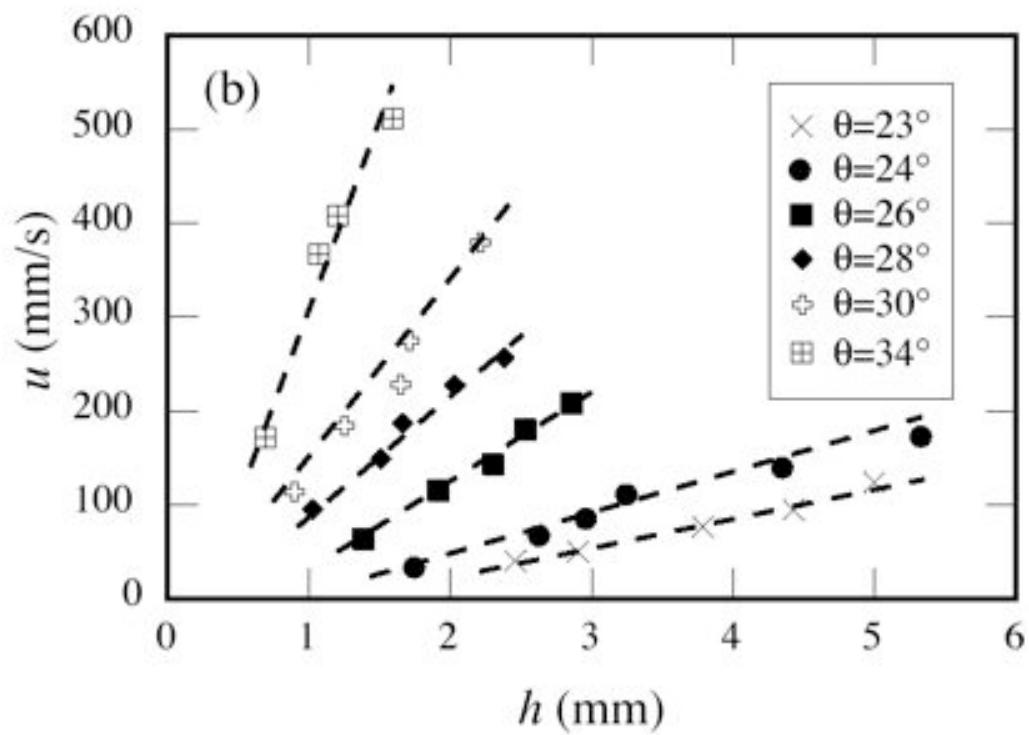
Changing time scales...
by putting the granular material in water
(Cassar et al, Phys. Fluids 06)





Immersed

Dry

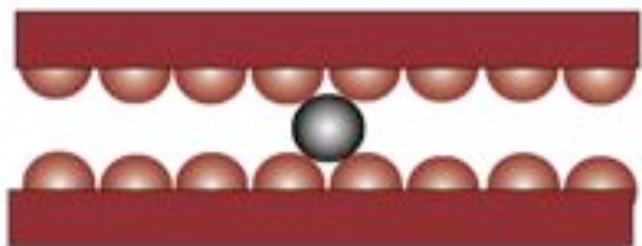


A naive idea :

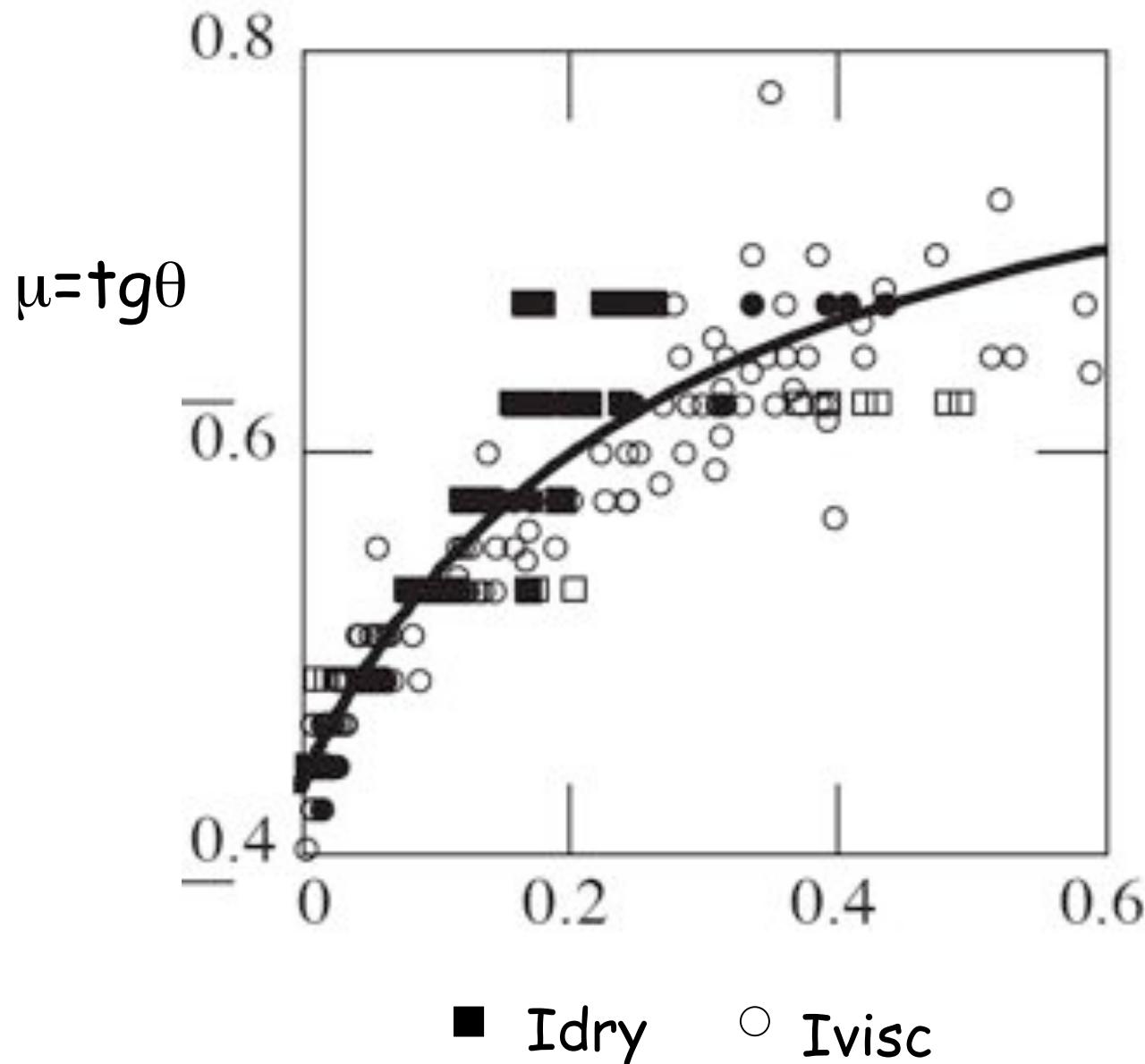
fluid only plays a role by changing the time scale
of rearrangements

$$\tau = P \mu(I) \quad \text{with} \quad I = \dot{\gamma} t_{\text{micro}}$$

viscous : $t_{\text{micro}} = \frac{\eta_f}{P}$



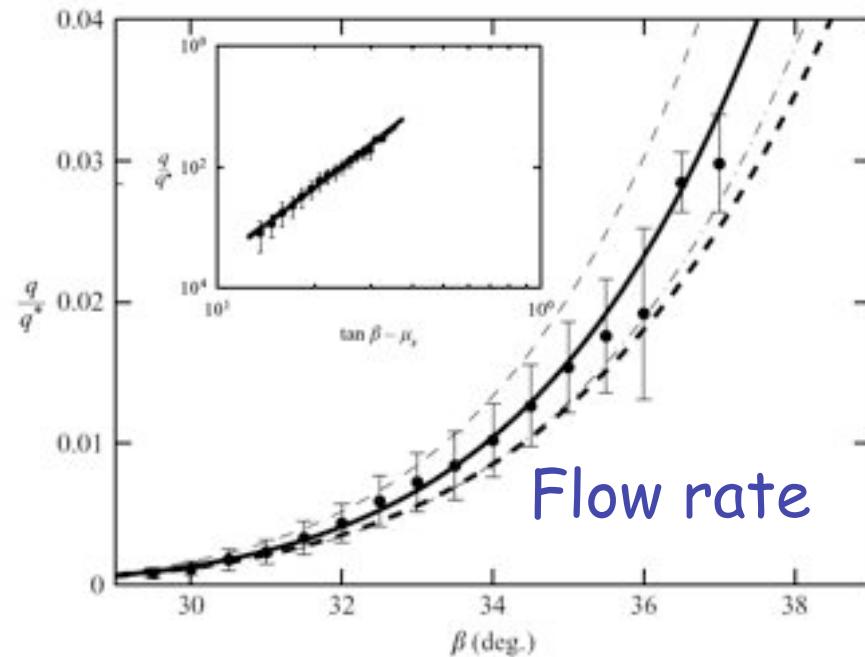
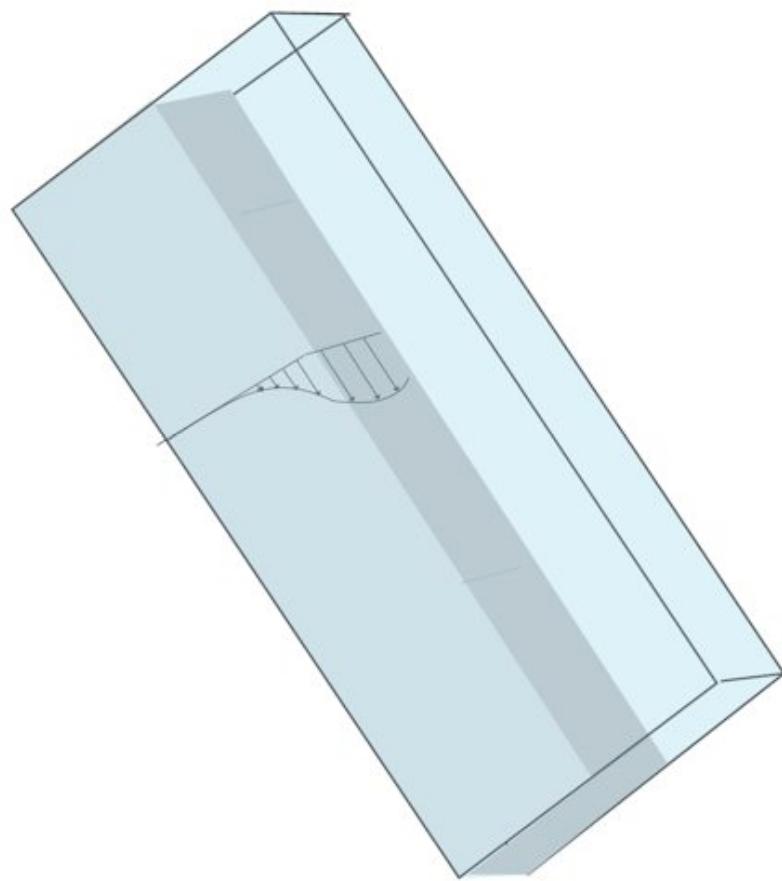
dry : $t_{\text{micro}} = \frac{d}{\sqrt{P/\rho_s}}$



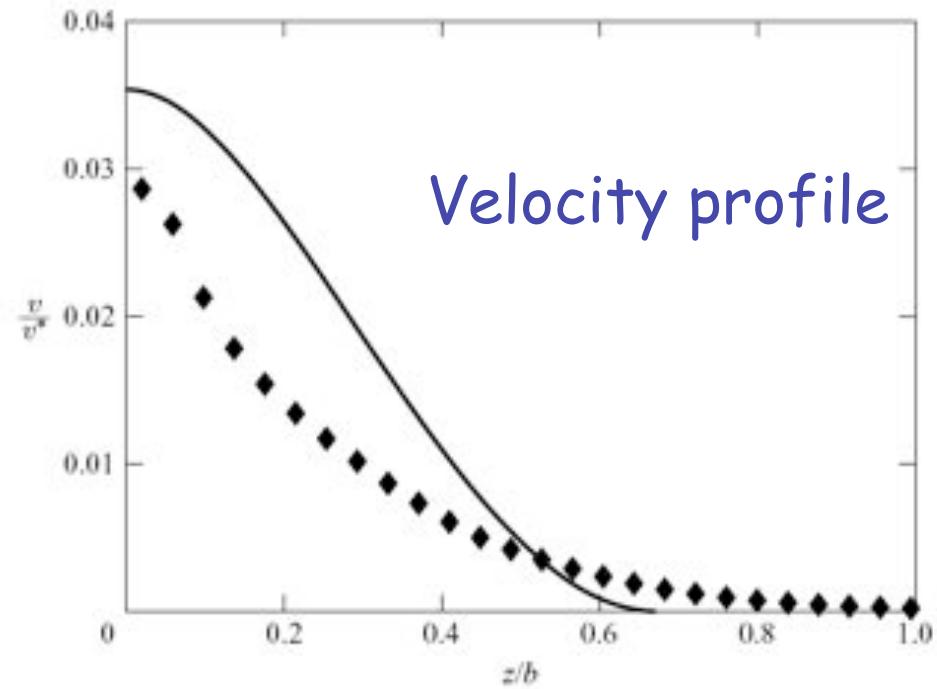
Cassar et al. Phys. Fluids 05

Submarine flows on heap

Doppler et al, JFM 07



Flow rate



Velocity profile

And dilatancy ???

And Pore pressure ??

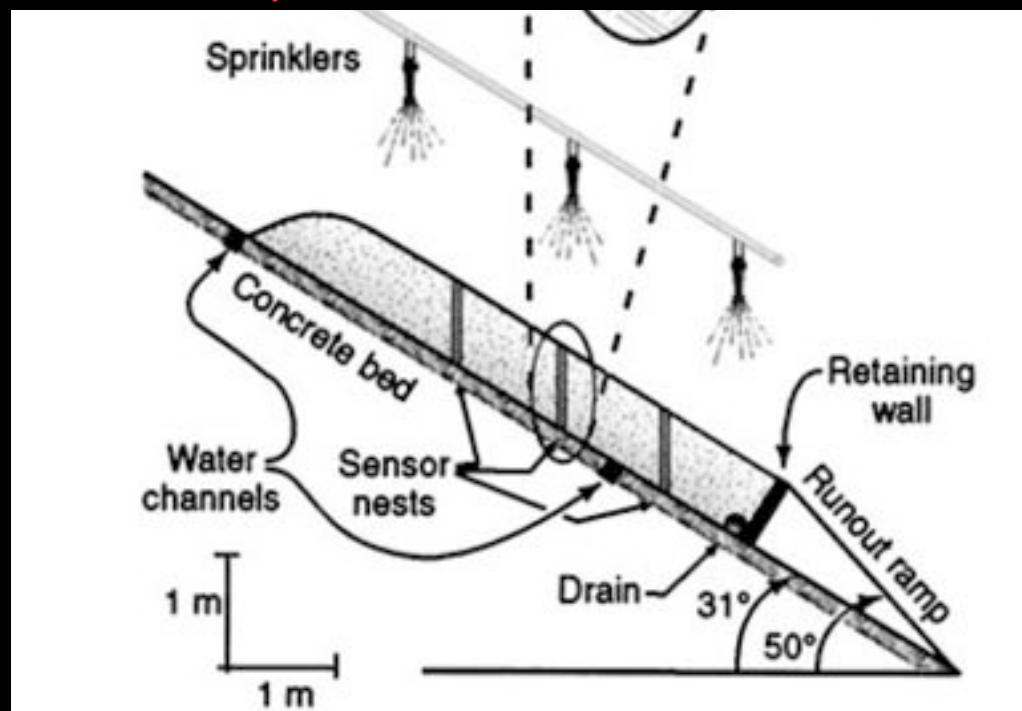
Cf In Faults

Rice JGR 75, Rudnicki JGR 84, ...

How to explain the variety of landslides observed in nature ?

Iverson et al , (2000) Science

Large scale experiments in the USGS facility



Dense preparation

Courtesy of Dick Iverson



12:25 PM
JUN. 17, 1999

Loose preparation

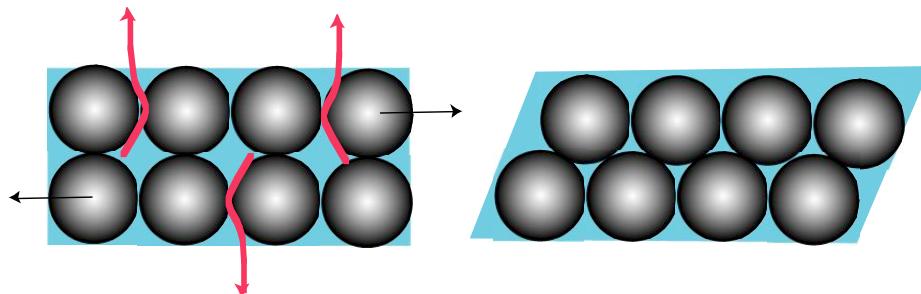
Courtesy of Dick Iverson



Pore Pressure feedback argument

(Iverson Rev. Geo. 97, JGR 05)

Loose case



$$\Phi \nearrow$$

⇒ Fluid expelled

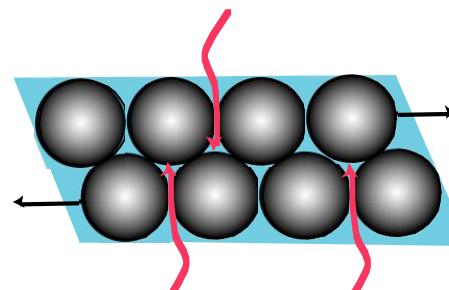
$$\Rightarrow P_{\text{fluid}} \nearrow$$

$$\Rightarrow P_{\text{eff}} \searrow$$

⇒ Friction ↓

⇒ Less friction
between grains

Dense case



$$\Phi \searrow$$

⇒ Fluid sucked

$$\Rightarrow P_{\text{fluid}} \searrow$$

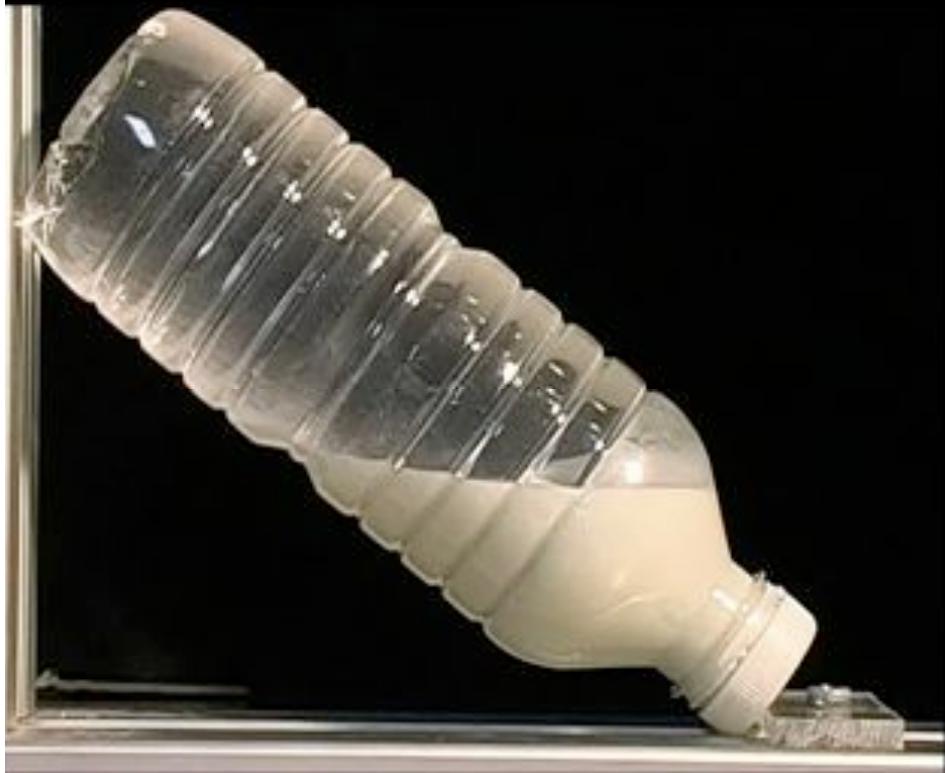
$$\Rightarrow P_{\text{eff}} \nearrow$$

⇒ Friction ↑

⇒ higher friction
between grains

In faults: rice JGR 75, Rudnicki JGR 84, ...

A simple experiment:



Dense sample



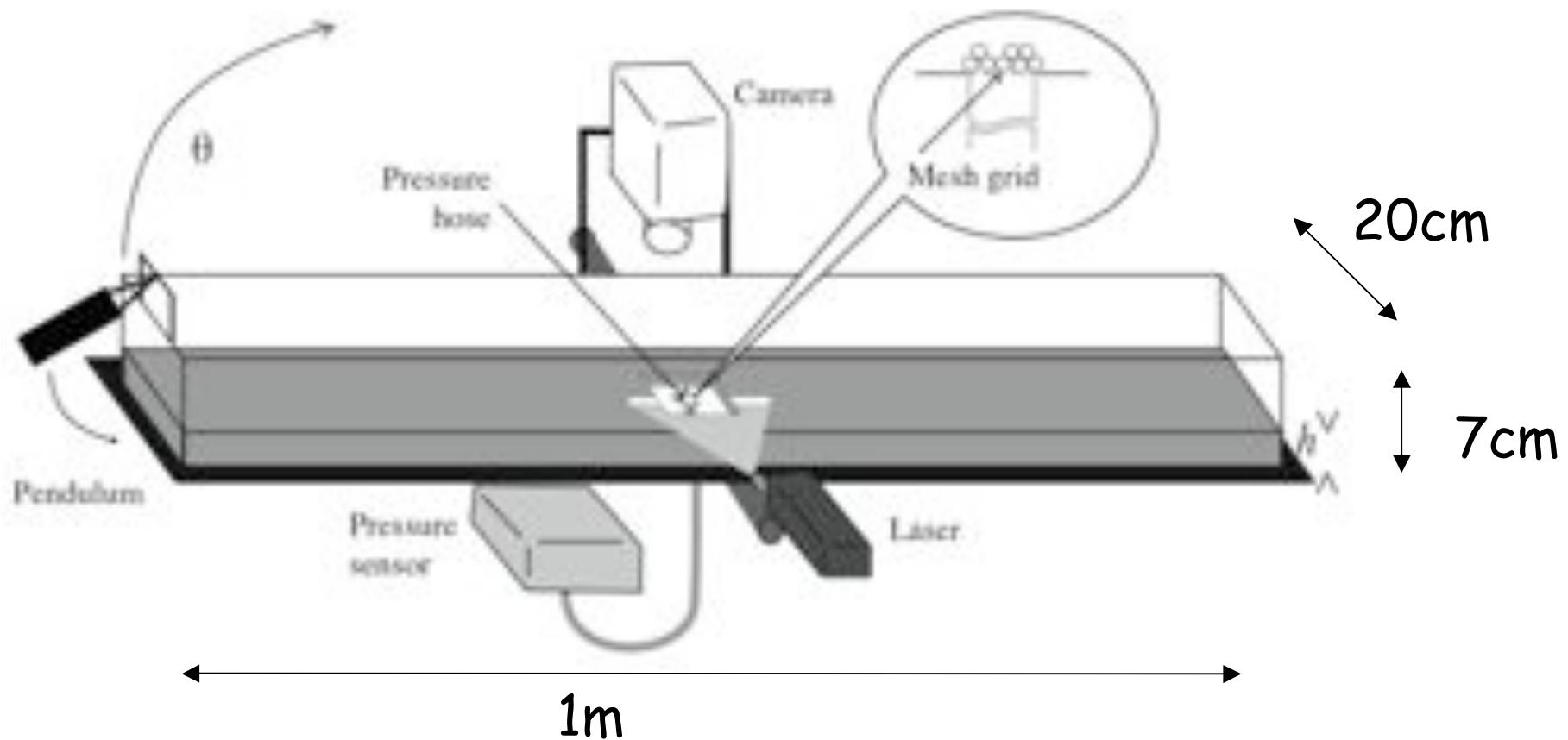
Loose sample

Experimental setup

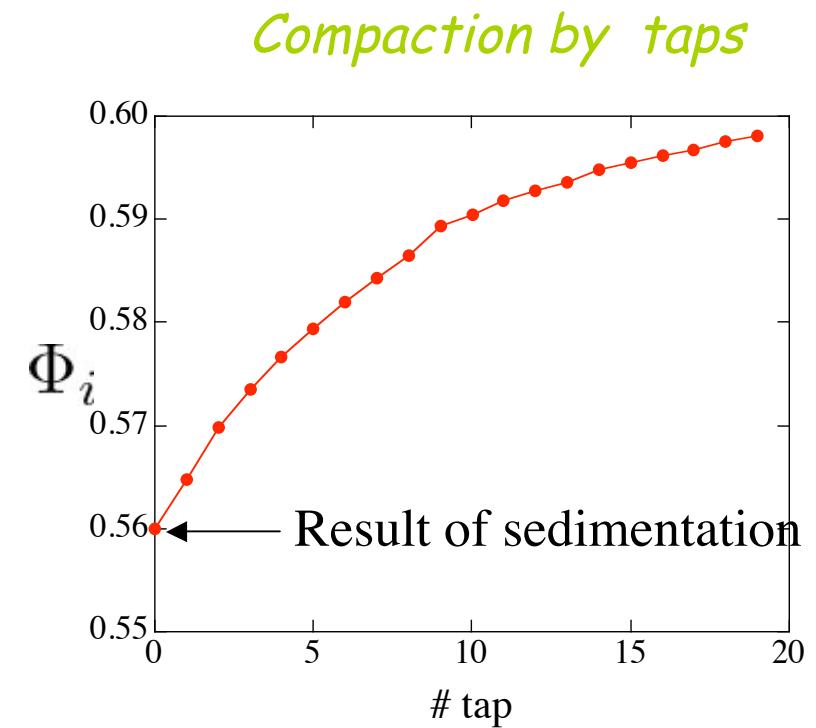
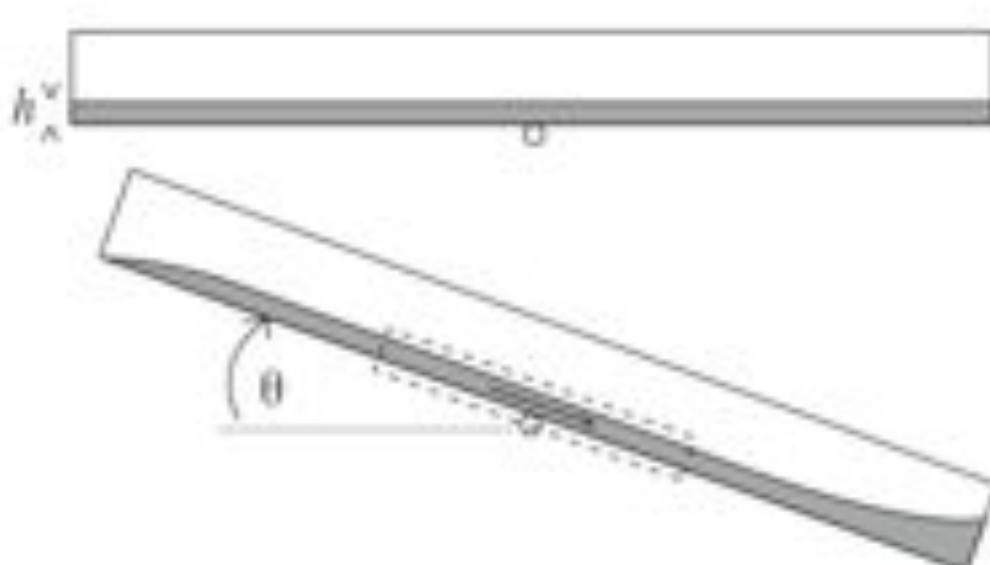
(Pailha et al 08)

Glass beads : $160\mu\text{m}$

Liquid: mixture of water and Ucon oil:
 $\eta=9.8 \cdot 10^{-3} \text{ kg/m.s}$
 $\eta=96 \cdot 10^{-3} \text{ kg/m.s}$



Experimental procedure

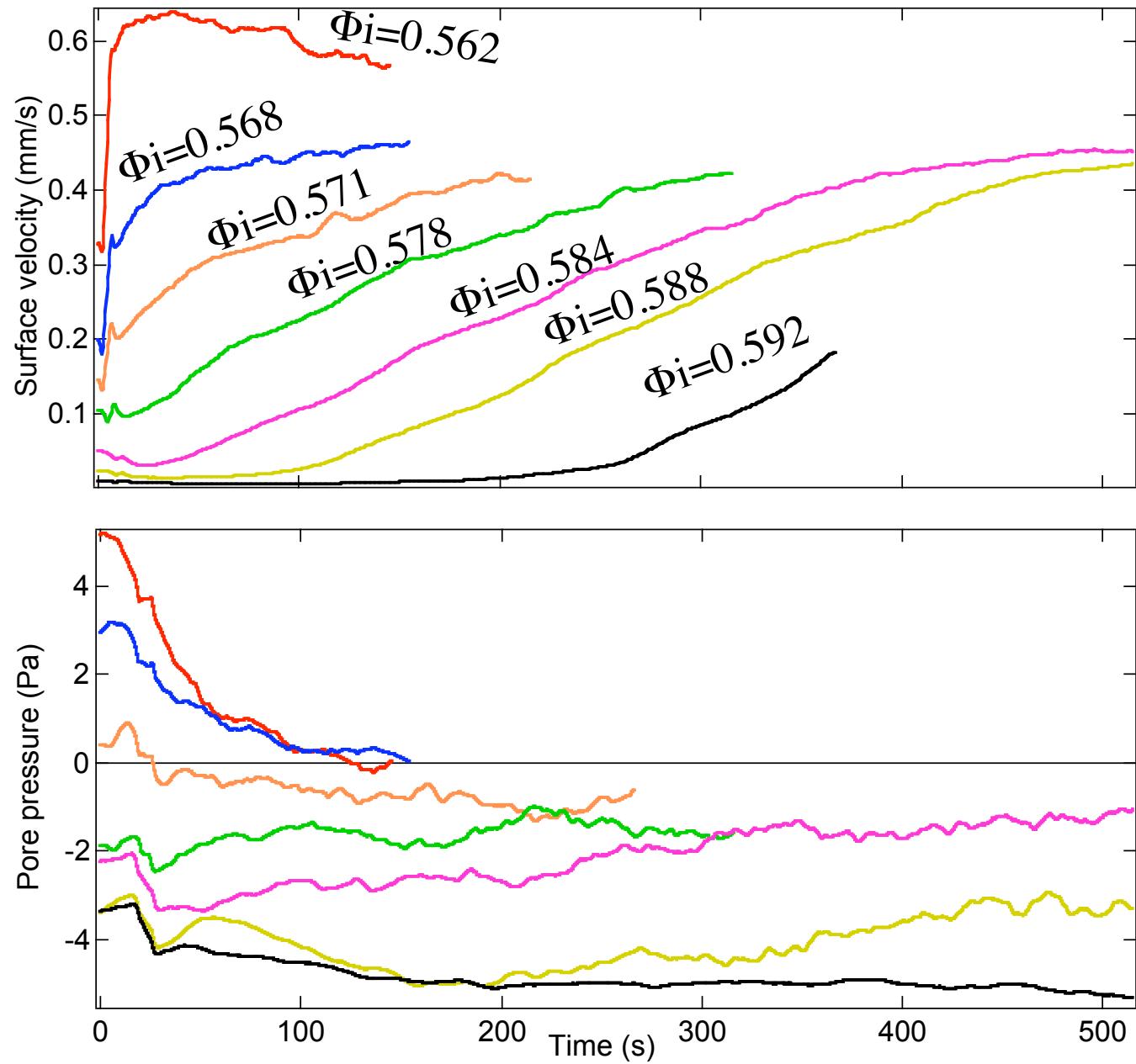


Velocity of the Free surface

Typical results

$\Theta=25^\circ$
 $h=5\text{mm}$
 $\eta=96 \cdot 10^{-3} \text{ Pa.s}$

Pressure under
The avalanche



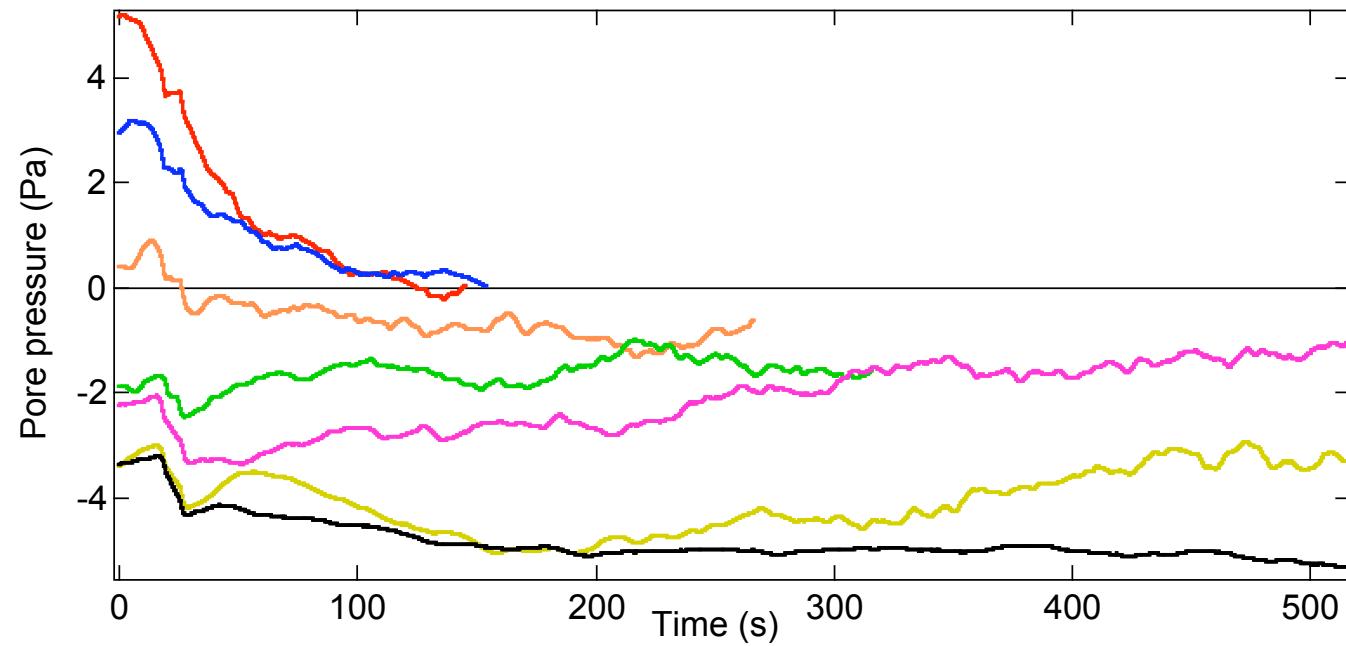
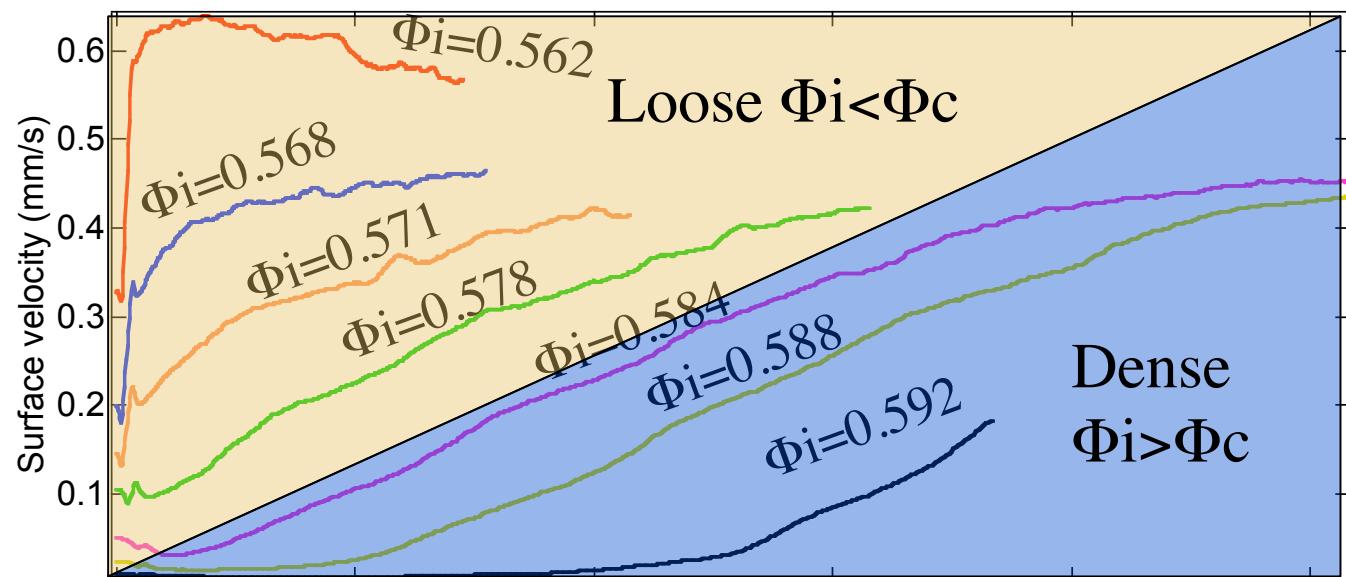
(Pailha et al Pof 08)

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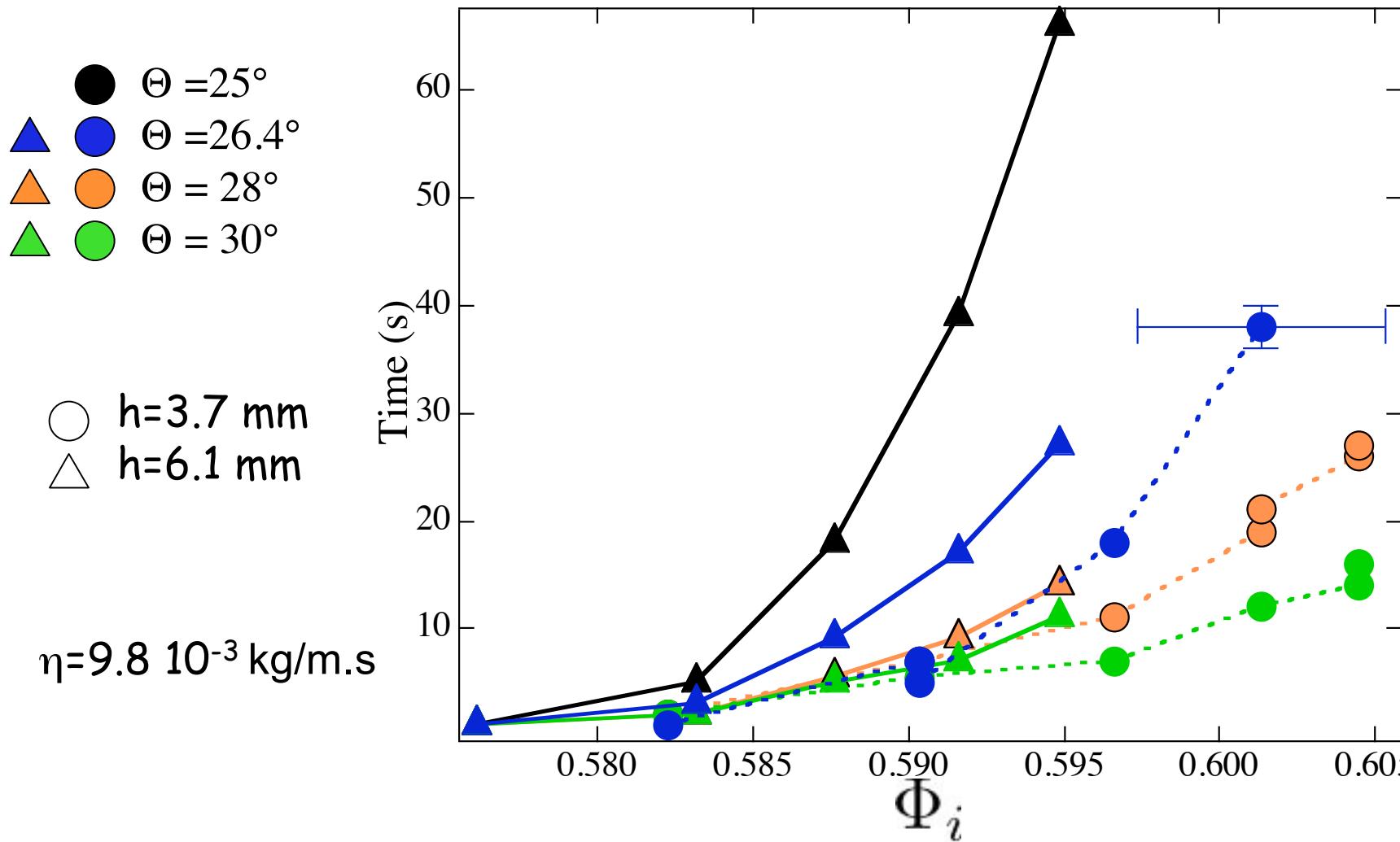


(Pailha et al Pof 08)

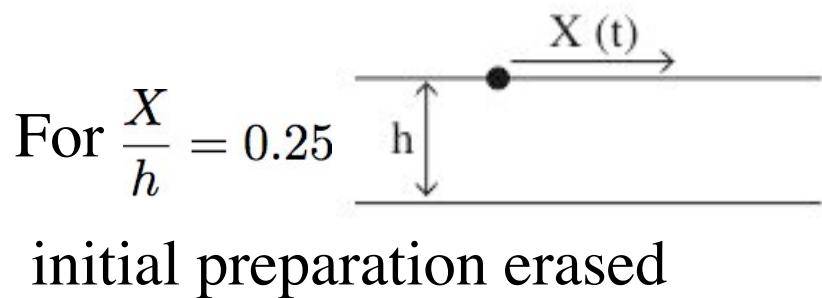
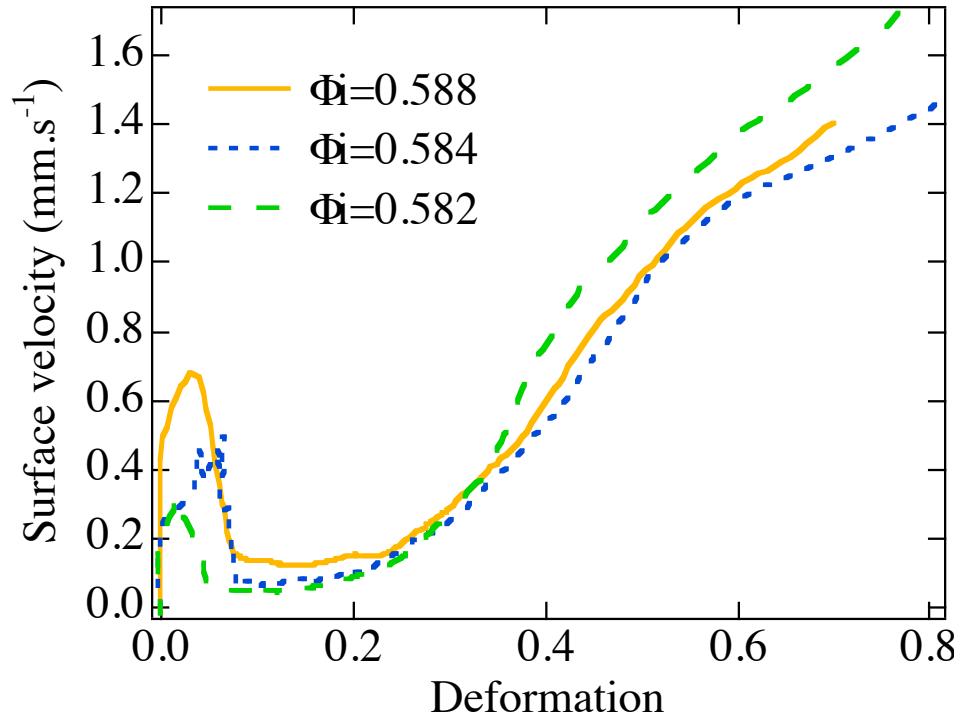
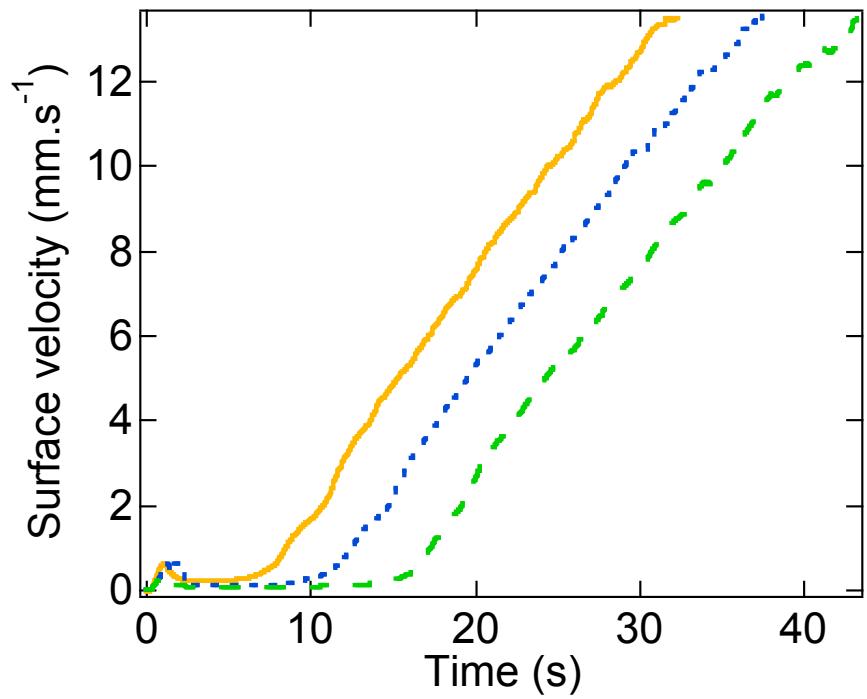
Triggering time

in the dense case

Triggering time



Deformation



$$\frac{t_{\text{trig}} u}{h} = 0.25$$

Two phase flow model

1 Coupling with the liquid:
Two phase equations

Fluids mechanics

2 Rheology of the
granular phase

Granular matter

3 Dilatancy

Soil mechanics

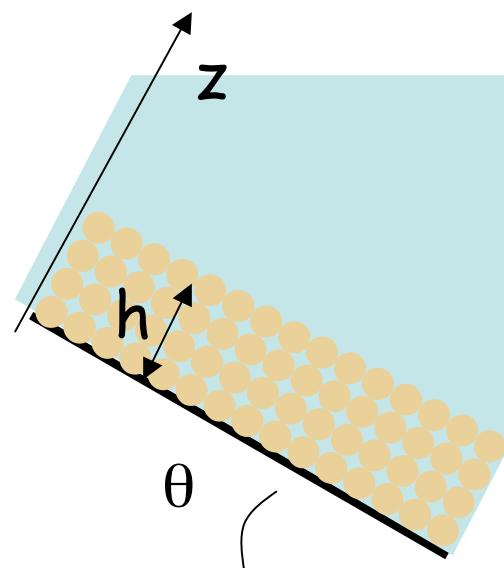
submarine avalanches :

Depth averaged approach (Pitman and Le 05) :

$$\frac{d\bar{\phi}h}{dt} = 0$$

$$\rho_p \frac{d\bar{\phi}h\bar{u}^p}{dt} = (\rho_p - \rho_f)g\bar{\phi}h \sin \theta - \tau_b^p + (1 - \bar{\phi})\beta(\bar{u}^f - \bar{u}^p)h$$

$$\rho_f \frac{d(1 - \bar{\phi})h\bar{u}^f}{dt} = -(1 - \bar{\phi})\beta(\bar{u}^f - \bar{u}^p)h$$



Submarine granular avalanches:

Shear rate
critical state
theory

$$\dot{\gamma}_b = 3 \frac{u^p}{h}$$

$$\tau^p = (\mu(I) + \tan \Psi)p^p$$

$$\tan \Psi = K(\Phi - \Phi_{eq}(I))$$

$$\frac{1}{\Phi} \frac{d\Phi}{dt} = \dot{\gamma}_b \tan \Psi$$

$$I = \frac{\dot{\gamma}_b \eta_f}{p^p}$$

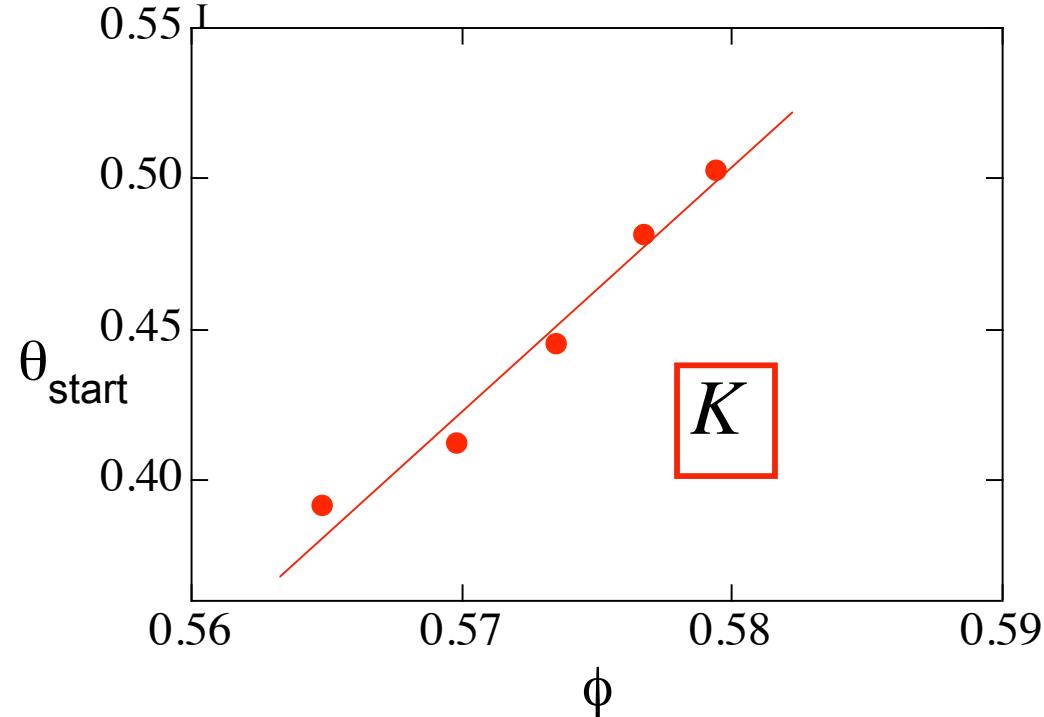
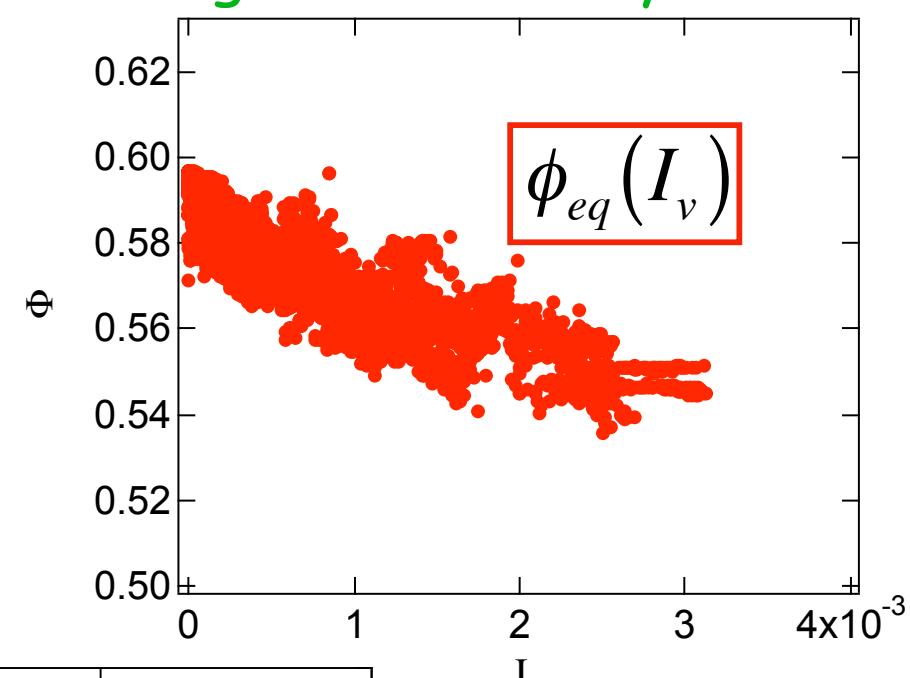
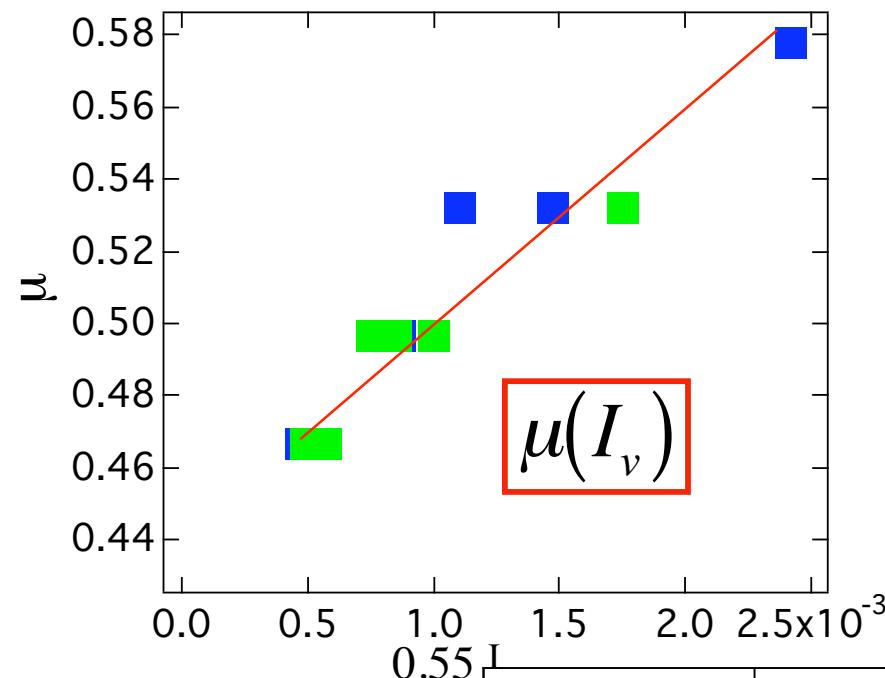
(Cassar et al 05,
Doppler et al 07)

Particle
-fluid
coupling

$$p^p = \Delta \Phi g h \cos \theta - K_2 \frac{\eta}{d^2} h u^p \tan \Psi$$

↑
Relative weight ↑
Viscous drag due to the
Vertical displacement

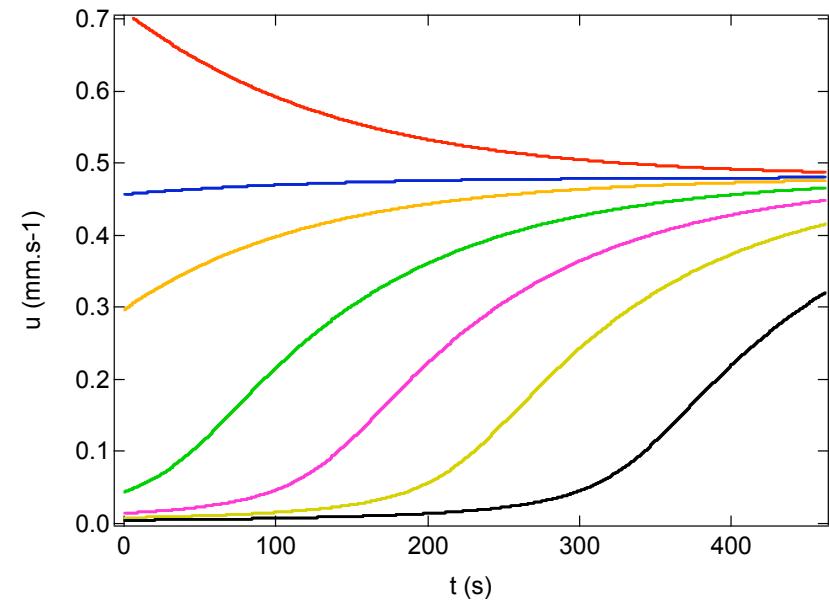
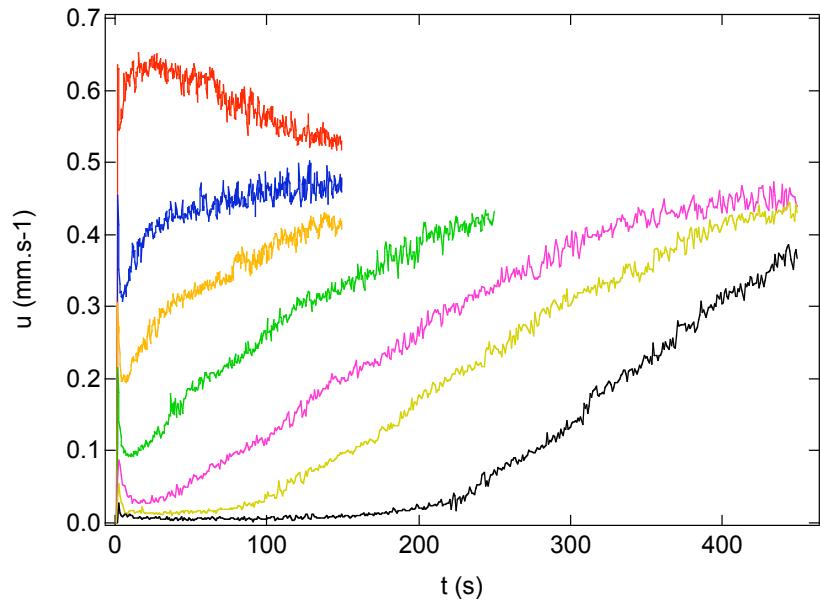
Calibration of the model looking at the steady state



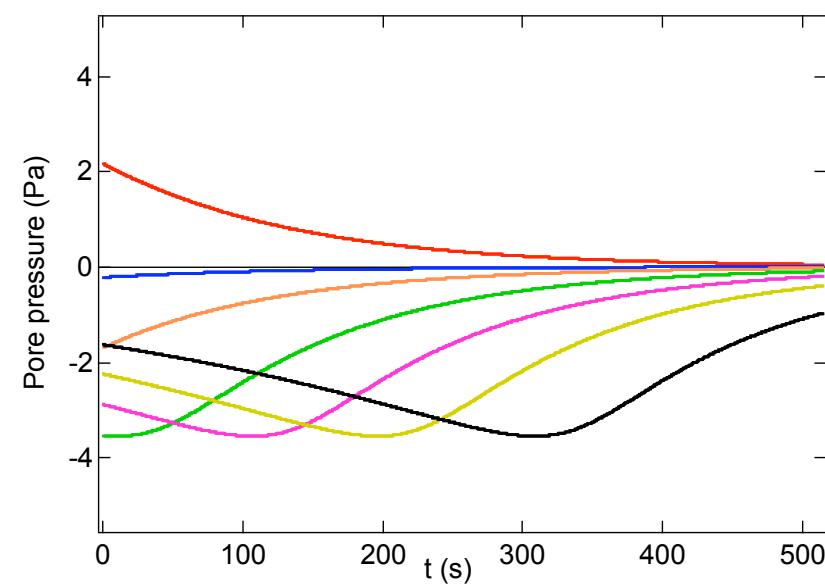
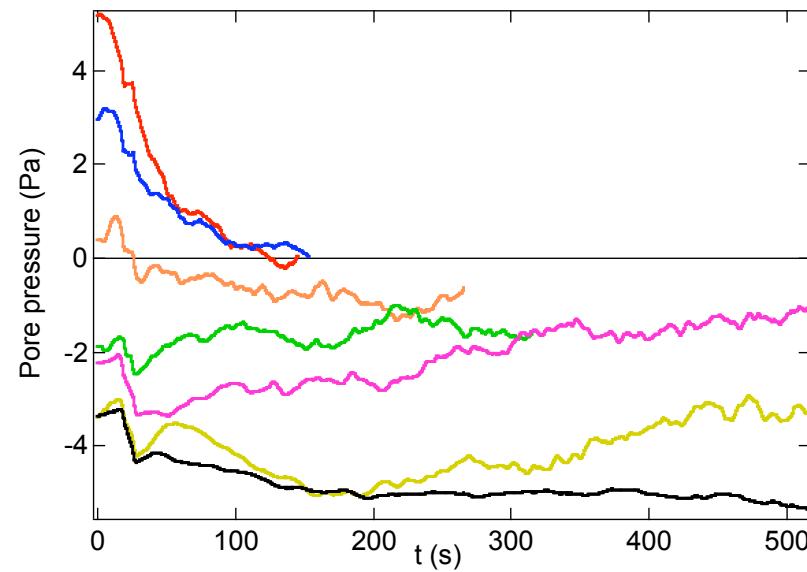
A single free
Parameter
 K_2

Predictions :

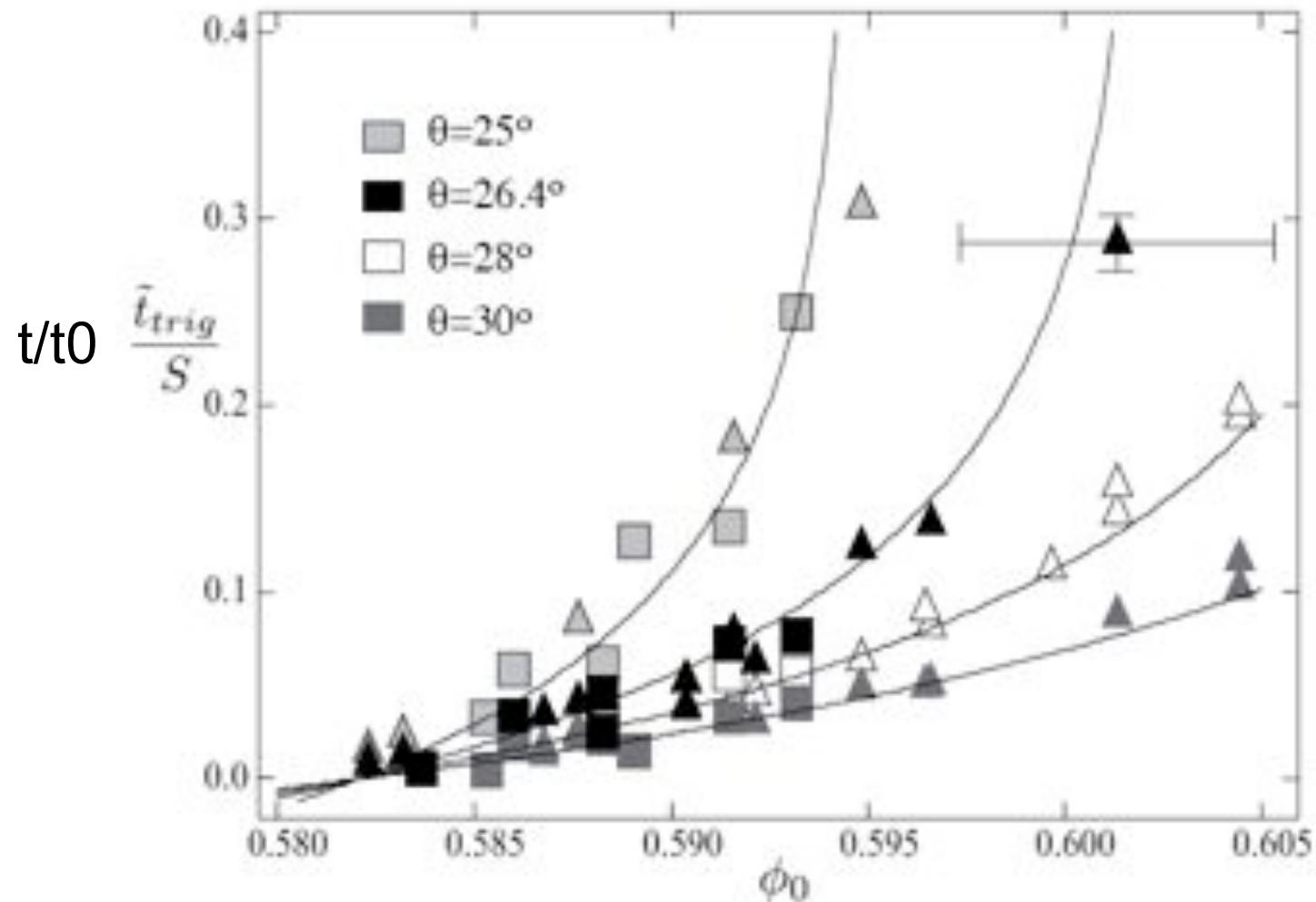
Velocity



Pressure



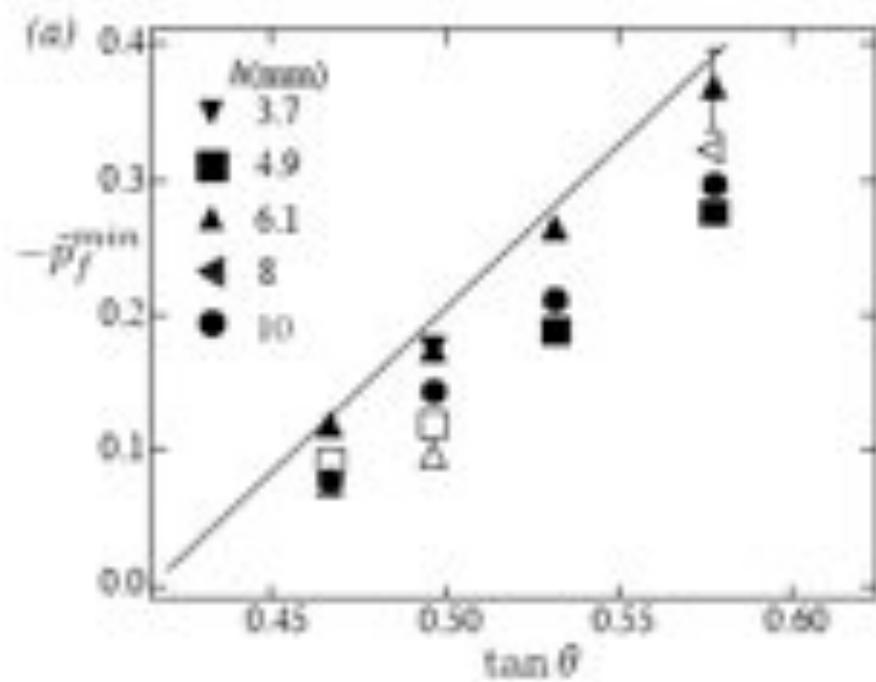
Scaling of the triggering time



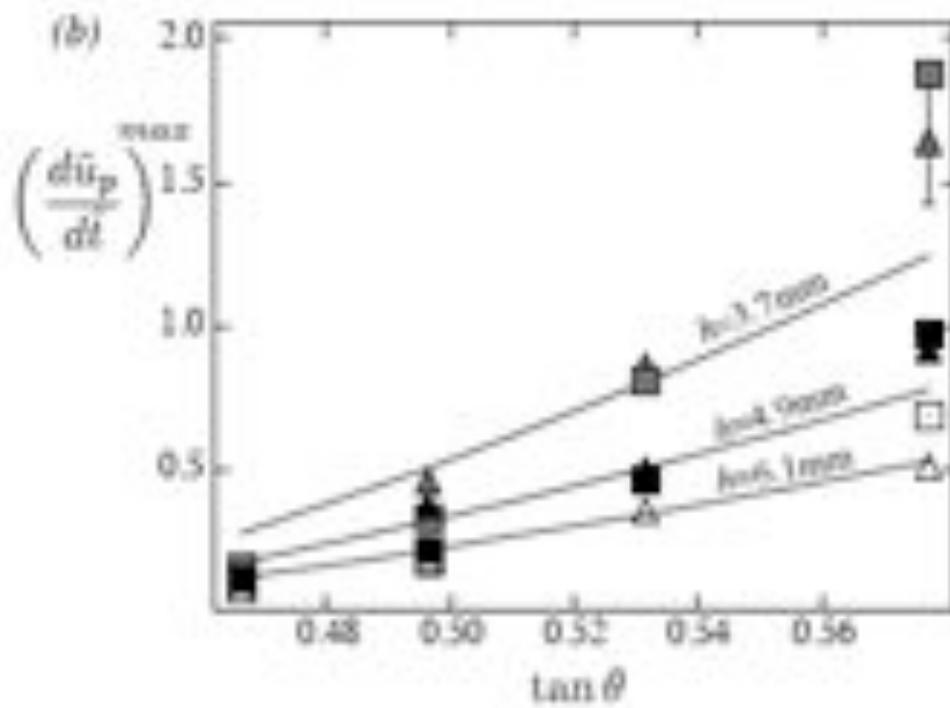
$$t_0 = \frac{0.25\eta h}{2\alpha d^2 \Delta \rho g \Phi_i \cos \theta}$$

Different h
Different viscosities

Pore Pressure



Maximum acceleration



Conclusions for submarine avalanches

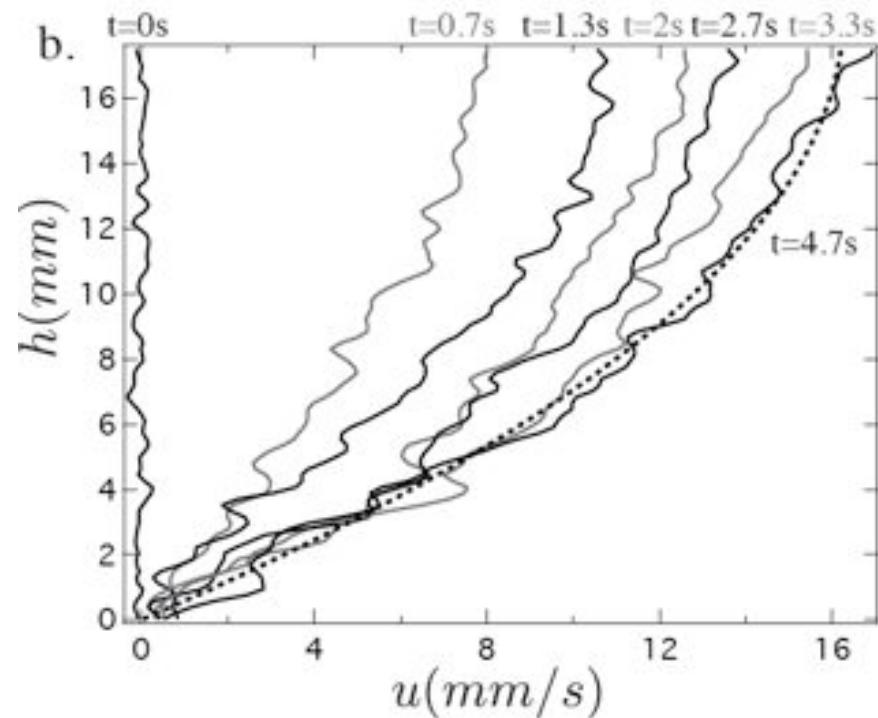
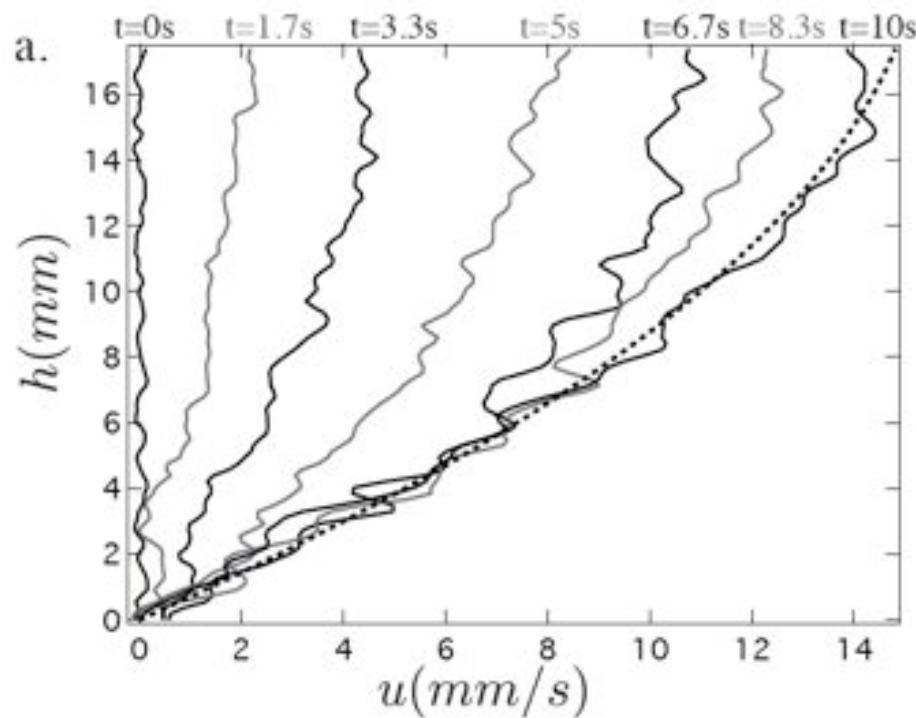
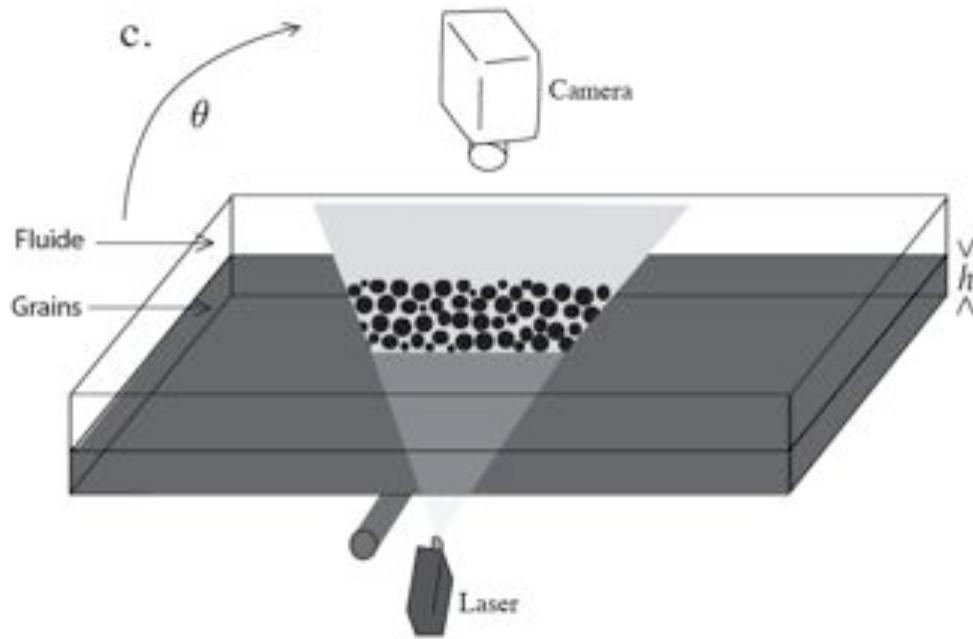
A simple critical state approach + a viscoplastic rheology
+ two phase flow equations

⇒ Semi quantitative predictions in the complex
dynamics of the flow initiation of submarine avalanches

Beyond the depth averaged approach ?
Question of the numerical implementation of such models?

Index matching method

Mickael Pailha
unpublished



Conclusions for constitutive modeling of granular flows

Visco-plastic approach gives the order zero of viscous behavior of granular flows

It can serve as a base for further developments:

- irregular particles?
- cohesive particles?
- polydispersed materials?
- breakable particles?

(dilatancy, underwater granular flows, cohesive flows...)

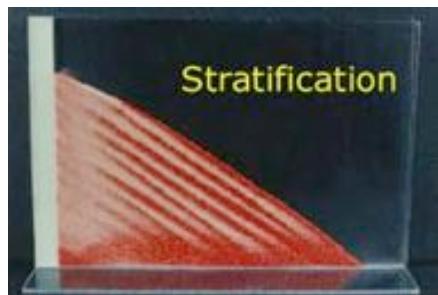
- link with the microscopic physics?
- how to capture non local effects (role of fluctuations, link with glassy systems,...) ?

Towards more complex granular media:

Polydispersed :

Felix et Thomas PRE 04

Rognon et al 06...



granular matter with
fluid interactions



Cohesive granular matter:

Rognon et al 08

Halsey et al 06

Richefeu et al 06 ...



Merci à

Mickael Pailha
Pierre Jop,
Cyril Cassar
Yoël Forterre
Pascale Aussillous
Maxime Nicolas
Prabhu Nott
Jeff Morris
Neil Balmforth
Bruno Andreotti
Olivier Dauchot...